





Improving Treatment to Reduce Storage

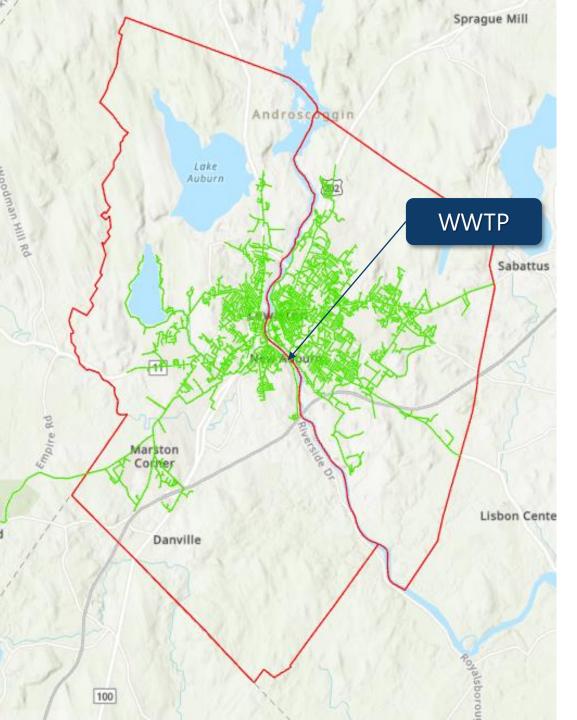
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January 24, 2023



Agenda

- \rightarrow Background
- → Technical Approach
 - Collection System Improvements
 - Treatment Plant Optimization
 - Right-Sized Storage
- → Conceptual Design and Cost Estimating
- \rightarrow Conclusion



Background – Wastewater Collection & Treatment

- → City of Auburn
 - West side of Androscoggin River
 - ▶ Pop ~24,000
- → Auburn Sewerage District (ASD)
 - ~112 miles collection system piping
 - → 4"-54"
 - Crosses Androscoggin River through triple siphon (2x18" 1x24")
- → City of Lewiston
 - East side of Androscoggin River
 - Pop ~37,000
 - ~155 miles collection system piping
 - → 4″-6′x12′
- → Lewiston Auburn Water Pollution Control Authority (LAWPCA) WWTP
 - Constructed 1971
 - Primary + Secondary + Disinfection
 - 32 MGD Peak Wet Weather Capacity

Background – CSO Abatement Progress (First CWAMP in 1998)

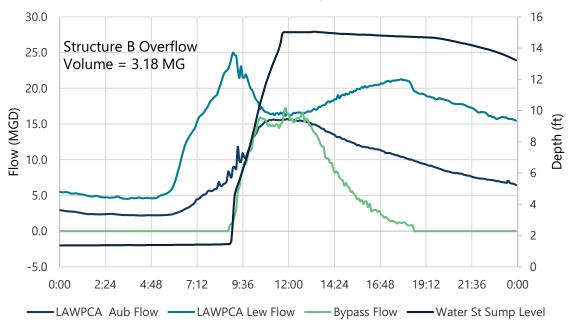
	ASD	Lewiston	LAWPCA
CSO Outfalls (initial)	8	32	1
CSO Outfalls (present)	2	8	1
Annual CSO Volume (MG) 2000	45	100	200
Annual CSO Volume (MG) 2017 – 2021	0.2 – 1.7	8.5 – 23	14.5 – 33.7
Percent Public Roads Separated	100%	96%	NA
Investment in Reduction 2000 – 2021	\$22M	\$37.5	\$3.25
Cost per MG (approx.)	\$0.5M	\$0.4M	\$0.02M
Next Step - S	torage at LAWPC	A (3.1 MG)	
Storago Taple	¢ 4 0 + N 4		

Storage Tank\$40+MAnnual CSO Volume Post Project (est.)0-8 MGCost per MG (approx.)\$2+M

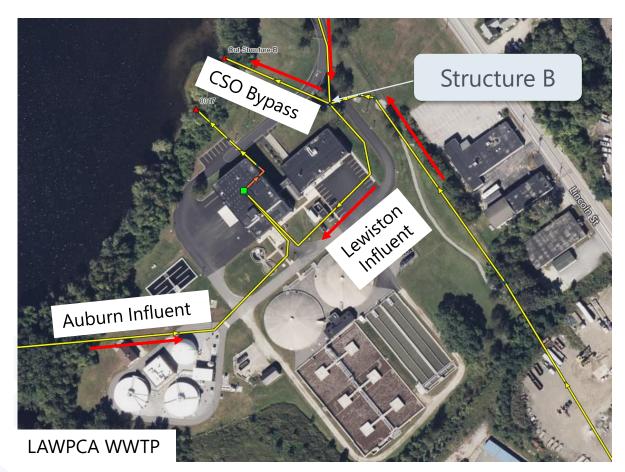


Project Objective

Eliminate overflow at Structure B during 1-year, 6-hour design event: 2.05 inches; 1.6 in/hour

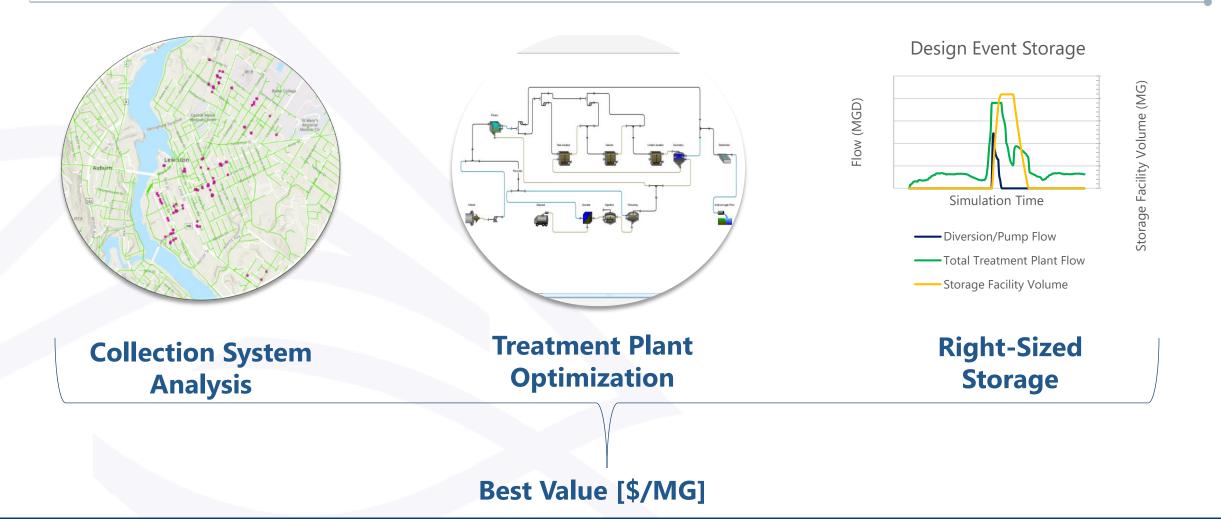


CSO Event February 27, 2020





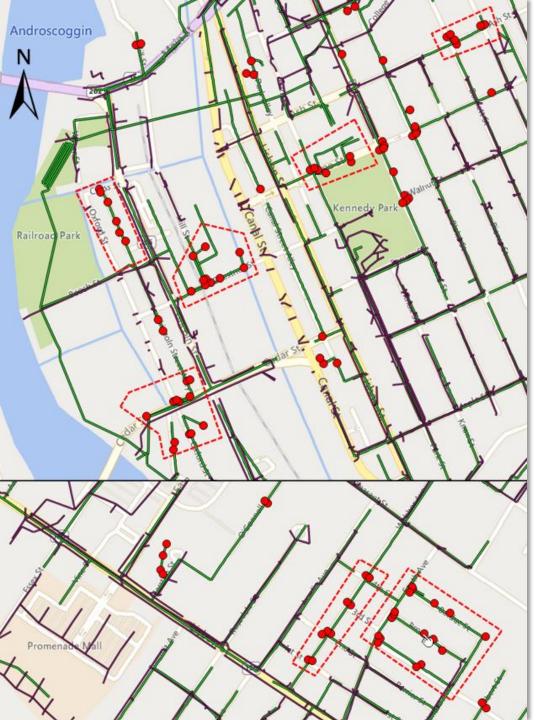
Project Approach





Collection System Analysis

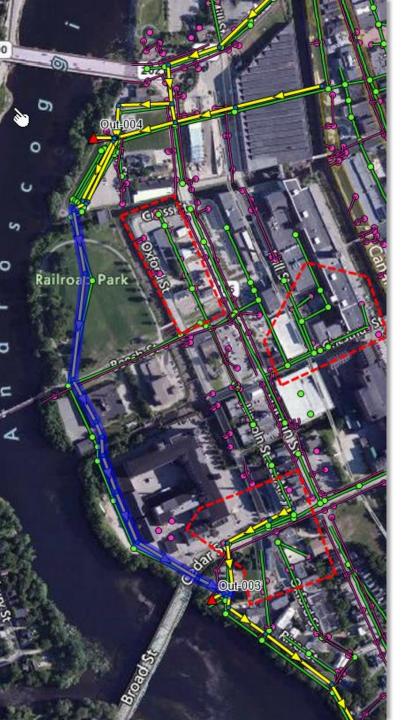




Lewiston Sewer Model Review

Identified Inflow Sources

- \rightarrow 262 drain structures connected to sewer
- → 41 catch basins scheduled for separation (2019 CWAMP)
- → 62 additional structures identified for potential separation
- \rightarrow Up to 0.6 MG CSO volume reduction



Lewiston Sewer Model Review

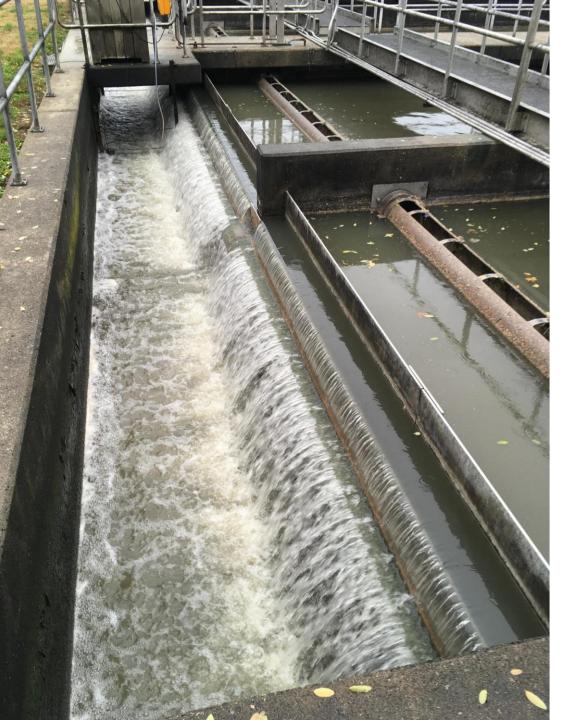
Identified pipes with excess capacity during design event

- → Northwood Rd to Jepson Brook (0.07 MG)
- → Railroad Park to Cedar St (0.07 MG)
- → Up to 0.14 MG CSO volume reduction

Total Collection System Improvements Cost: \$2.8M; 0.74 MG

Treatment Plant Optimization

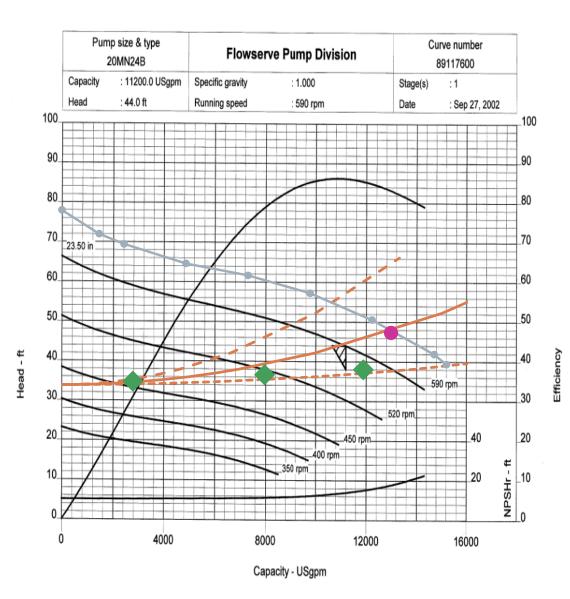




Treatment Plant Optimization

- → Hydraulic Capacity
 - Influent Pumps
 - Gravity Hydraulics
- → Process Capacity
 - Secondary Clarifiers
 - Other Processes
 - » Flow meters
 - » Influent Screens
 - » Grit
 - » Primary
 - » Chlorine Contact

→ Capacity can be increased from 32 MGD to 38 MGD with modest improvements



Influent Pumps

- →Three 200 hp pumps
- →32 MGD with two pumps
- →Increasing speed achieves 38 MGD
 - 640 rpm, 186 hp
 - Still a good operating point
 - Switch from12 to 10-pole motors
 - Increase speed to 63 Hz
- →Other options:
 - Fourth pump (39 MGD)
 - Parallel FM (37 MGD)
 - Fourth Pump and Parallel FM (50 MGD)
 - Larger pumps (45 MGD)

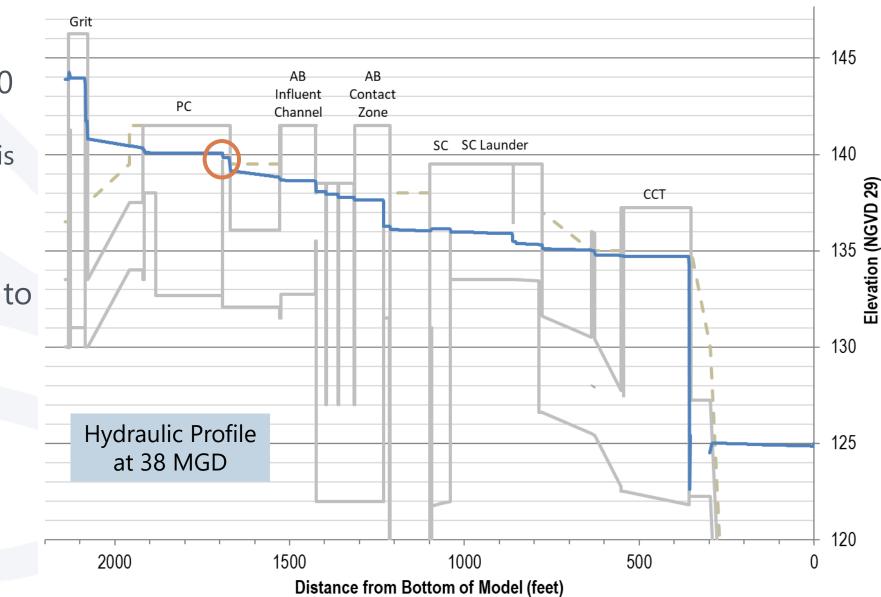
Gravity Hydraulics

→Primary clarifier weir submerges at 36 to 40 MGD

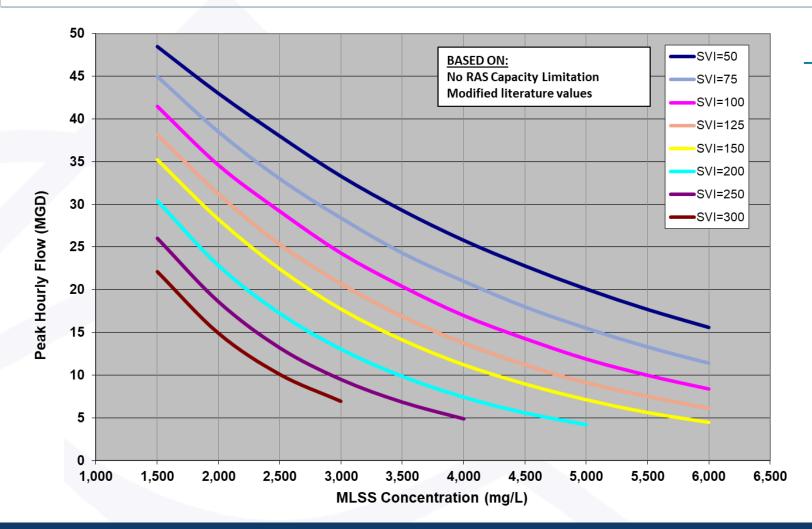
- Operators observe this occurs at 33 MGD
- Investigate possible blockage of PE pipe

→Could push the plant to 43 to 47 MGD

> Scum systems are submerged



Secondary Clarifiers



→Clarifier operating diagram based on modified state-point equation

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Secondary Clarifiers

	Sludge Volume Index (g/mL)			
	100	125	150	
Mixed Liquor Concentration (mg/L)	Secondary Clar	ifier Peak Hour Flow	Capacity (MGD)	
1000	49	46	43	
1500	42	38	35	
2000	35	31	28	
2500	29	25	22	

- → Process optimization can achieve 38 MGD clarifier capacity
 - wet weather contact stabilization
 - chemical addition
 - selector optimization
- →Capital improvement required for higher flows
 - Intensification
 - Additional Clarifier





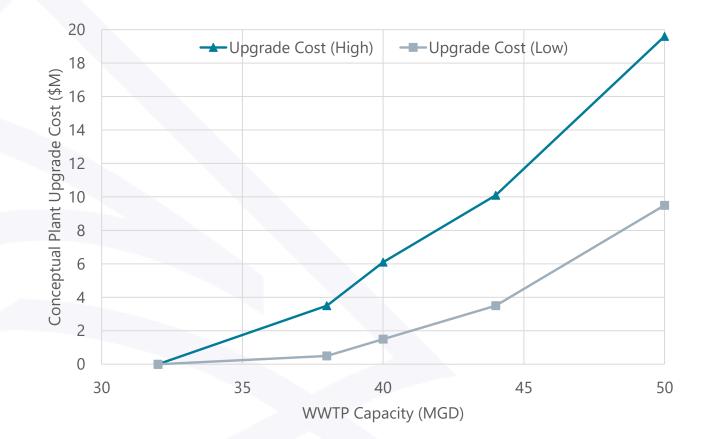
Other Processes

- →Influent Flow Meters
 - currently being evaluated
- →Influent Screens
 - design underway for new multi-rake screens

→Grit

- 38 to 76 MGD capacity
- →Primary
 - 44 MGD nominal capacity based on surface overflow rate
 - consider baffling or chemical addition
- →Chlorine Contact
 - 38 MGD (15 min contact time)
 - 42 MGD (upstream dosing)
 - Increase doses of hypo & bisulfate

Conceptual Plant Upgrade Cost



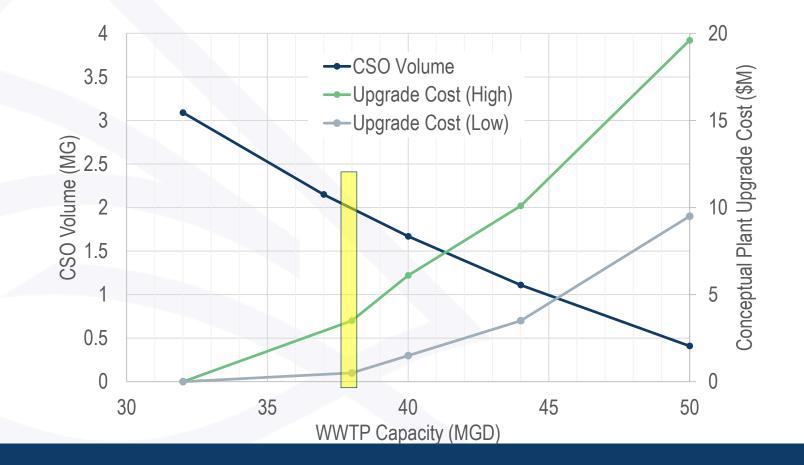


Right-Sized Storage & Alternatives Analysis



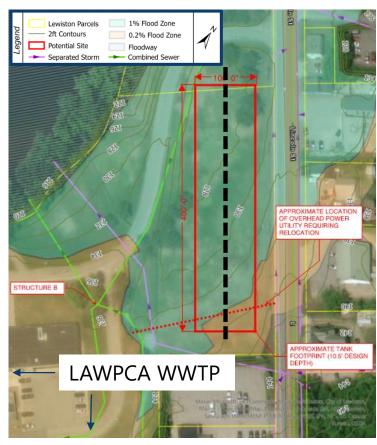
Treatment Plant Capacity vs Storage Size

CSO Volume Required Without Plant or Collection System Improvements: 3.1 MG

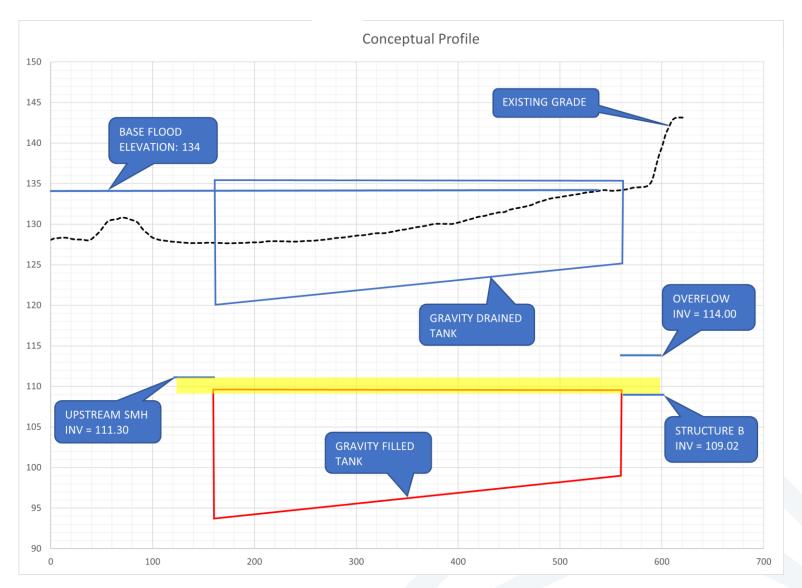




Gravity vs. Pump



Conceptual Layout - LAWPCA parcel



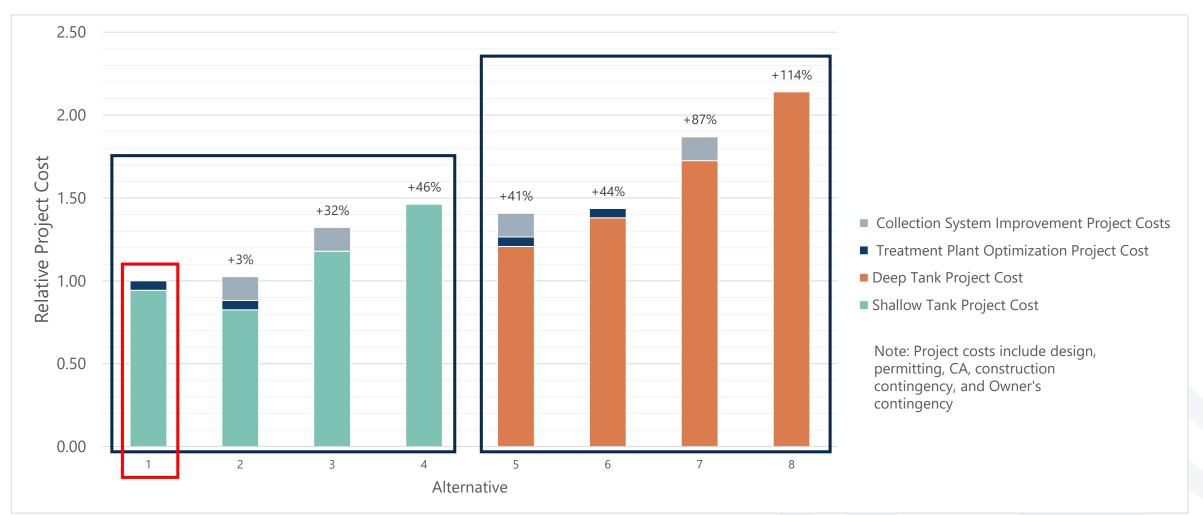


Alternatives Evaluated

Scenario	Treatment Plant Capacity	Collection System Improvements	Tank Depth	Pumping	Tank Volume (MG)
1	38	No	Shallow	Required to fill	2.1
2	38	Yes	Shallow	Required to fill	1.75
3	32	Yes	Shallow	Required to fill	2.5
4	32	No	Shallow	Required to fill	3.1
5	38	Yes	Deep	Required to empty	1.75
6	38	No	Deep	Required to empty	2.1
7	32	Yes	Deep	Required to empty	2.5
8	32	No	Deep	Required to empty	3.1



Alternatives Cost Comparison





Conceptual Design & Cost Estimate



Conceptual Design Layout

- DIVERSION
 STRUCTURE
- WET WELL &
 PUMP STATION
- VALVE VAULT
- STORAGE CONDUITS
- DRAIN GATES &
 PIPING
- ELECTRICAL
 BUILDING &
 GENERATOR



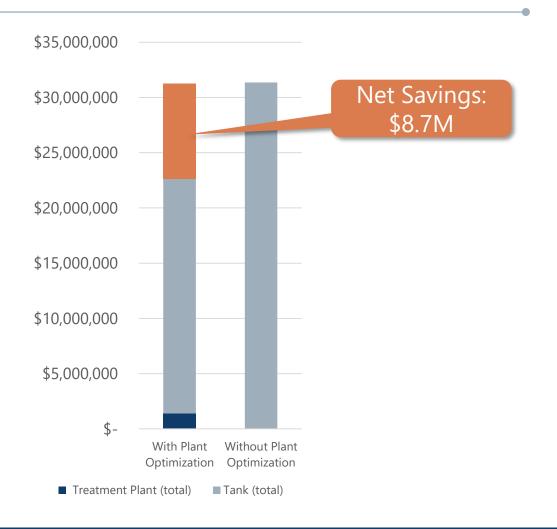
Opinion of Probable Project Cost

Project Component	Estimated Cost
Storage Conduit & Piping	\$16,370,000
Pump Station & Valve Vault	\$2,980,000
Electrical Building, Equipment, & Site Utilities	\$1,950,000
Treatment Plant Optimization	\$1,400,000

Estimated Total Project Cost \$22,700,000

Note: Project costs include design, permitting, CA, construction contingency, and Owner's contingency

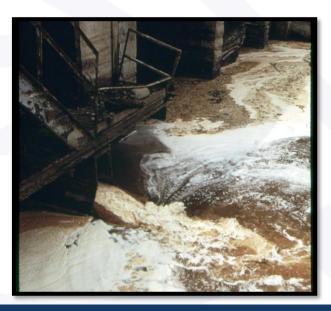
Next Step - Storage at LAWPCA				
Option	Project Cost	Approx. Cost/MG Abated		
3.1 MG Deep Storage Tank	\$40+M	\$2M/MG		
3.1 MG Shallow Storage Tank	\$31.4M	\$1.6M/MG		
2.1 MG Shallow Storage Conduits	\$22.7M	\$1.1M/MG		





Conclusion

- → Early phases of LTCP attack low-hanging fruit
- →Costs per gallon abated only increase
- →As the investment gets bigger, more detail is warranted
- →If spending \$1.4M can save \$8.7M, it's worth looking closer











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Thank You!