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# *Alkaline Hydrolysis of NC fines and comparative evaluation of post-hydrolysis techniques for nitrogen removal*

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# Alkaline Hydrolysis (AH) of waste NC fines



## Outline

- 1. Kinetics of alkaline hydrolysis (AH) for degradation of NC fines (pure/waste) at bench scale*
- 2. Pilot scale testing of AH-liquor*
- 3. Evaluation of post-hydrolysis techniques for nitrogen removal from AH-liquor*
- 4. Nitrogen removal from post-AH NC liquor with bimetal reduction*
- 5. Nitrogen removal from post-AH NC liquor with conventional denitrification with BOD assessment of post-AH NC liquor*



# Nitrocellulose (NC) fines

- Generated through nitration of cellulose ester polymer
- Used in production of propellants, smokeless gunpowder, and some explosives<sup>1</sup>
- Self ignition stability is directly related to degree of nitrogen purity<sup>1</sup>
- Higher nitration – more unstable
- Insoluble in water<sup>2</sup>
- Solubility in other liquids depends on nitrogen content
- Low nitrogen mixtures soluble in acetone and Ether-alcohol mixtures<sup>3</sup>
- High nitrogen mixtures soluble in acetone

NC	
N Content	12.6-14%
Flash point	12.8 °C
Melting and ignition	160-170 °C
Specific Gravity	1.66
m.w.	504.3

1. Kim, Byung J, and Jae K Park. Comprehensive Evaluation and Development of Treatment Technologies for Nitrocellulose Fines and Process Wasterwaters. U.S. Army, 1993.

2. Weston, Roy F. Composting Nitrocellulose Fines - Hazard Analysis. Weston, Inc, 1995.

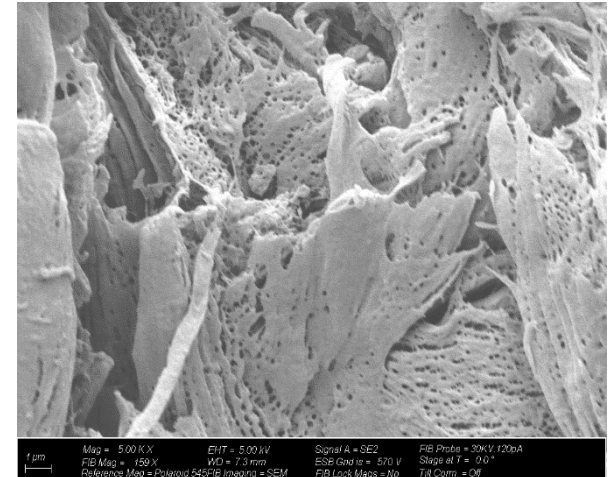
3. López-López, María, et al. "New Protocol for the Isolation of Nitrocellulose from Gunpowders: Utility in Their Identification." Talanta, Elsevier, 25 Mar. 2010.

# Nitrocellulose (NC) fines

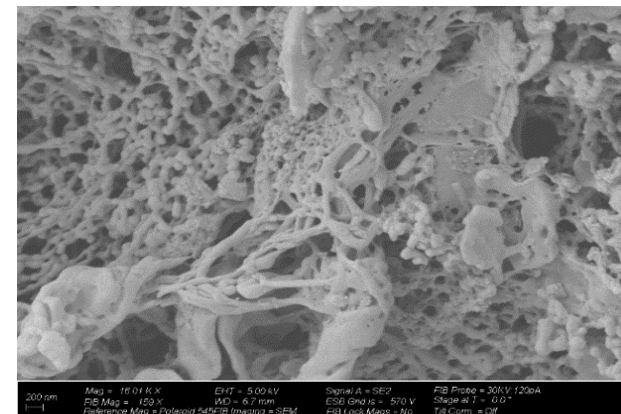
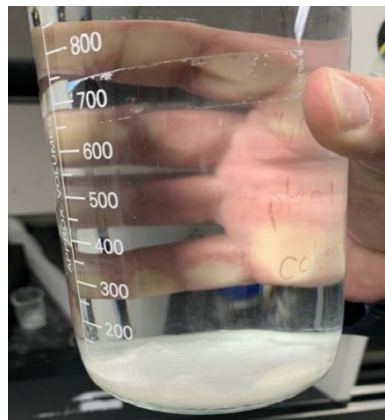
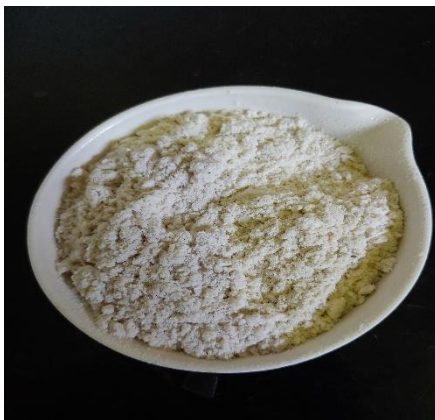
- Production grade NC fines [NC (p)]



NC(p)	
Water %	40-50
Elemental analysis	
C%	25.43
H%	2.49
N%	12.75



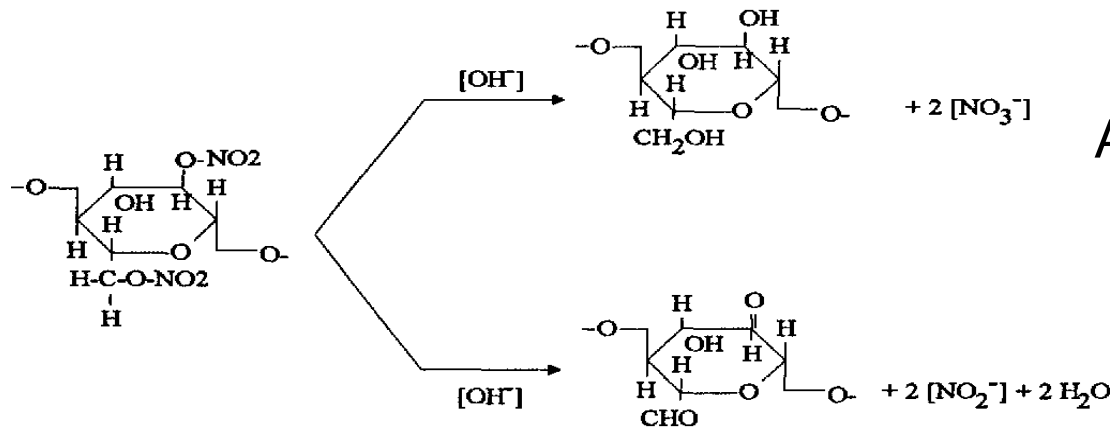
- NC fines from wastewater stream [NC(w)]





# Alkaline hydrolysis (AH): kinetic study

- NC wastewater with 3% solids concentration
- AH is a resilient technique proved for degradation of NC
- AH can achieve denitration of NC while also decomposing the primary cellulose backbone



Alkaline driven mechanism for NC decomposition  
(Christodoulatos et al., 2001)

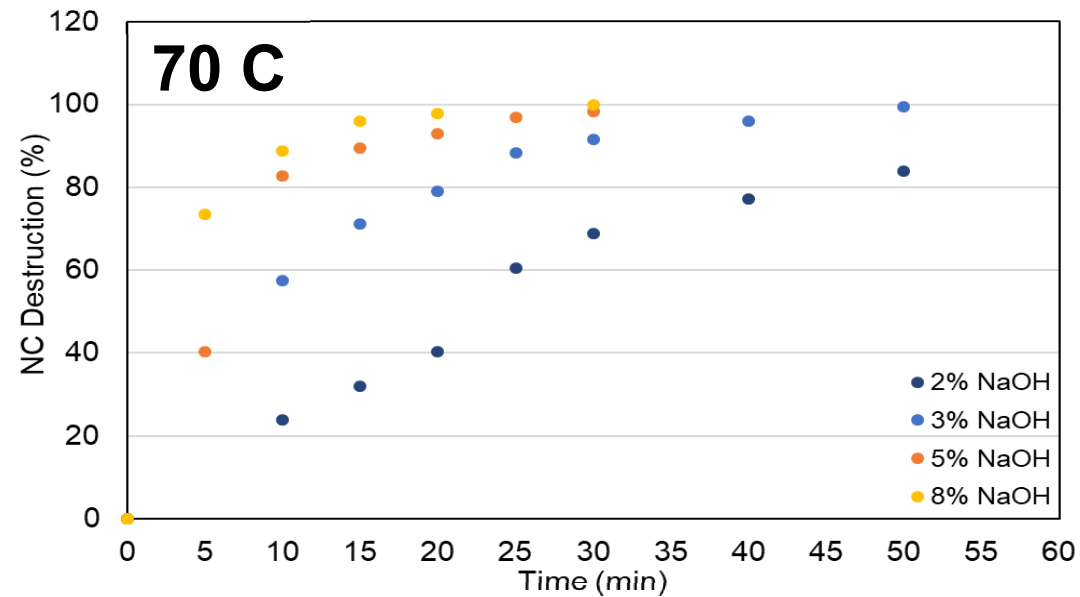
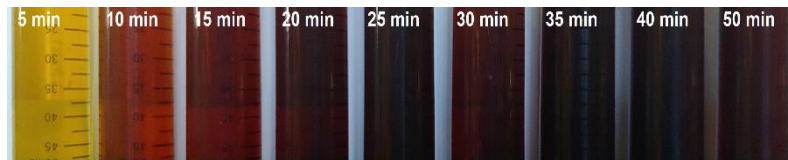
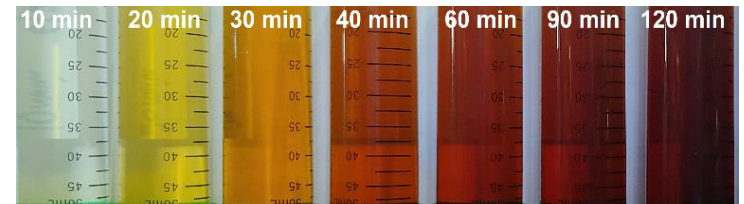
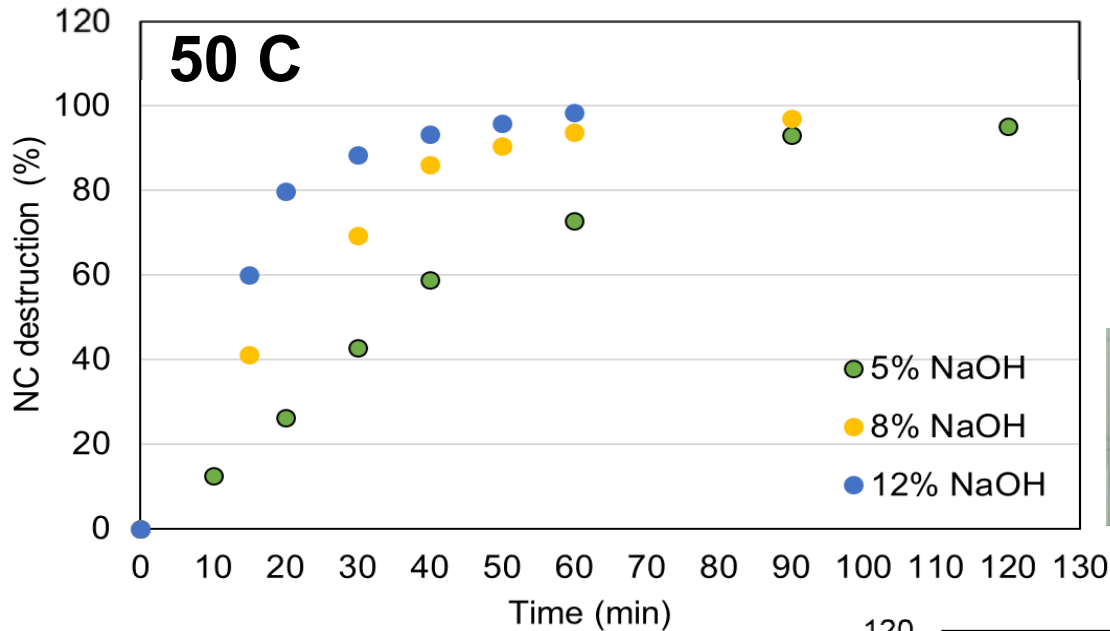
## Bench scale testing

- Sodium Hydroxide as alkaline medium
- One flask (250 ml Erlenmeyer flasks, 100 ml reaction volume) for each sampling point sacrificed at specific time intervals

## Testing conditions with NC(p)

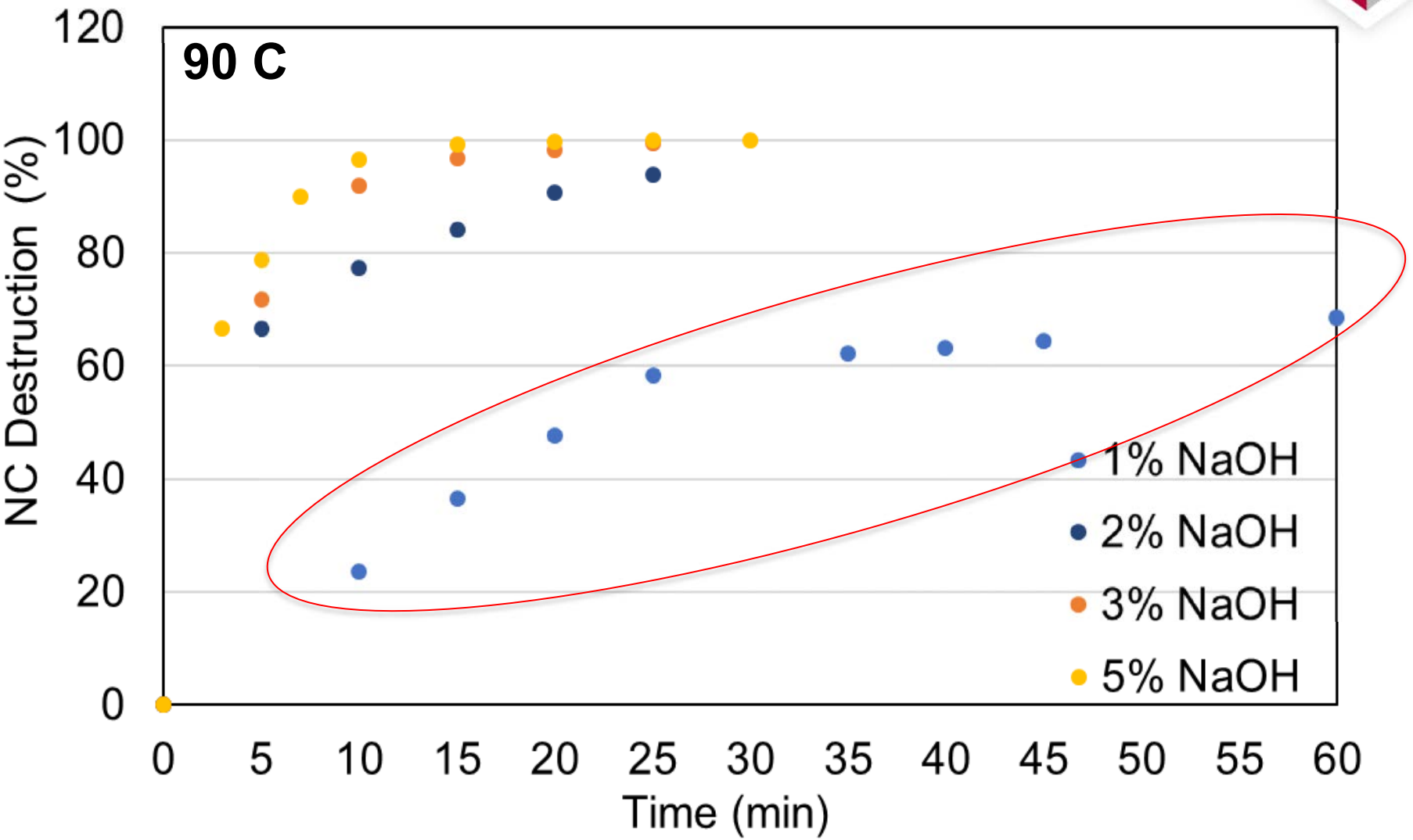
Parameter	Value
Temperature (C)	50,70,90
NaOH (%)	1,2, 3, 5, 8, 12
NC (%)	3

# AH of NC(p)





# AH of NC(p)

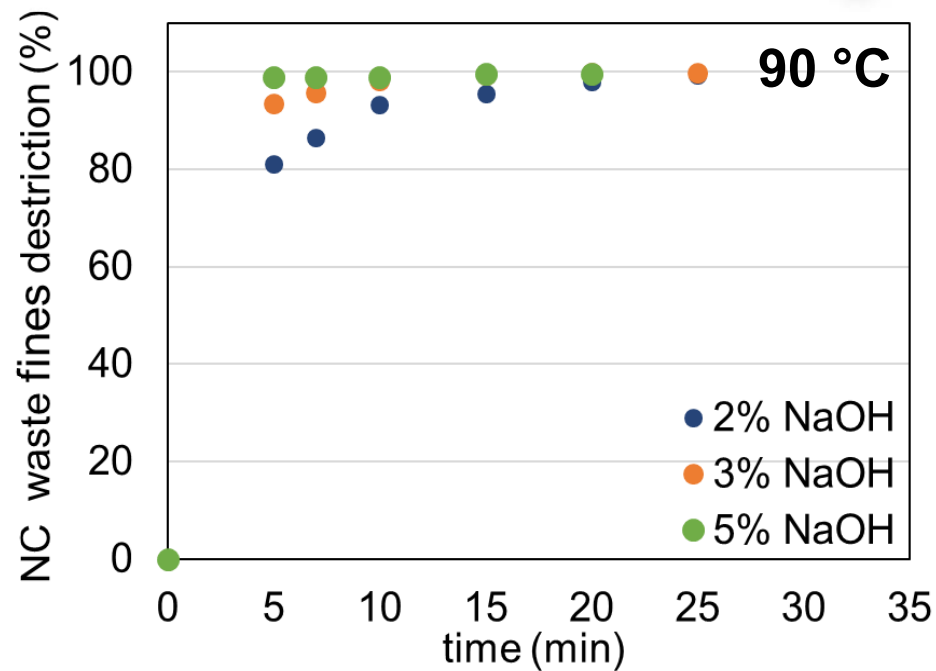
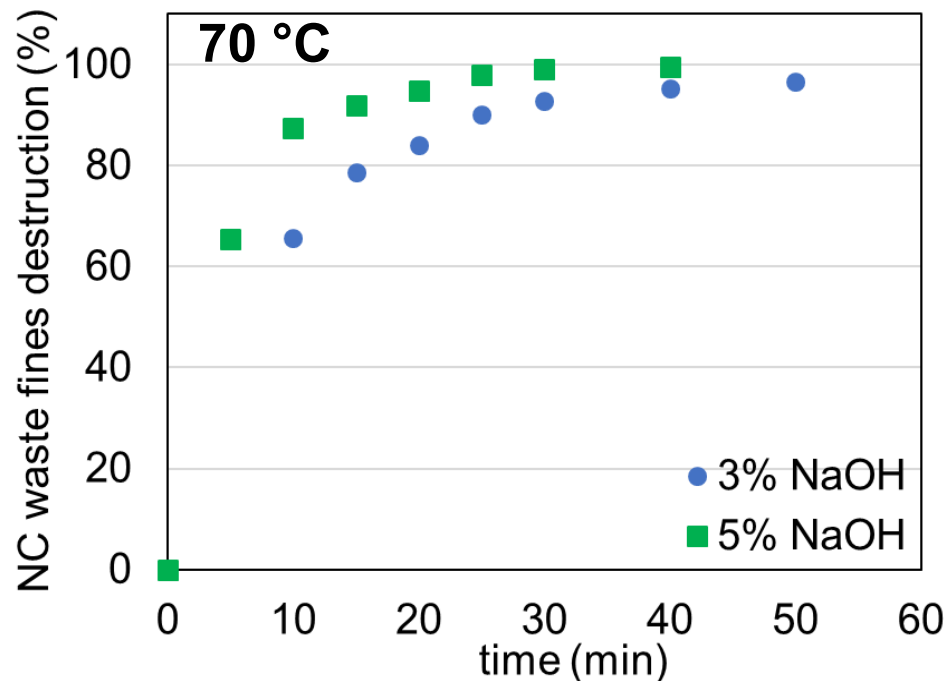


Average time to reach 99% destruction  $\geq 25$  min



# AH of NC(w)

Testing 3% solids content with waste NC fines from wastewater stream



*NC:NaOH solids ratio of 1:1 will obtain 99% destruction within 30-60 min for with 90-70 °C*



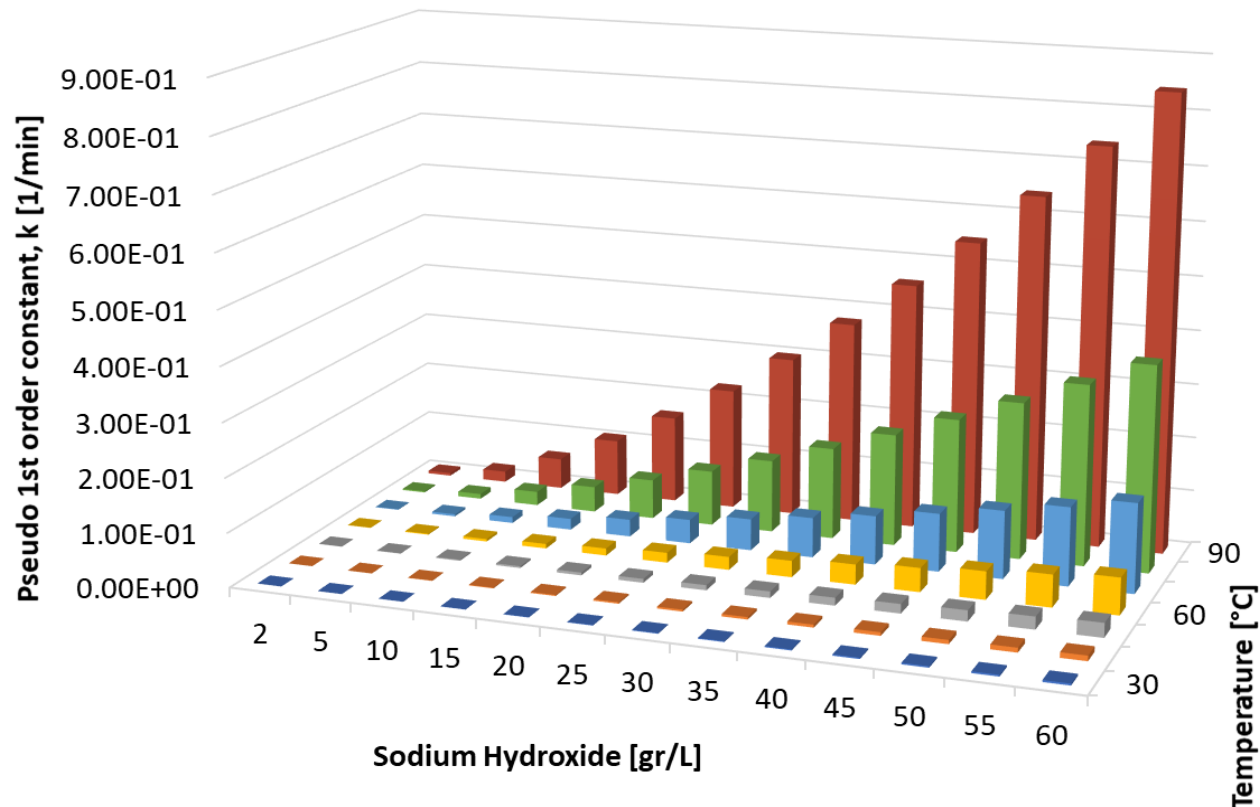


# AH kinetic study

*Kinetic model for degradation of NC fines*

$$C_{NC} = C_{NC}^0 \exp \left[ \left( -2.44 \times 10^9 (C_{NaOH}^0)^{1.5} \exp \left( -\frac{10152}{T} \right) \right) t \right] \text{ for } [NaOH] \left[ \frac{gr}{L} \right]$$

*Estimated AH  
Pseudo First Order  
Constants (k)  
for NC fines  
degradation as a  
function of  
NaOH (g/L) and  
Temperature*



# Characterization of post-AH NC liquor

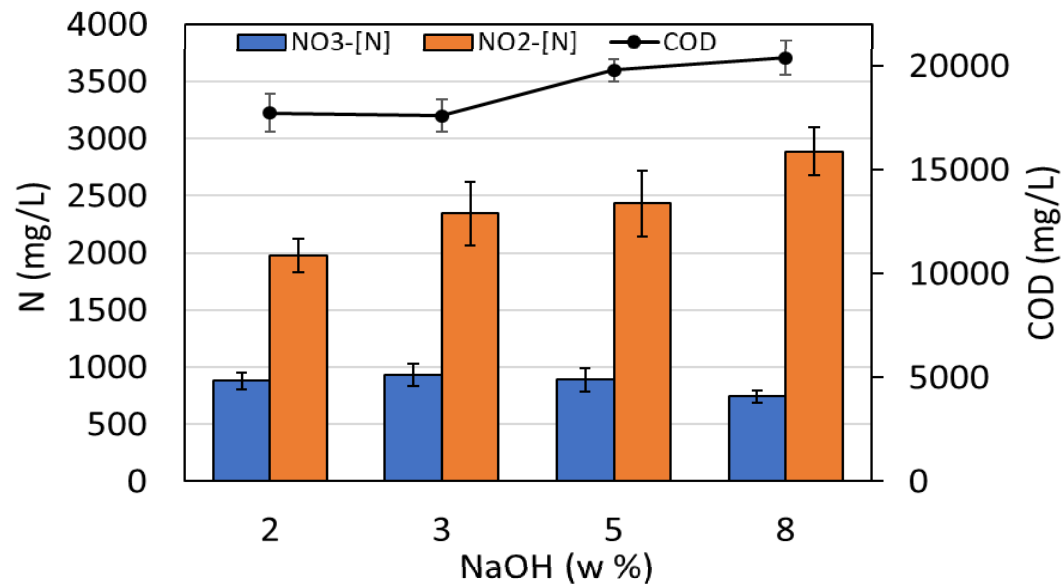
- *Extremely dark color*
- *High pH*
- *Inorganic nitrogen load up to 4000 mgN/L*
- *Organic carbon load up to 18 g/L*



pH (f)	NO <sub>3</sub> -N (mg/L)	NO <sub>2</sub> -N (mg/L)	NO <sub>2</sub> /NO <sub>3</sub>	COD (g/L)
13.25±0.1	1025±50	2860±50	2.8±0.1	18±5

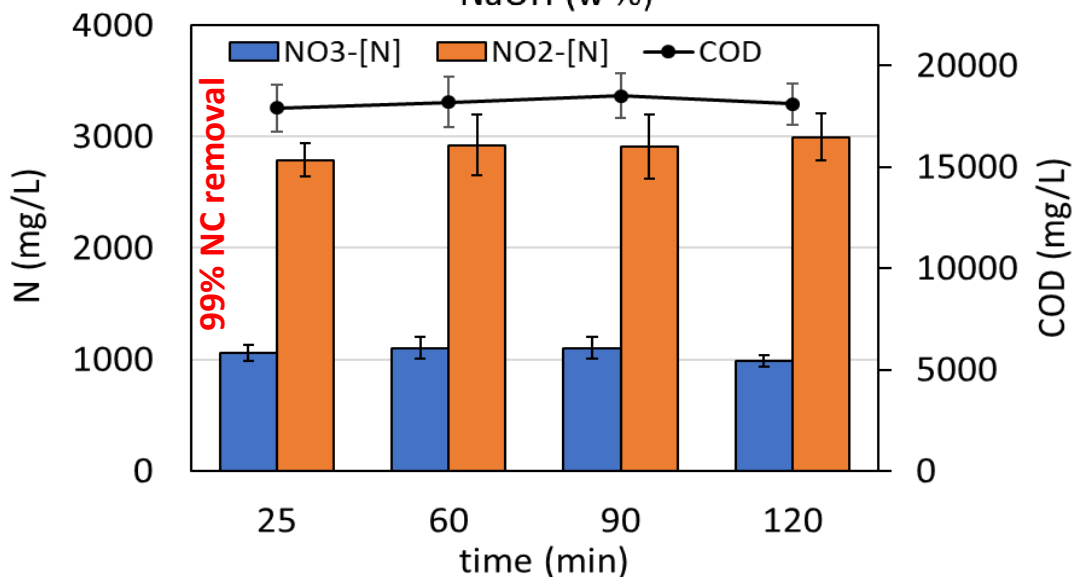


# Characterization of post-AH NC liquor



## Effect of caustic strength

- Fix NCw 3%
- Fix T (90 C)



## Effect of AH time

- Fix NaOH 3%
- Fix T (90 C)
- Fix NCw 3%

# Alkaline hydrolysis (AH): parametric study



## Pilot scale testing

### ***USA Lab-30FS reactor***

- Condenser with collection flask
- T monitor and mix controller
- 30 L volume reactor vessel
- Working volume 10 L
- mixing speed fixed to  $180 \pm 5$  rpm

*Testing conditions  
with pure NC fines*

Parameter	Value
Temperature (C)	90, 70
NaOH (%)	3
NC (%)	3





# AH pilot scale for NC(p) fines



***T=5 min***

***T=30 min***

***T=1 h***



Parameter	Value
Temperature (°C)	<b>70</b>
Time (min)	60
NC removal	99%
COD (mg/L)	19010

***T=5 min***

***T=15 min***

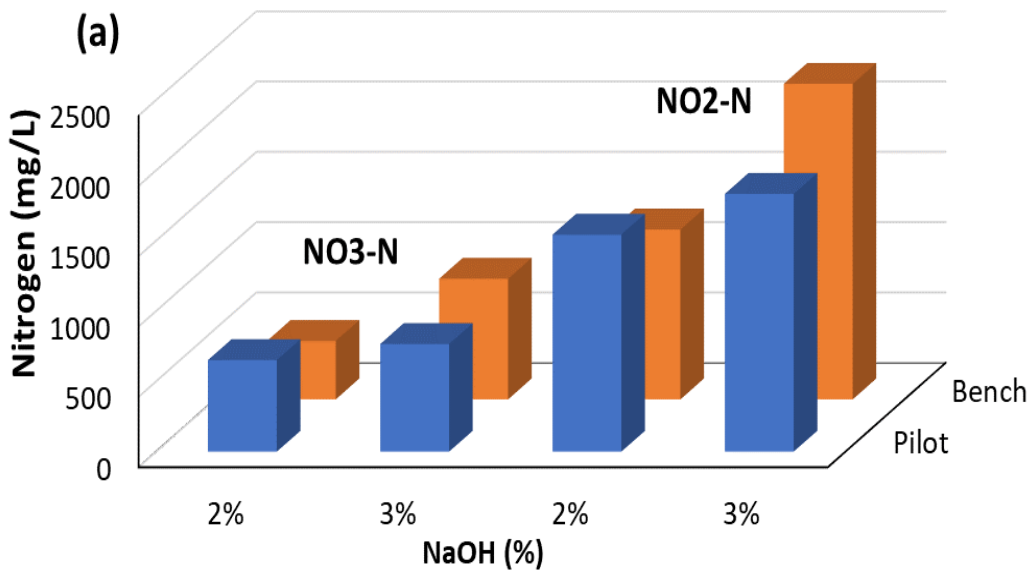
***T=25 min***



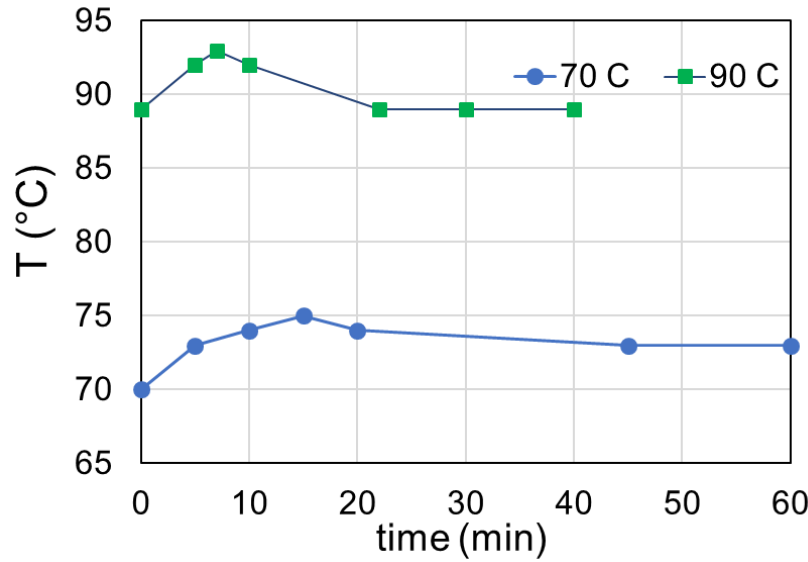
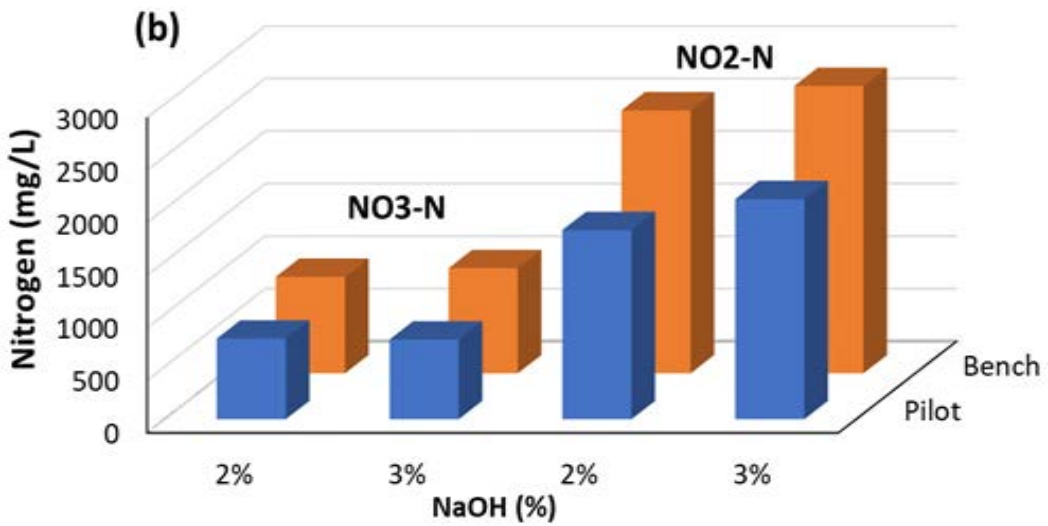
Parameter	Value
Temperature (°C)	<b>90</b>
Time (min)	30
NC removal	99%
COD (mg/L)	19500



# AH pilot scale for NC fines



Nitrate and nitrite concentrations as nitrogen from bench and pilot scale tests at (a) 70 °C and (b) 90 °C







# AH kinetic study

## Summary

- AH is confirmed effective in degradation of targeted NC fines from wastewater
- NC: NaOH solids ratio of 1:1 at 90 °C will achieved 99% destruction within 30 min
- An equation for modeling of NC fines degradation was obtained using non linear regression and pseudo first order approximation
- Higher temperature play a significant role in enhancing kinetic rate of reaction compared to caustic strength
- Optimal conditions from bench scale tests compare well with outcomes from AH tests at larger scale

$\text{NO}_3\text{-N}$ (g/L)	$\text{NO}_2\text{-N}$ (g/L)	COD (g/L)
1.02±5	2.86±5	18±5

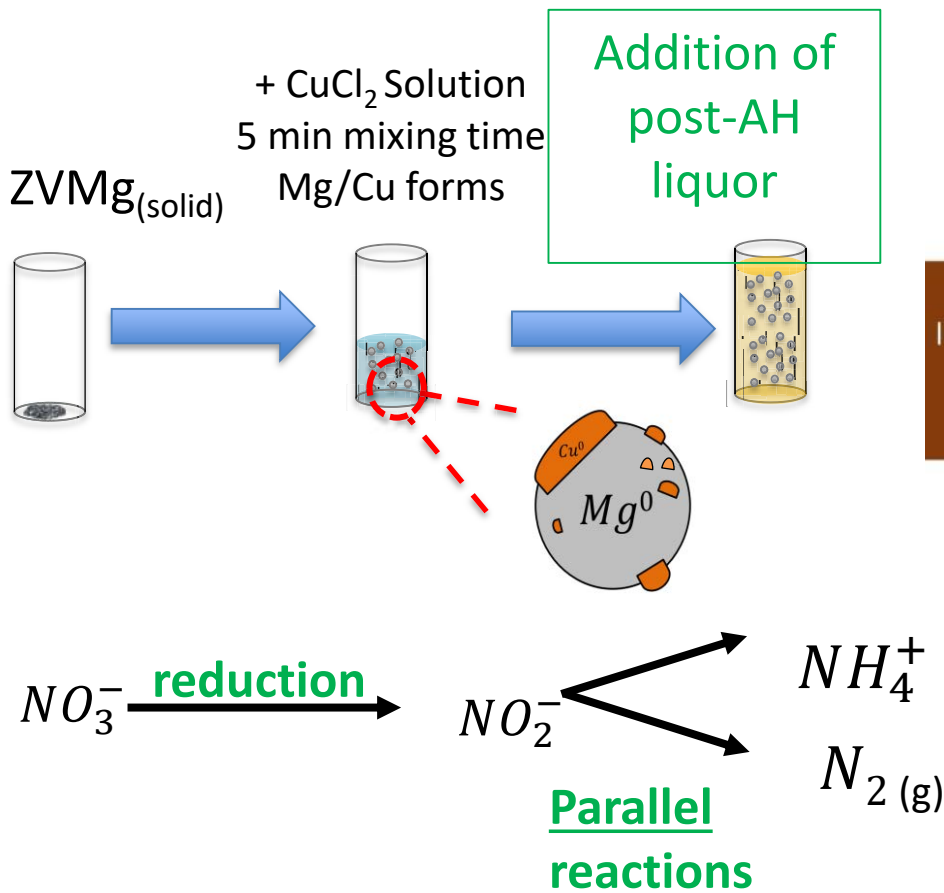
*How to address nitrogen and COD in post-hydrolysis liquor?*

# Nitrogen removal in post-AH NC liquor



## Physicochemical process

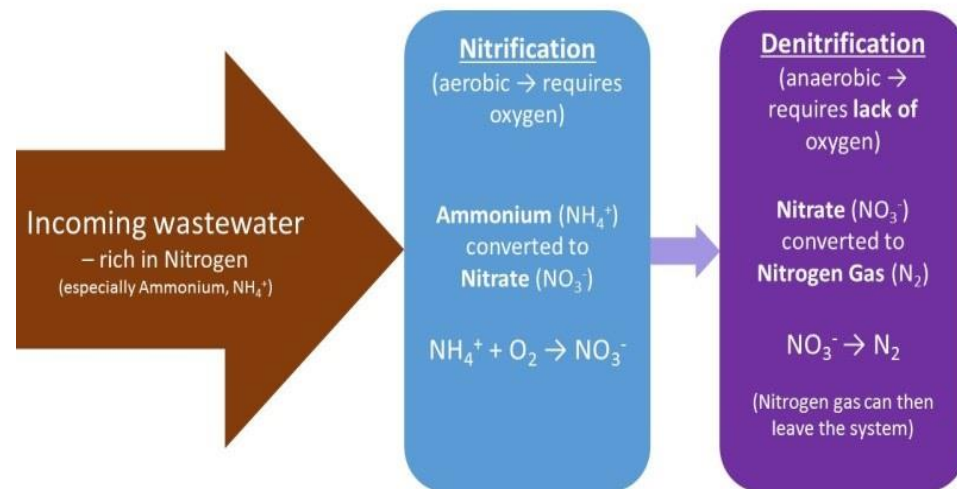
### Bimetal reduction



## Biological process

### Heterotrophic denitrification (HDN)

#### Nitrogen removal in wastewater treatment plants



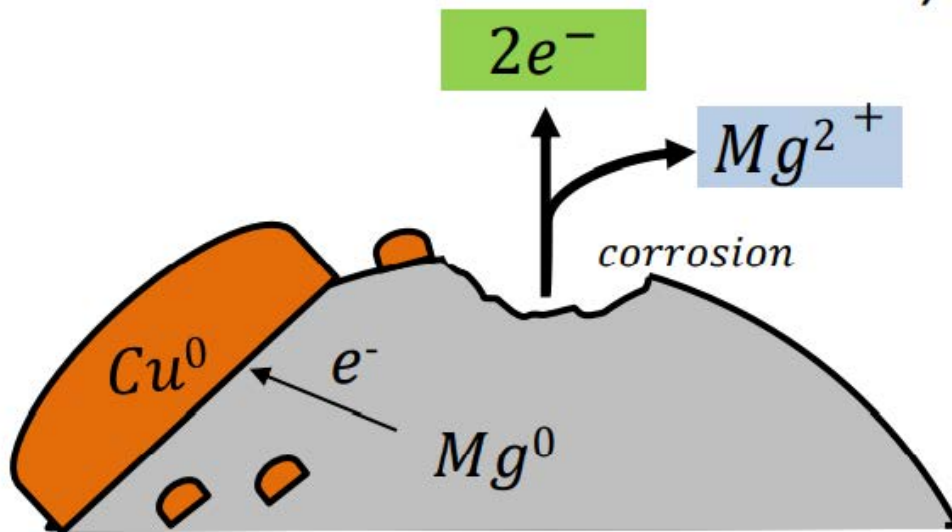


# Bimetals reduction for post-AH liquor

- Zero valent iron (ZVI) widely used for environmental remediation
- Process enhanced by
  1. metals with higher reduction potential (Mg)



2. Bimetals contact (galvanic corrosion)



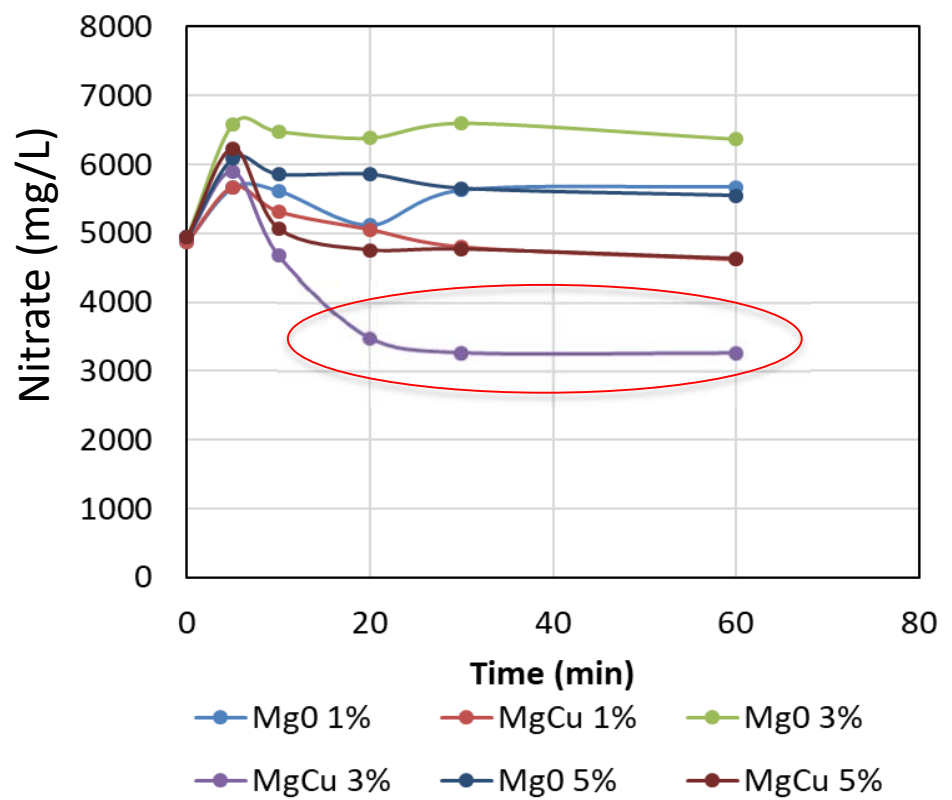
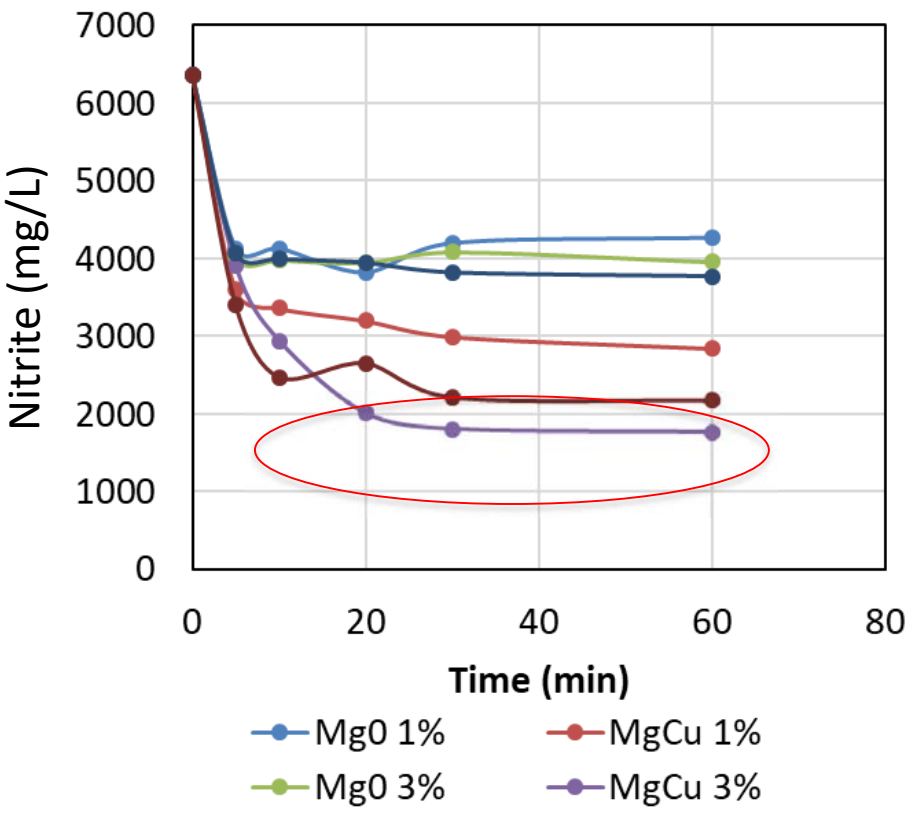


# Bimetals reduction for post-AH liquor

Testing Conditions:

- ZnMg only
- Mg/Cu at 10:1 ratio
- Initial pH of post-AH liquor adjusted to  $\leq 2.0$

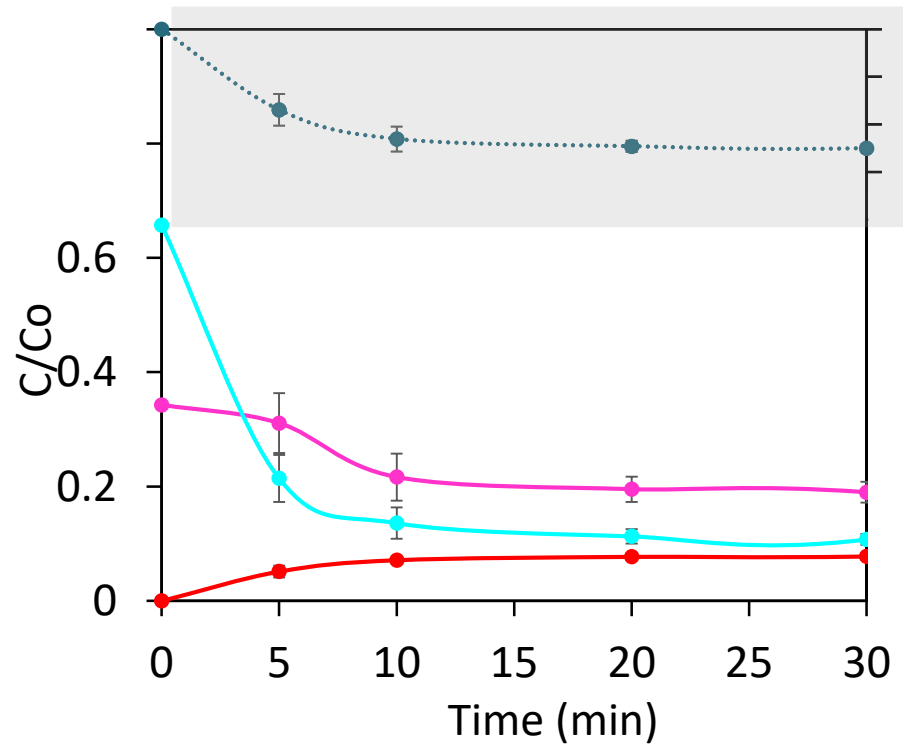
*Solids to liquid (S/L) percentages ratio 1-5%*



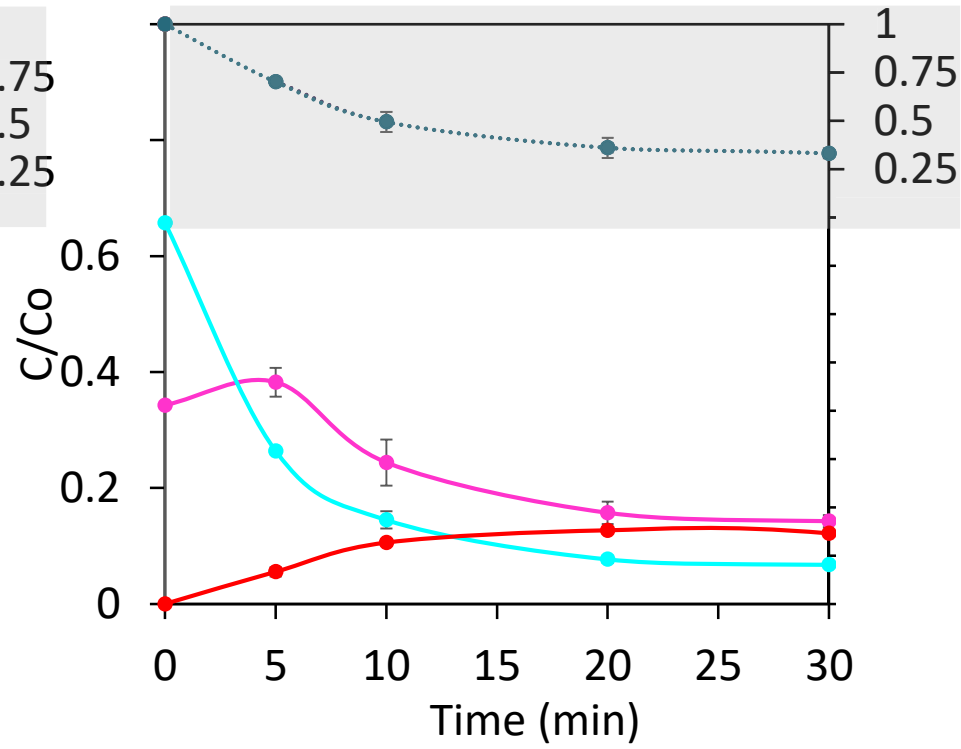


# Bimetals reduction for post-AH liquor

Nitrogen removal from post-AH liquor at 3% S/L



**Undiluted AH liquor**



**2x Dilution AH-liquor**

.....●..... Total N    ●— NO<sub>3</sub>-N    ●— NO<sub>2</sub>-N    ●— NOH<sub>3</sub>-N

Nitrogen removal from post-AH liquor at 60-70%



# Bimetals reduction for post-AH liquor

COD removal from post-AH liquor at 3% S/L

Target AH liquor	Dilution AH liquor	% COD Removal
AH-liquor from NC(p)	2X	77.5
	4X	79.1
AH-liquor from NC(w)	2X	83.0



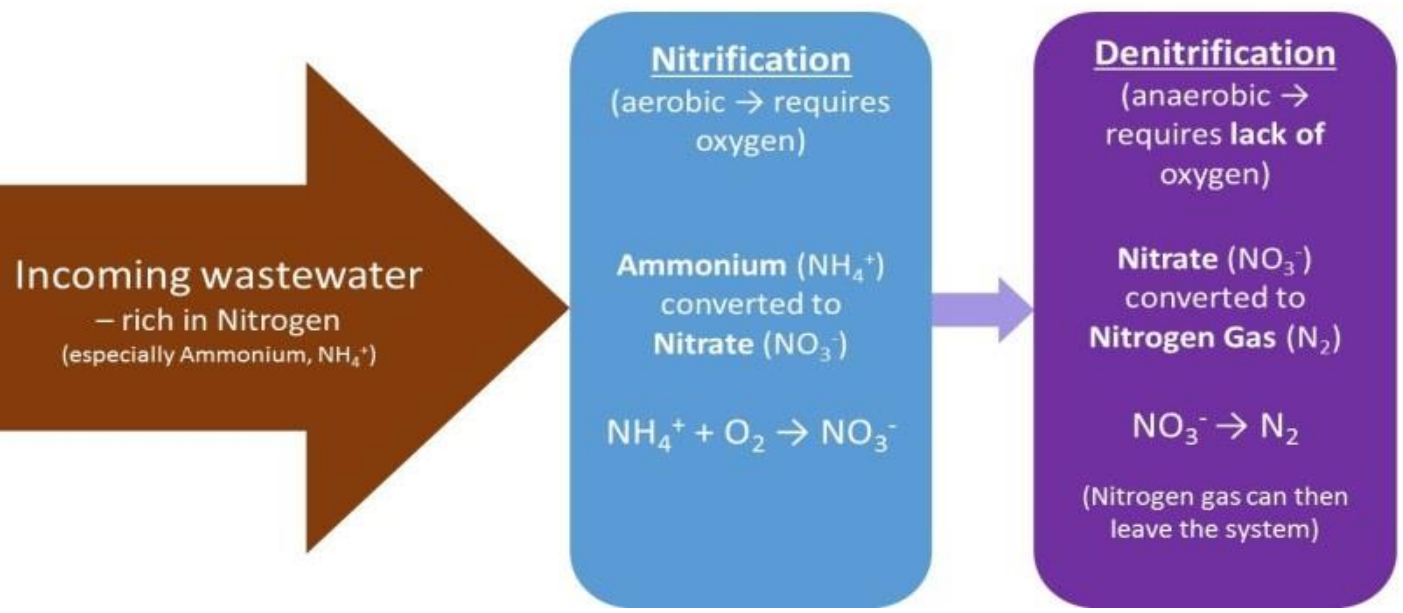
post-AH liquor before and after treatment with Mg/Cu





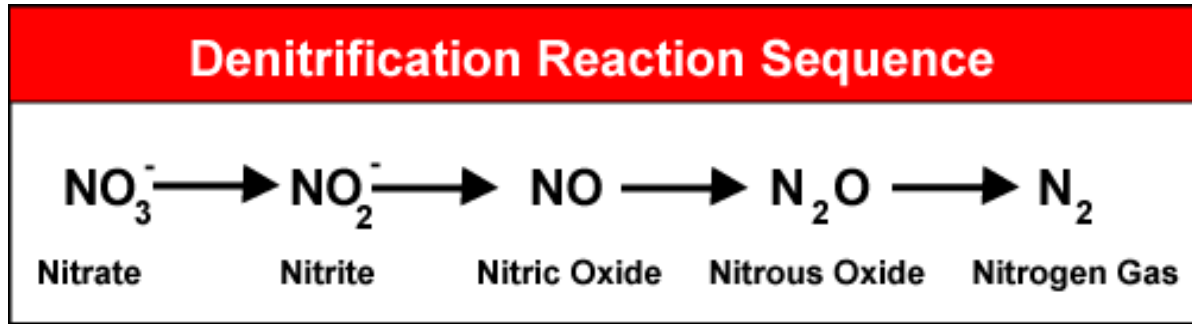
# Heterotrophic Denitrification (HDN) of post-AH liquor

Nitrogen removal in wastewater treatment plants



Dissolved Oxygen  $\leq 0.5 \text{ mg/L}$

*In anoxic environment, heterotrophic bacteria will use the oxygen from nitrates as they assimilate BOD, producing nitrogen gas.*





# HDN of post-AH NC liquor

## *Requirements for HDN*

- Biochemical Oxygen Demand (BOD)/ to nitrous oxygen (NO<sub>x</sub>-[N]) of min 2.5-max 5
- A COD/BOD ratio  $\leq 2$
- 99% transformation of 3% NC solids generate about 3800 mg/L of NO<sub>x</sub>-N
- Identify BOD/NO<sub>x</sub>-N and COD/BOD ratios in post-hydrolysis NC liquor

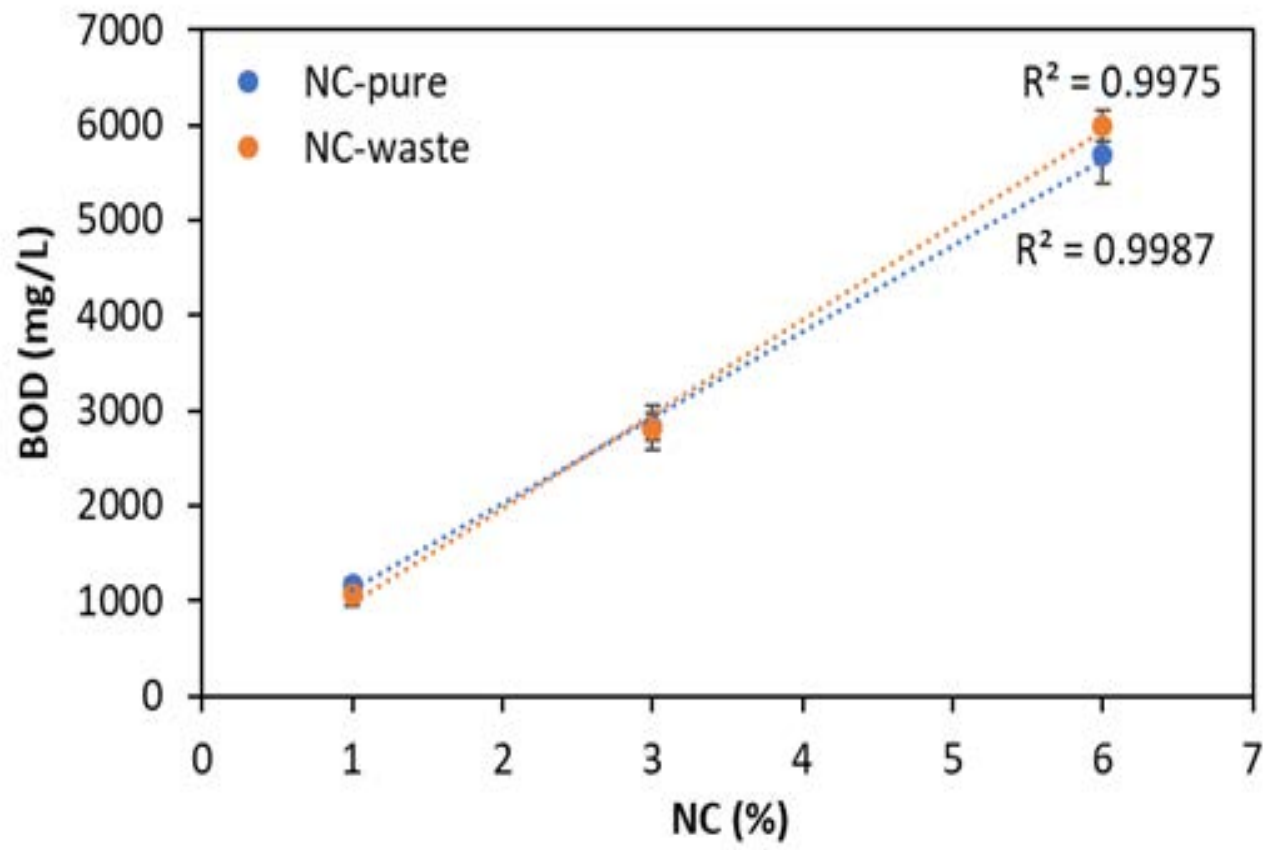
NC (w) %	COD (g/L)	$\Sigma$ NO <sub>x</sub> -N (g/L)
1	6.82	1.50
3	16.8	3.73
6	32.1	6.09
NC (p) %	COD (g/L)	$\Sigma$ NO <sub>x</sub> -N (g/L)
1	6.20	1.50
3	16.2	3.73
6	29.9	6.09

*Characterization  
of post-AH liquor  
for different NC  
%*



# BOD in post-AH NC liquor

*BOD vs NC fines %*



AH of NC fines yield of 1000 mg BOD/g NC hydrolyzed



# HDN of post-AH NC liquor

## *BOD Requirements for HDN*

- Based on BOD assessment and characterization of post-AH liquor

NC (w) %	COD/BOD	BOD/ $\Sigma$ NO <sub>x</sub> -N
1	5.79	0.78
3	5.94	0.76
6	5.65	0.93
NC (p) %	COD/BOD	BOD/ $\Sigma$ NO <sub>x</sub> -N
1	5.81	0.78
3	5.75	0.85
6	4.99	0.99

- Ratios for NC(w) do not meet the standard criteria for HDN
- In WWTP, HDN is downstream to aerobic treatments
- Addition of organic carbon to sustain HDN is common
- Methanol selected for external supply to post-AH liquor

# HDN experimental set up



## *Winpact Evo System Controller and bioreactor*

30 L reactor capacity, recirculation jacket with heating/cooling system; online DO, pH, ORP probes with online pH adjustment

Operating Parameter	Value
Temperature (C)	30
AH liquor dilution	8x
Flow (L/d)	8
Working volume (L)	15
HRT (d)	1.8
Total Influent N (mg/L)	430±10
Influent NO <sub>2</sub> -N (mg/L)	323±5
Influent NO <sub>3</sub> -N (mg/L)	107±10



# HDN of post-AH liquor

*Operating conditions by influent nitrogen*

Phase	Influent Nitrogen progression	Time (d)
1	100% NO <sub>3</sub> synthetic solution	8
2	25% NO <sub>3</sub> , 75% NO <sub>2</sub> synthetic solution	8
3	Diluted AH liquor (8X) from NC(p)	20

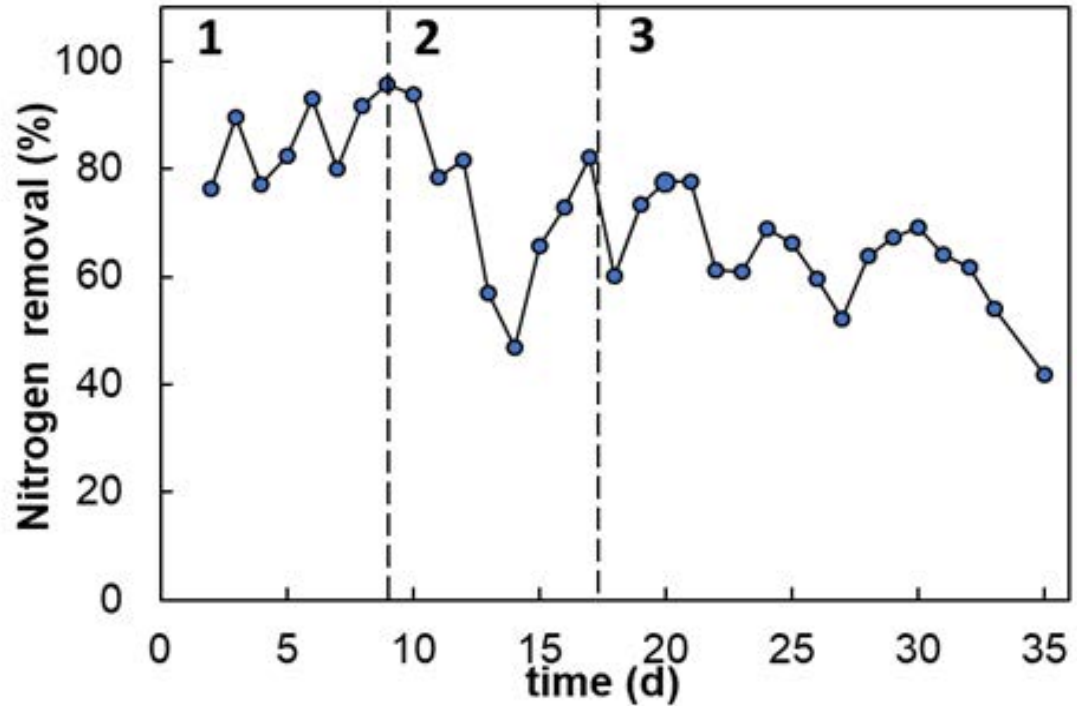


*Activated Sludge from local wastewater treatment plant (Bergen County Utility Authority) utilized as initial inoculum acclimated for a period of 2 weeks*





# HDN of post-AH NC liquor

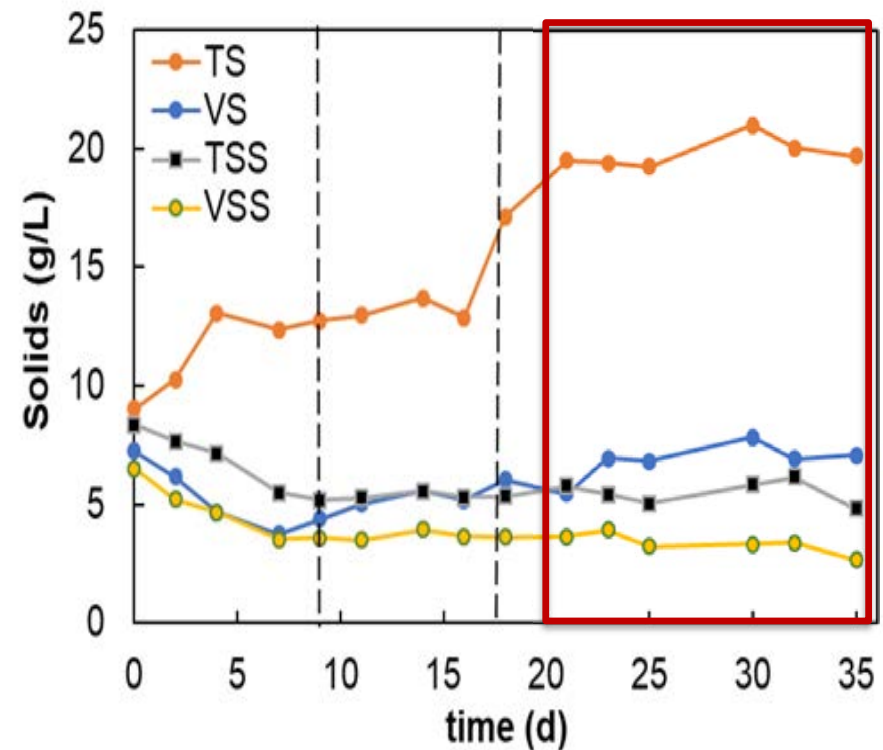
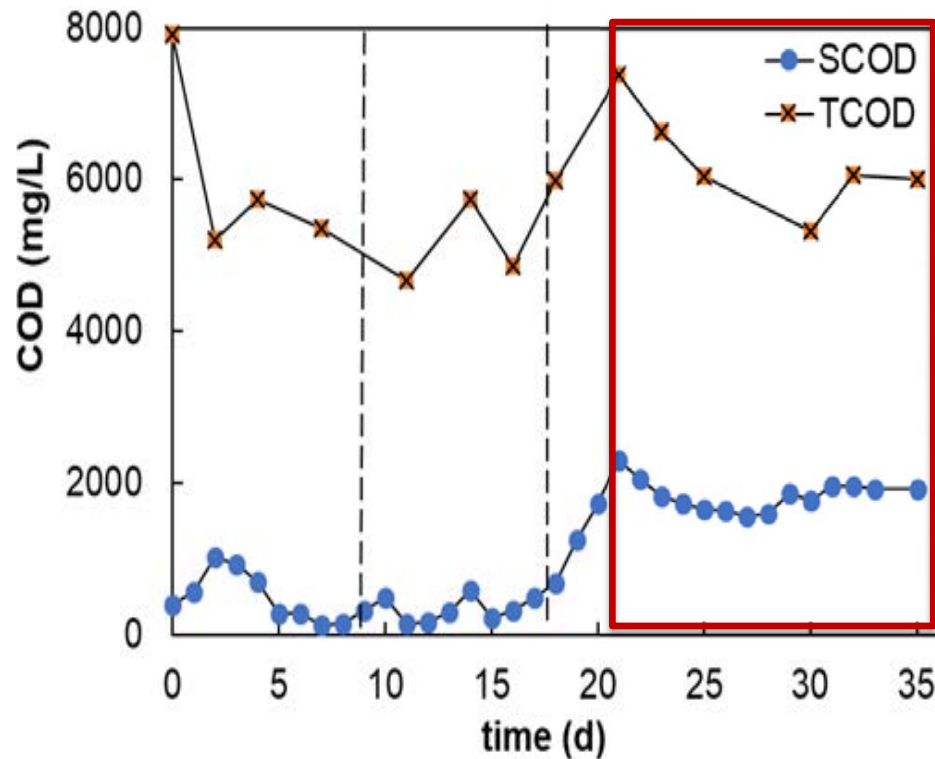


## Average performance parameters

- Avg MLVSS (g/L) 1.81±0.05
- Avg TSS/VSS ratio 0.50
- Avg COD removal 57%
- Avg N removal 60%

Phase	Influent Nitrogen progression	Time (d)	Supplied MeOH (mg/L)	Influent pH
1	100% NO <sub>3</sub> synthetic solution	8	1060	7.55
2	25% NO <sub>3</sub> , 75% NO <sub>2</sub> synthetic solution	8	765	7.60
3	Diluted AH liquor (8X) from NC(p)	20	460	8.40

# HDN of post-AH NC liquor



- Inhibition of denitrifiers activity over time
- Decline of COD removal
- Gradual decline in VSS which indicate biomass loss
- Induced toxicity may derive by synergistic effect between salts accumulation and COD in post-AH liquor

# Comparison of Nitrogen removal in post-AH NC liquor



## *Summary and conclusions*

- Bimetals reduction and HDN were both effective in reducing the concentrations of nitrate and nitrite in the post-AH liquor
- Both processes required dilution of initial AH-liquor due to COD and nitrogen overload
- Reduction with bimetal (Mg/Cu) achieved higher inorganic nitrogen and COD removal ( $\geq 70\%$ ) with less dilution and faster kinetic compared to HDN ( $\leq 60\%$ )
- Bimetals obtained also de-coloration of AH liquor (i.e. clear color)
- Denitrifies bacteria in HDN process showed toxicity inhibition from AH-liquor which may result in higher complications for large scale applications



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attention!**

**Questions?**