



# Tighe&Bond

Engineers | Environmental Specialists

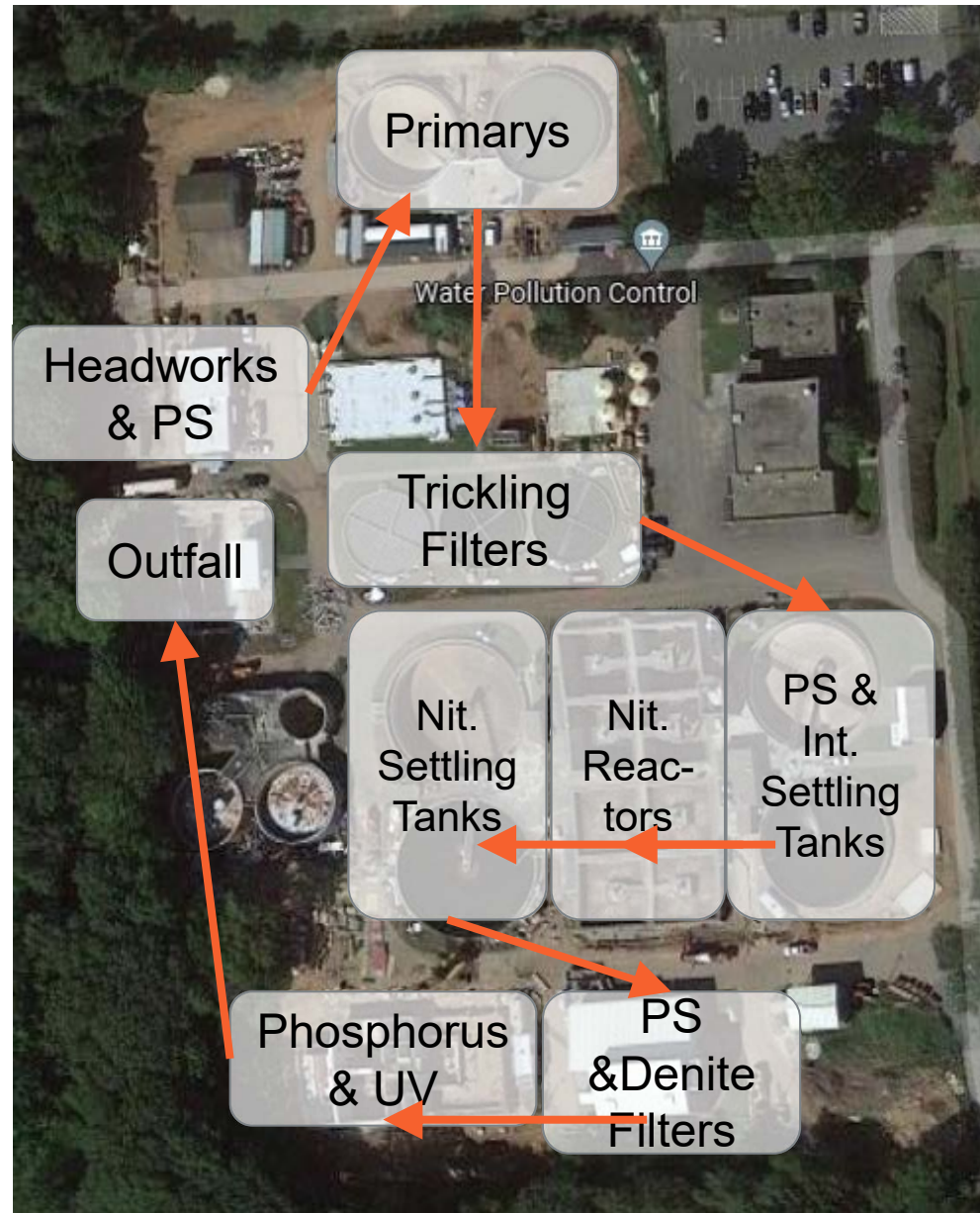


## **LESSONS LEARNED INSTALLING AND STARTING-UP THE COMAG PROCESS FOR LOW LEVEL PHOSPHORUS REMOVAL AT THE SOUTHINGTON CT WPCP**

**NEWEA Annual Conference – January 25, 2022 (Session 20)**

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# PLANT OVERVIEW - LIQUID TREATMENT



# SOUTHINGTON WPCF

- **Design Capacities**

- Design Average Daily Flow 7.4 mgd
- Design Peak Hourly Flow 15.9 mgd

- **Drivers for Upgrade**

- Aging Equipment (most from early 1980s)
- Odor Control
- Phosphorus Limits
  - Seasonal – April 1 through October 31
  - Interim Limit - 0.7 mg/L (2013)
  - Final Limit (April 2022)
    - 7.53 lbs./day, Equivalent to
    - <0.2 mg/L at current ADF of 4.5 mgd
    - <0.12 mg/L at design ADF of 7.4 mgd



# SOUTHINGTON WPCF UPGRADE

- **Construction**

- Construction Cost of ~\$40 M
- Notice to Proceed - January 2019
- Substantial Completion - April 2021

- **Funding**

- Clean Water Fund
  - 50% grant (low level phosphorus removal)
  - 30% grant (nutrient removal)
  - 20% grant (other costs)
  - Loan
- Energy Utility Rebate Incentive



**EVERSOURCE**

# PHOSPHORUS TECHNOLOGY SELECTION



## Facilities Plan 2014

Technologies were screened through workshops with the town using a ranking process, from several to the top three:

- Ballasted Flocculation
- Disc Filters
- Deep Bed Sand Filters



## Technology Scoring

Ballasted Flocculation scored most favorable for:

- Present Worth Cost
- Ease of Operations
- Existing Installations (at the time)
- Low Return Flow Rates
- Seasonal Shutdown Flexibility



## Redundancy

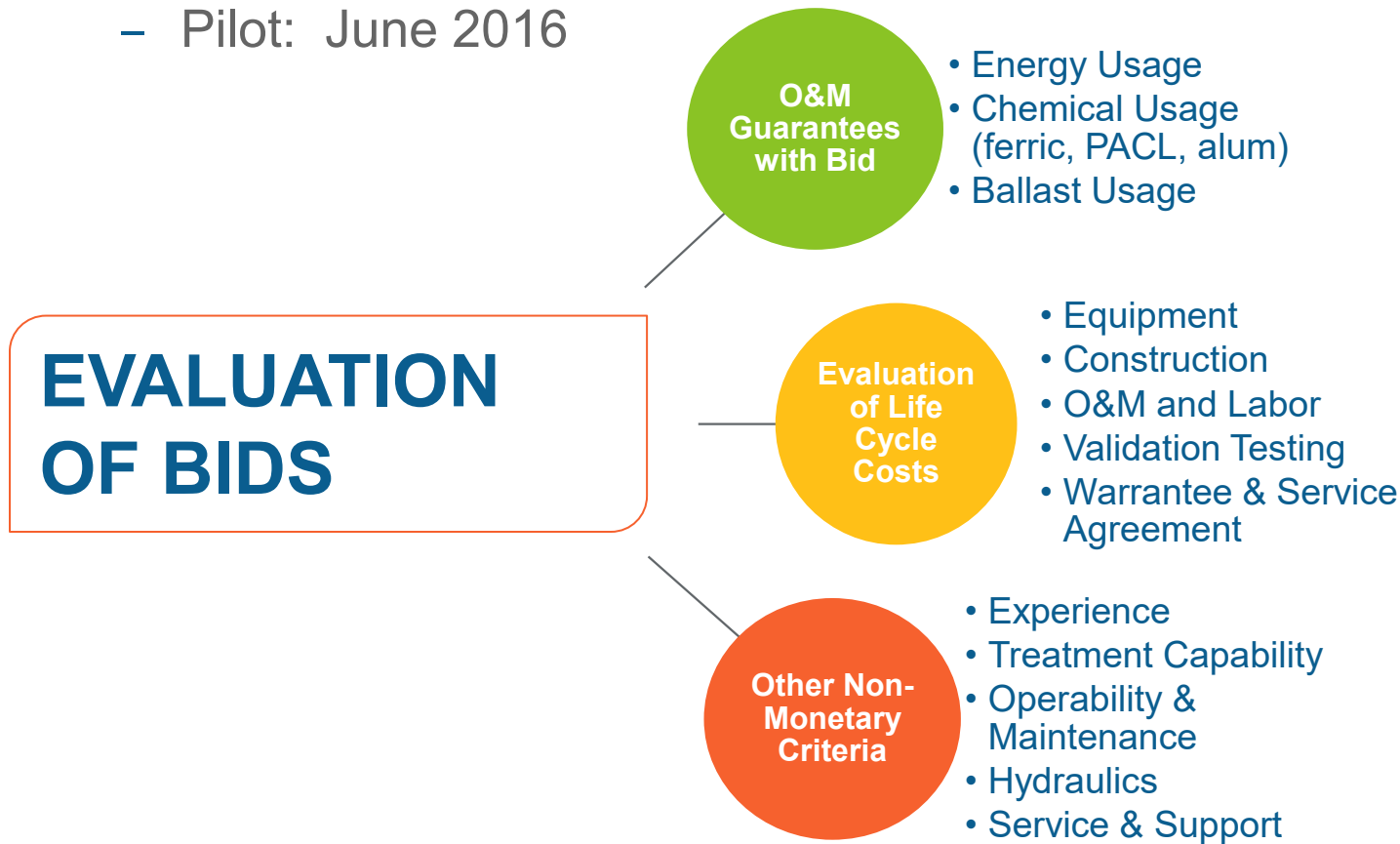
For Seasonal System

- Two Full Duty Trains,
- Other installations visited had 1 train of reactors and 2 trains of clarifiers

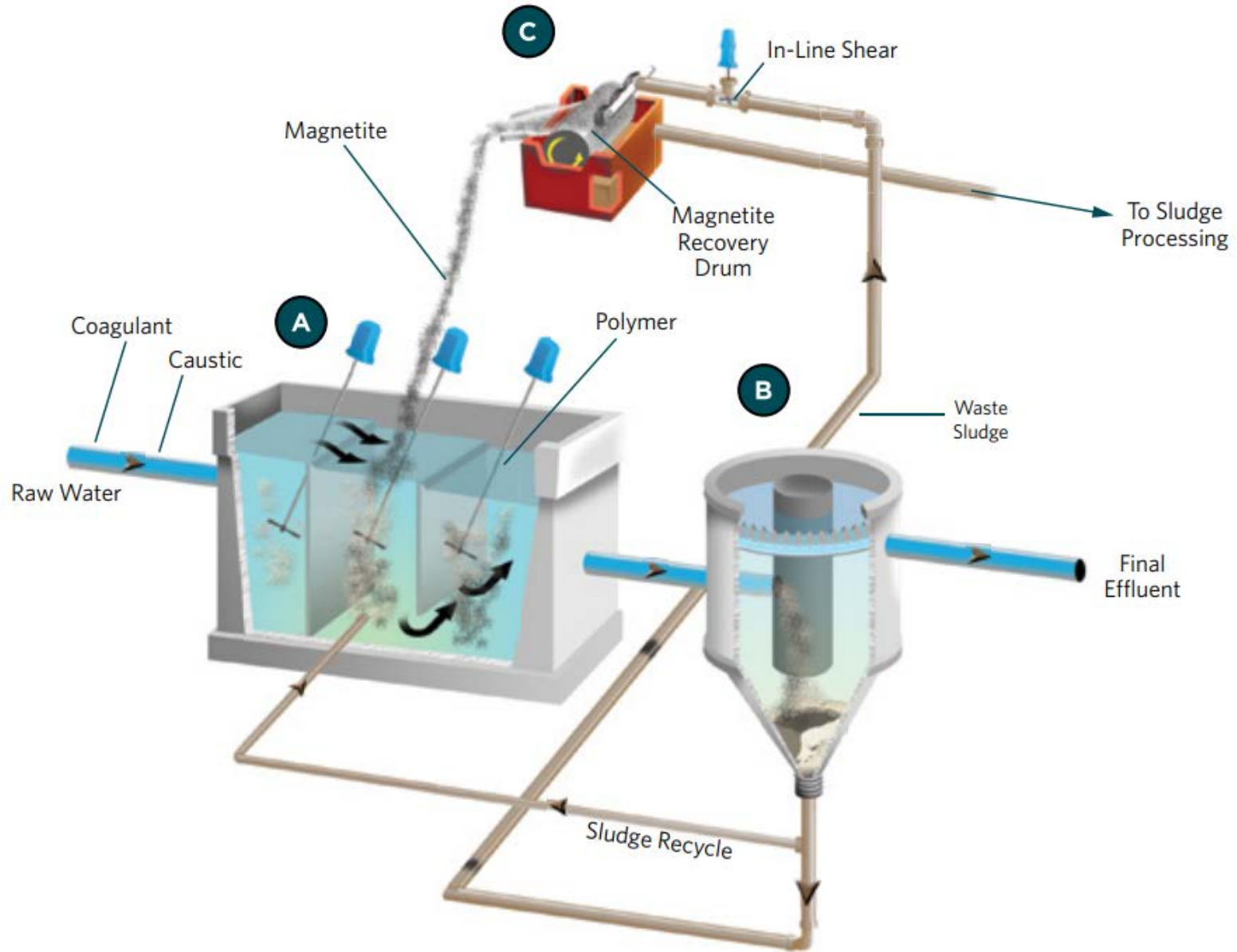
# PRE-PROCUREMENT

- **Public Bidding**

- Request for Proposals: December 2015
- Bid Opening: January 2016
- Notice of Award: March 2016
- Pilot: June 2016



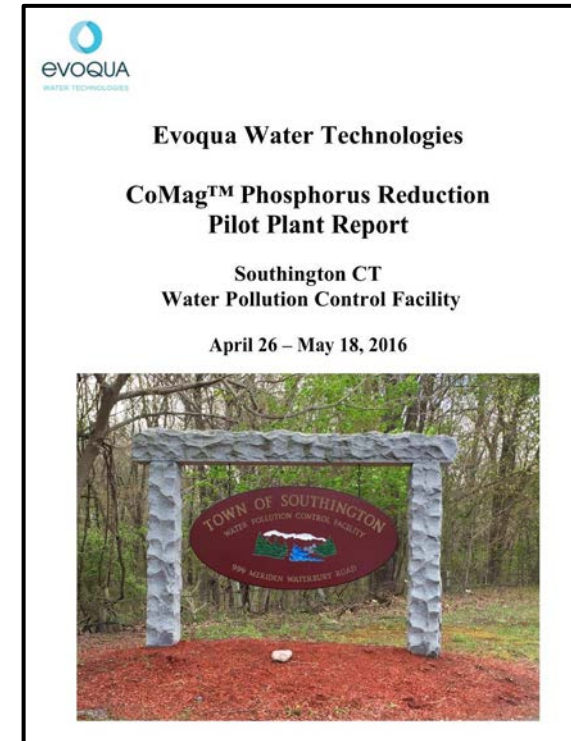
# COMAG PROCESS OVERVIEW





# BIDDER VALIDATION TEST - GOALS

- **Prove System Performance Guarantee**
  - Effluent P
  - Loading Rates
- **Prove System O&M Guarantees**
  - PACL Usage
  - Alum Usage
  - Ferric Chloride Usage
  - Energy Usage
- **Will Soluble Non-Reactive Phosphorus (SNRP) interfere with performance?**



# BIDDER VALIDATION TEST – LESSONS LEARNED

- **Chemical Performance**

- PACL – Did not perform (High usage) ✗
- Alum and Ferric – did perform ✓ ✓
- Re-evaluated Bids – CoMag still first choice

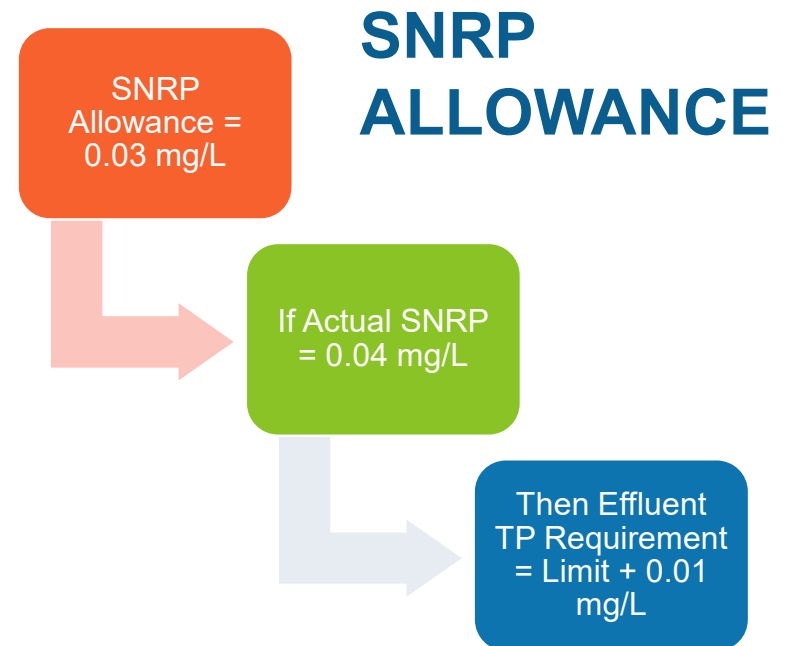


- **Design Plan – Chemical Feed**

- Design for any Chemical
  - Future Aluminum limits?
  - Corrosivity of Ferric drove material selection
- Multi-point (PACL – same as temporary system)
- CoMag (likely Alum – Owner’s preference)

# SOLUBLE NON-REACTIVE PHOSPHORUS (SNRP)

- SNRP = Soluble Total P – Soluble Ortho-P
- **Concerns**
  - Cannot be removed via treatment
  - Interim systems would for no apparent reason struggle to meet 0.7 mg/L for a week or two each summer (unknown reasons) –Was this due to SNRP?
- **Solutions:**
  - Build “Allowance” in Design Criteria
- **Lessons Learned:**
  - SNRP Not a factor in Jar Tests (winter), Pilot (early summer) or Startup (2021 Season)



# LESSONS LEARNED - DESIGN

- **Plan:**

- Gravity from Upflow Denite Filters to CoMag (and relocated UV)
- 15.9 MGD “Denite Pump Station & Filters Work Great”



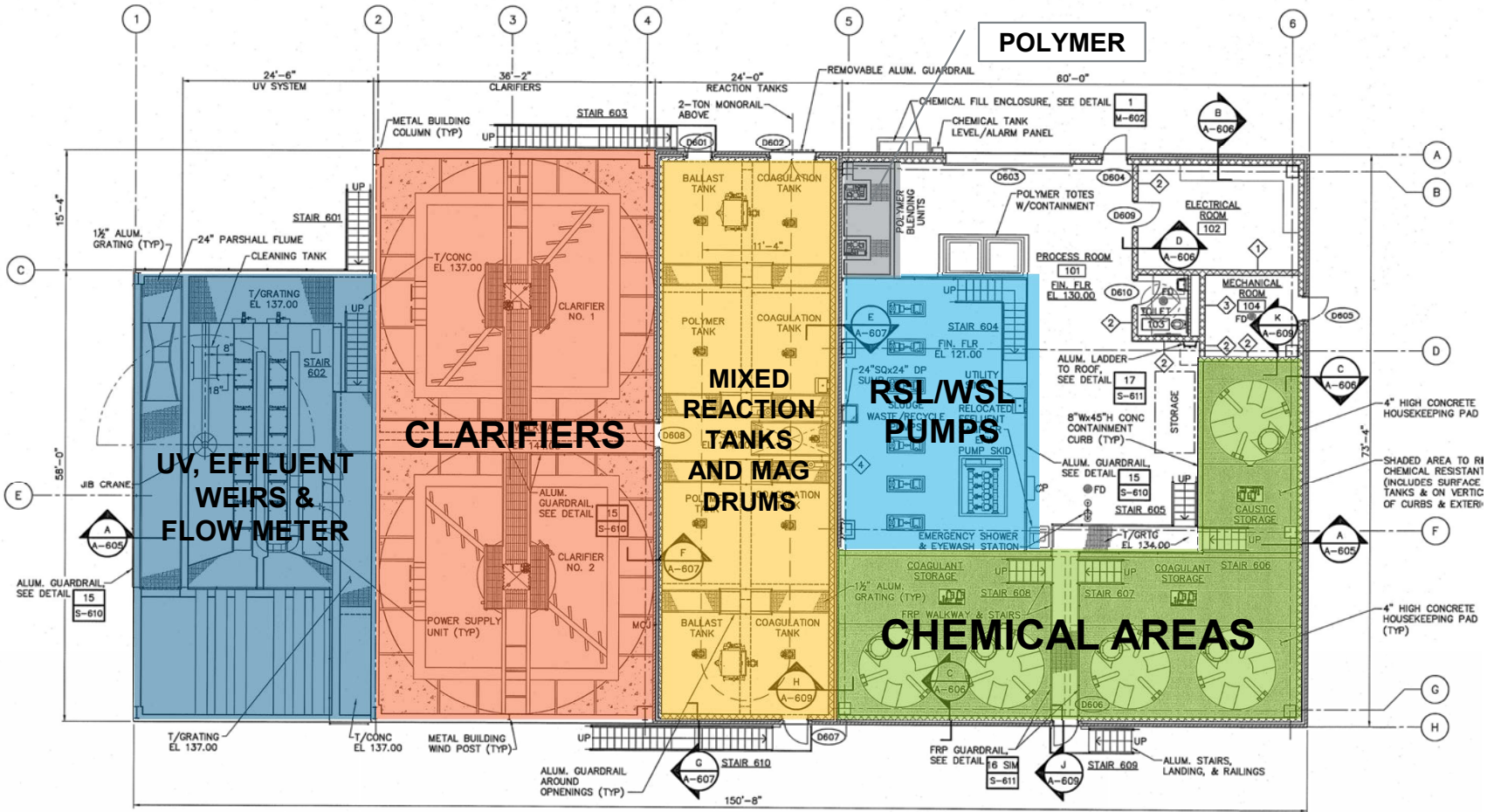
- **Learned:**

- Filters were only passing 10-12 MGD
- At High Flows - Operators shutting down & bypassing (to old UV)

- **Solution:**

- Get IDI/Suez Mfg Onsite – re-train (new) operators (12-14 MGD)
- Add a bypass around filters (to get >16 MGD)
- Denite PLC Code Improvements (over 6+ years)

# LESSONS LEARNED: CONSTRUCTION



# LESSON LEARNED: CONSTRUCTION

- **Schedule**
  - CoMag Bid – Jan 2016
  - Construction Start – Jan 2019
  - First CoMag Submittal – July 2019
- **Surprise – Pump Design Change**
  - Changed pumping design from 10% to 5% of plant's ADF
    - Act Fast – Pipe being laid soon!
- **Impacts**
  - Lower Flows means Smaller Pipe Sizes to suspend solids.
  - Revisit Pump Sizing & HP



# LESSONS LEARNED: START-UP

- **Plan:**

- Break-in-period required before performance testing CoMag
  - Troubleshoot equipment
  - Stabilize chemicals (magnetite levels, multipoint dosing)
  - Operator learning curve



- **Issue - Nitrification Reactor Upset**

- Loss of solids in nitrification reactors
- Drain valve left open – unintended wasting
- Delayed Testing for 1 month

# LESSONS LEARNED: START-UP



- **Issue - Denite Pump Station & Filters**

- Effluent Flow oscillations
  - 18 min. cycle
  - +/- 50% variation (e.g., 3-9 MGD)
- Not trended in Denite SCADA system
- New information:
  - Visible at CoMag weirs
  - New effluent flow meter

- Ruled out surging air in inverted siphon feed pipe
- Required PLC modifications



# LESSONS LEARNED: START-UP

- **Issue – Siphon Effect**

- Pipe returning solids to reaction tanks had an 18-foot drop
- Pump design had to assume no siphon effect – free fall in 4" drop pipe.
- Pump startup demonstrated siphon effect was maintained over wide range of flows – reducing energy costs

Return Sludge Piping above



Reaction  
Tanks  
Below

# PERFORMANCE TESTING GOALS

- **Meet Effluent Requirements**
  - TP < 0.1 mg/L (with O&M guarantees)
  - TP < 0.05 mg/L (potential future limit)
- **Meet O&M guaranteed values**
  - Chemical (Only Alum Tested)
  - Energy
  - Magnetite, plant water consumption, & waste solids flow

## Operations and Maintenance Guarantee

Parameter	Unit	Target Value
Average, 48% solution alum dosage	ppmvp	60
Average polymer dosage	ppmvp	2.6
Power Consumption	kWh/d	861
Average magnetite (ballast) usage	lb/d	45

# PERFORMANCE TESTING

- **Performance Testing Plan**
  - 28-day test
  - Four full-scale operating conditions
- **Process Adjustments**
  - Coagulant, magnetite, polymer
  - Flow split to parallel trains (1 or 2 online)
- **Effluent Requirements**
  - TSS, Turbidity, Total Phosphorus, pH

# PERFORMANCE TESTING

- **Overall Results**

- Two sets of effluent performance requirements Met
  - All 4 conditions
  - All Criteria (TP, TSS, Turbidity)
  
- O&M Guaranteed Values Met
  - Treating to TP<0.1 mg/L
  - Power, chemical, plant water use, magnetite



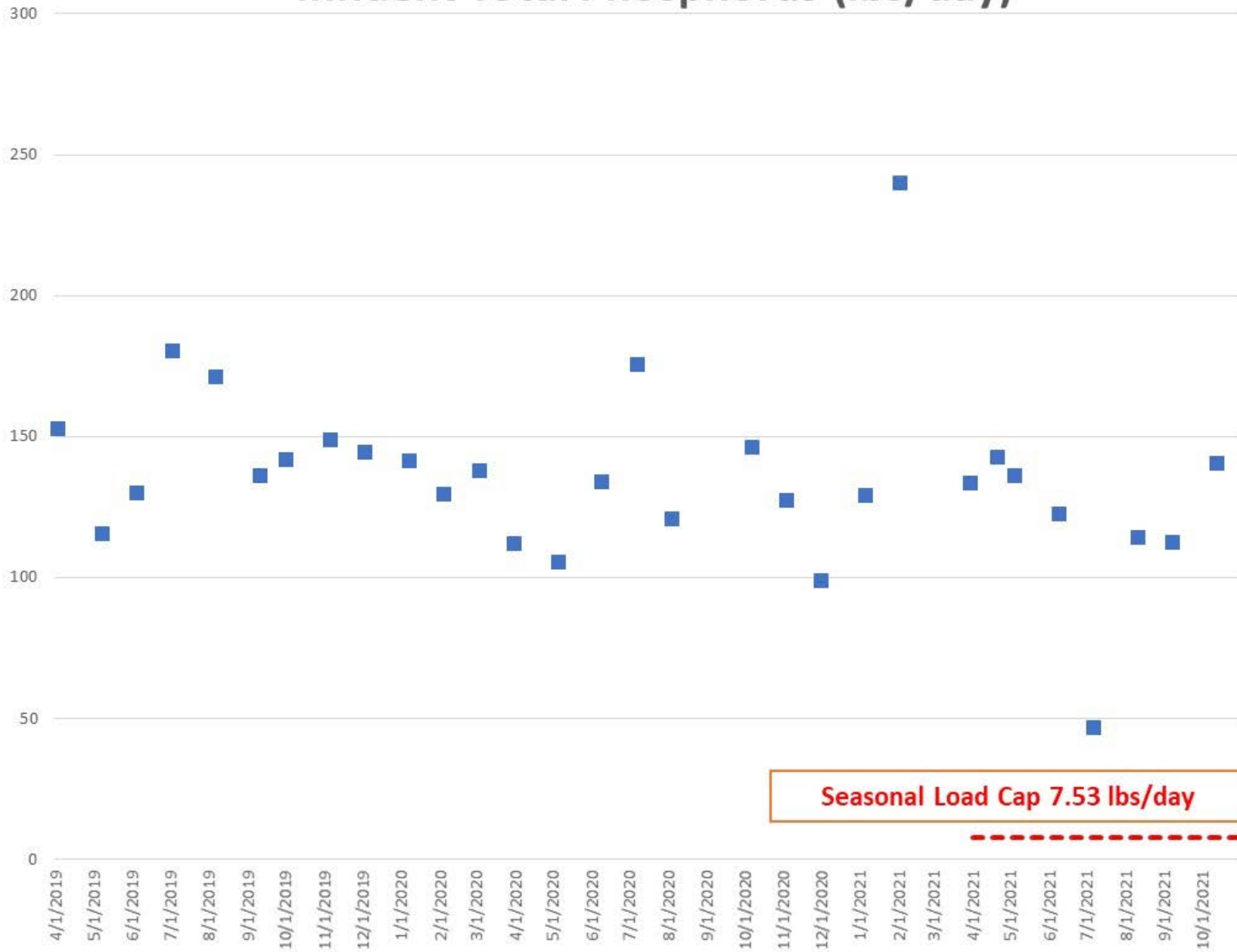
- **Notes**

- Some data was not considered (process upsets)
- Process responded quickly to upsets (polymer shut-downs)
- Return Sludge Pumping - Typically ran @ 2-3% of Plant ADF (energy usage well below guarantee)

# IMPACT ON PLANT OPERATIONS



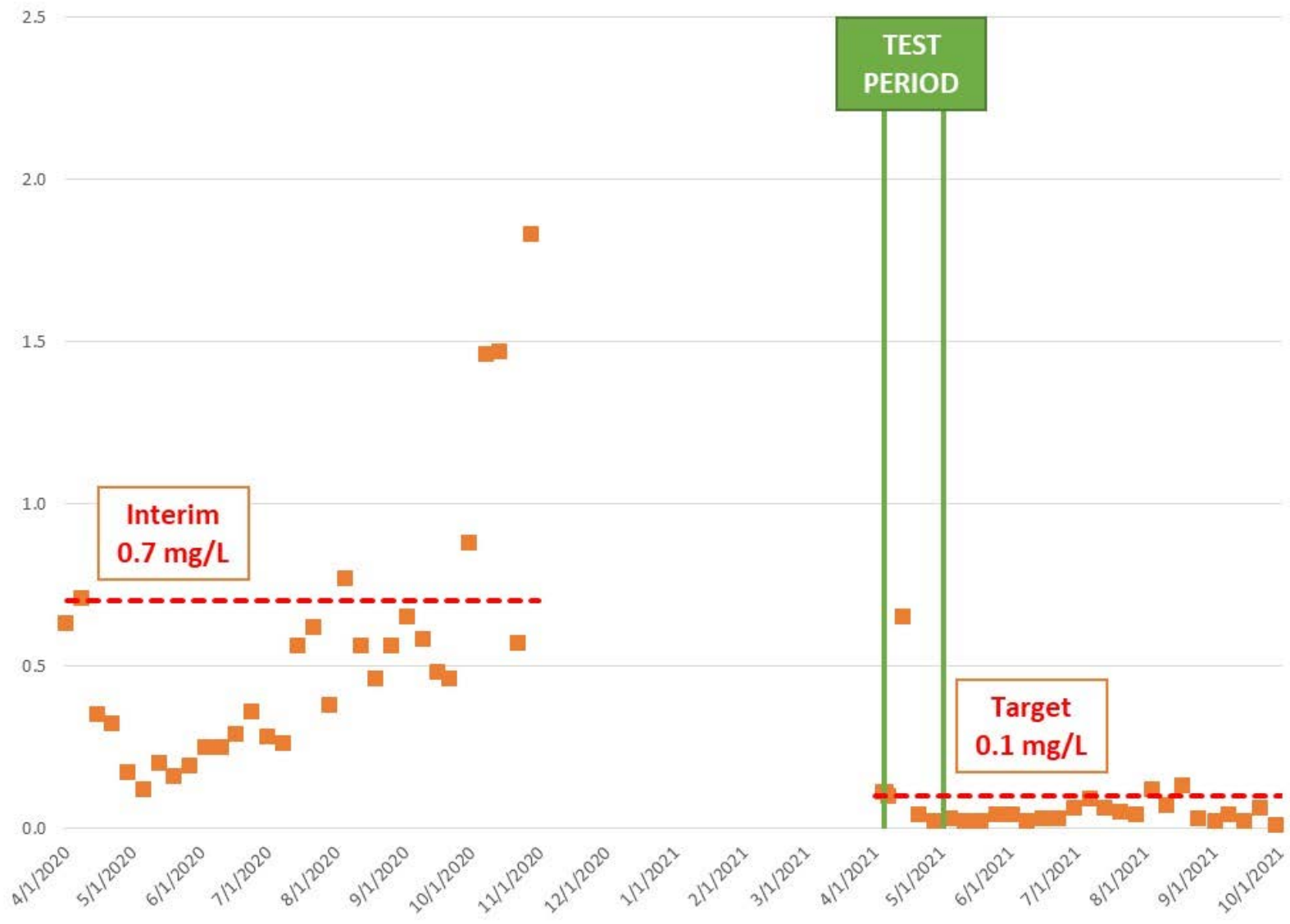
# Influent Total Phosphorus (lbs/day)



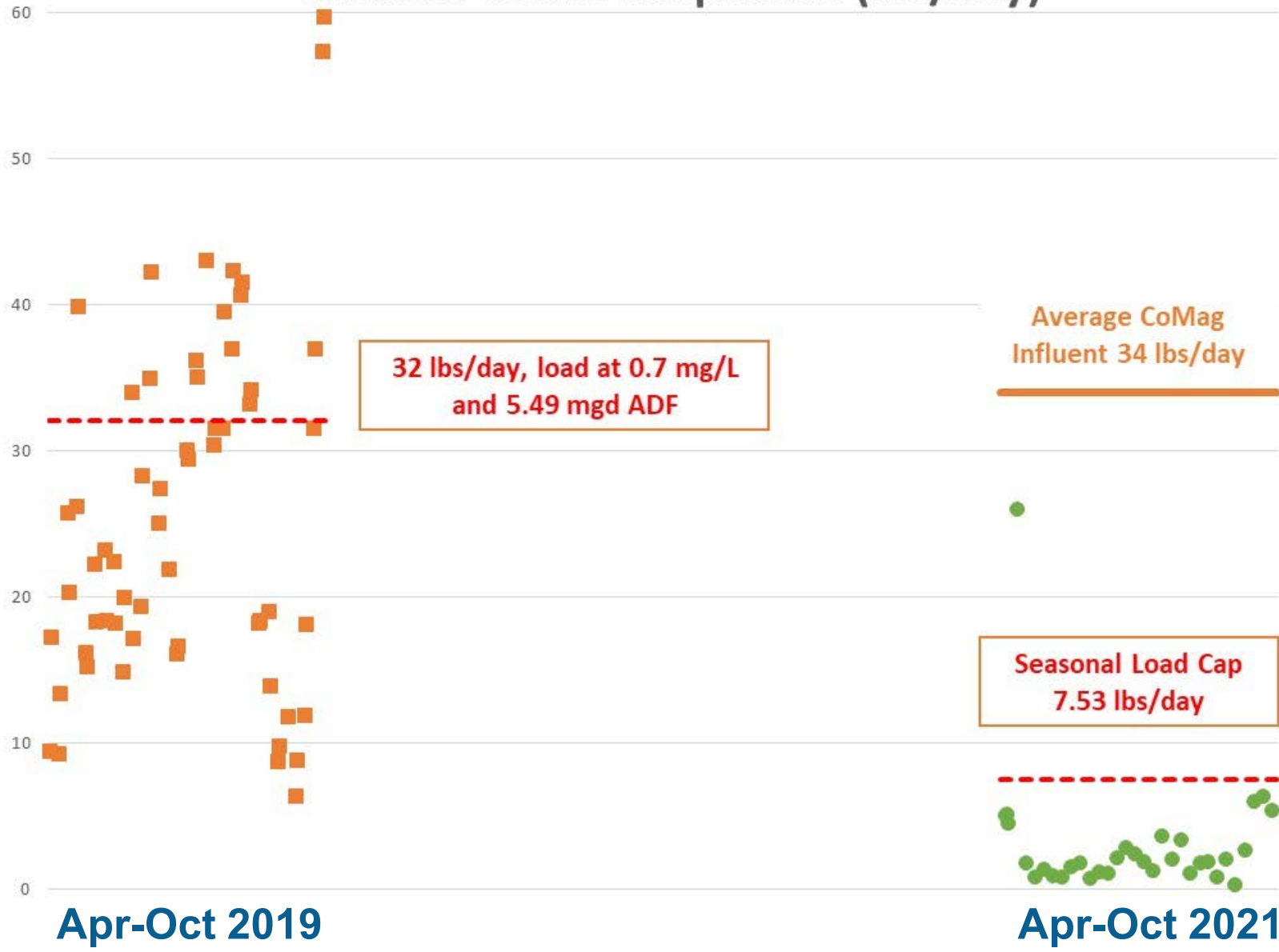
Seasonal Load Cap 7.53 lbs/day

# Performance Test Results

## Effluent Total Phosphorus (mg/L)



# Effluent Total Phosphorus (lbs/day)





# IMPACT ON PLANT OPERATIONS

PARAMETER	CHANGE 2019 → 2021	NOTES
Plant Flow	5.32 mgd → 4.68 mgd	Drier year
Plant Influent TP	147 lbs./day → 116 lbs./day	Lower loads
Effluent TP	25 lbs./day → 3 lbs./day	88% reduction
Effluent TSS	126 lbs./day → 99 lbs./day	22% reduction
PAC Usage (multi-point)	169 gpd → 73 gpd	57% reduction
Alum Usage (tertiary)	0 gpd → 410 gpd	New
Effluent Aluminum	0.11 mg/L → 0.22 mg/L	105% increase

# IMPACT ON PLANT OPERATIONS

- **Effluent Quality**

- Meeting New Permit – 1 year ahead of schedule!

- **Process**

- Process was robust and reliable
- Process adjustment reach steady state quickly (~ 1-Hr)

- **Up Ahead for 2022 Season**

- Continue process optimization with Evoqua
  - Minor Controls improvements
  - Minimize solids carry over from clarifiers to effluent
    - Causing added maintenance
    - Chemistry (Chemical, magnetite)?
    - Other options?

# ACKNOWLEDGMENTS

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# QUESTIONS?

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## QUIZ QUESTIONS (TRUE / FALSE)

- **Jar testing was a good prediction of using PACL for low level phosphorus removal ?**
  - False – Even though the town wanted to use PACL, field testing showed it was not an option
- **The volume of chemicals used decreased after CoMag was started up?**
  - False – PACL usage was reduced by 100 gpd but alum usage increased from 0 to ~400 gpd.