

REVIEW OF ZINC REMOVAL PILOT STUDIES

Sturbridge Wastewater Treatment Facility

NEWEA Annual Conference 2020

Ian Catlow, PE Austin Weidner, PE



PRESENTATION OVERVIEW

- Regulatory History
- Treatment Facility Overview
- Metals Removal Approach
- Zinc Removal Trials & Performance





REGULATORY HISTORY

• 2010 Plant Upgrade

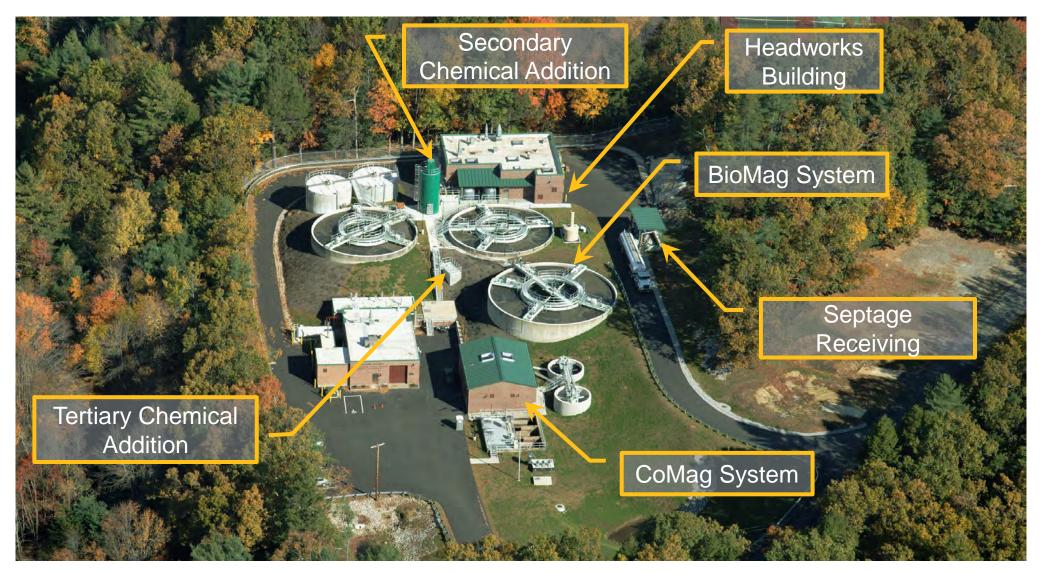
- Phosphorous Limit & Flow Increase
- 2012 Upgrade Complete
- 2014 New Total Zinc Limit
- Zinc Optimization Work Ongoing

NPDES PERMIT HISTORY

	2006 Permit	2014 Permit
Flow	0.75 MGD	1.3 MGD
Total Phosphorous	0.2 mg/L	0.12 mg/L
Ammonia	1.5 mg/L	0.87 mg/L
Total Zinc	No Limit	46.9 µg/L



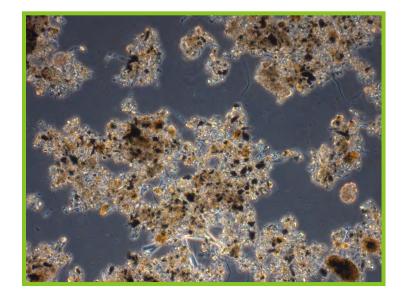
STURBRIDGE WWTF OVERVIEW





BIOMAG & COMAG TREATMENT CONCEPT

- BioMag Incorporates Ballast Into Biological Floc
- CoMag Incorporates Ballast Into Chemical Floc
- Ballasted Flocculation With Magnetite
 - SG Magnetite = 5.2
- Magnetite Is Liberated From WAS
 By Shear Mill
- Magnetite Is Recovered With A Magnet







METALS REMOVAL APPROACH

Source Reduction

• Industry

Drinking Water

- Source Water
- Corrosion

Accepted Waste

- Septage and/or Leachate

Treatment Options

• Chemical Precipitation

- Convert to a Solid \rightarrow Remove the Solids
- Adjust pH, coagulant, other

Sorption Processes

- More Surfaces = More potential for sorption
- Biological Uptake



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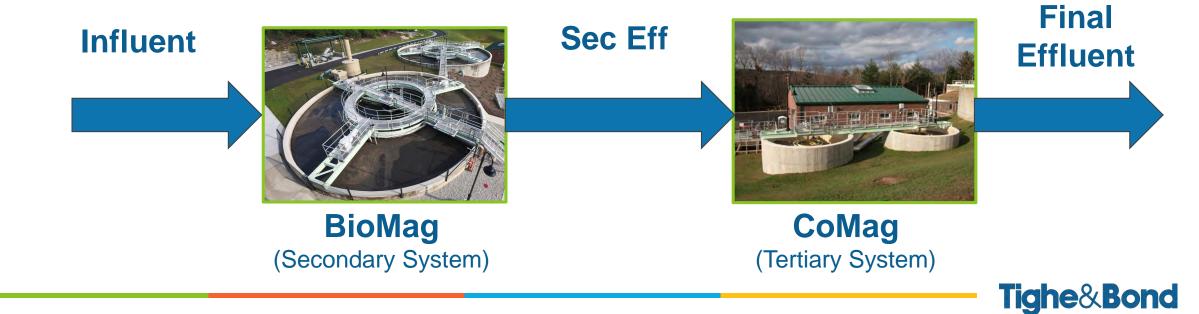
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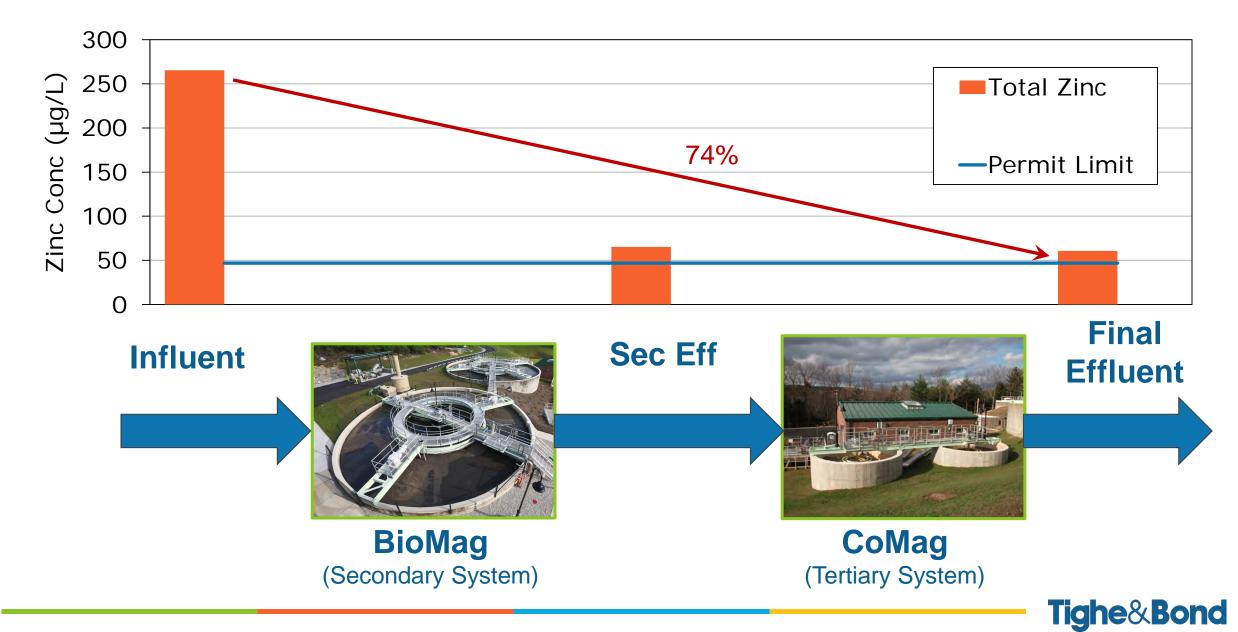
Data Collection



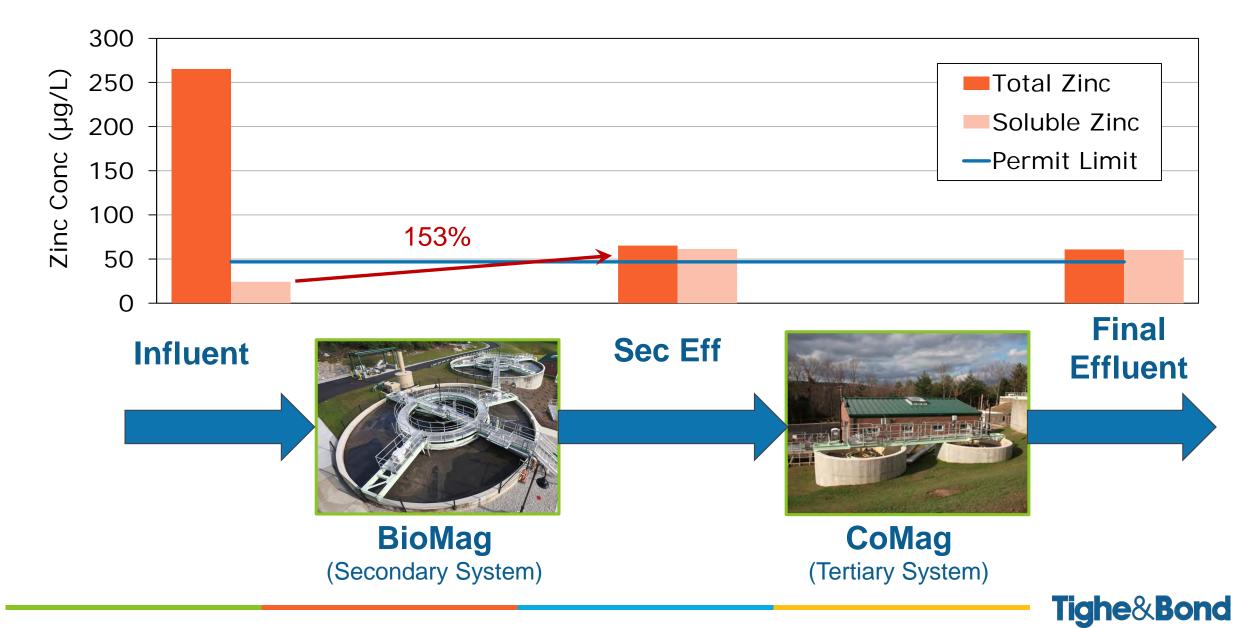
PLANT-WIDE ZINC BALANCE



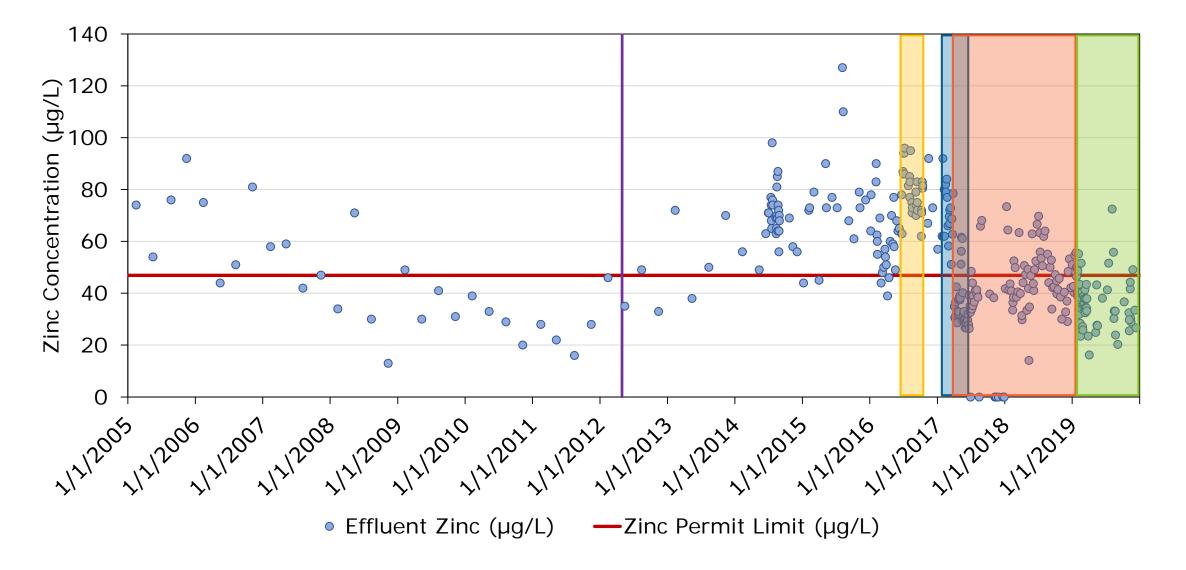
PLANT-WIDE ZINC BALANCE



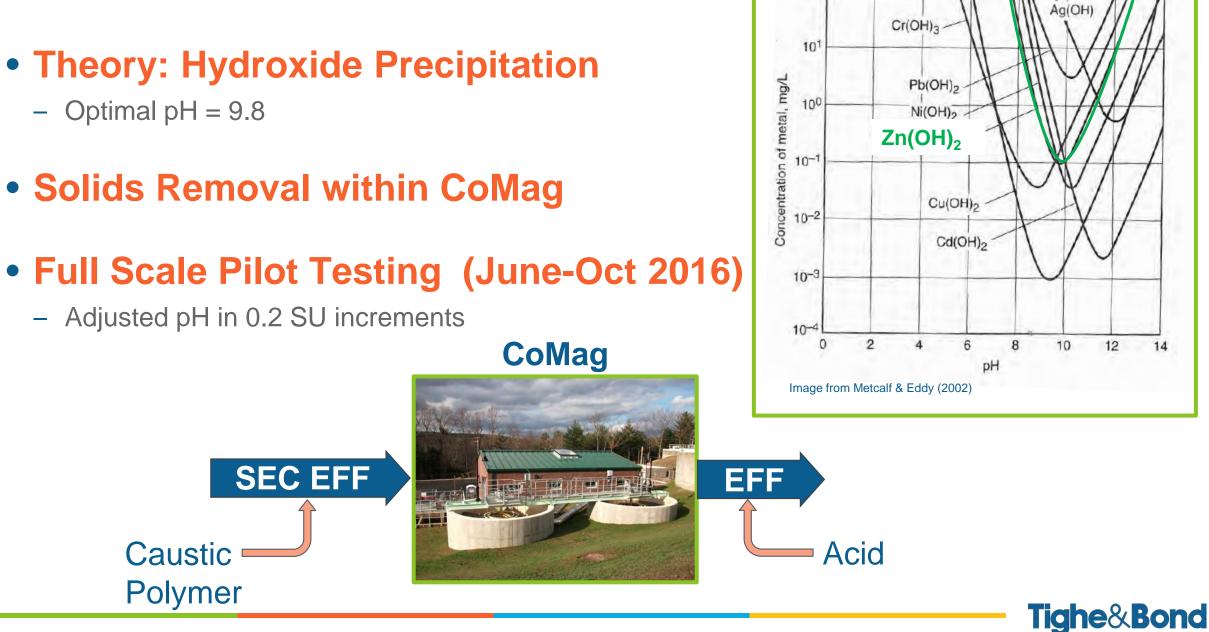
PLANT-WIDE ZINC BALANCE



HISTORY OF ZINC REMOVAL AT STURBRIDGE

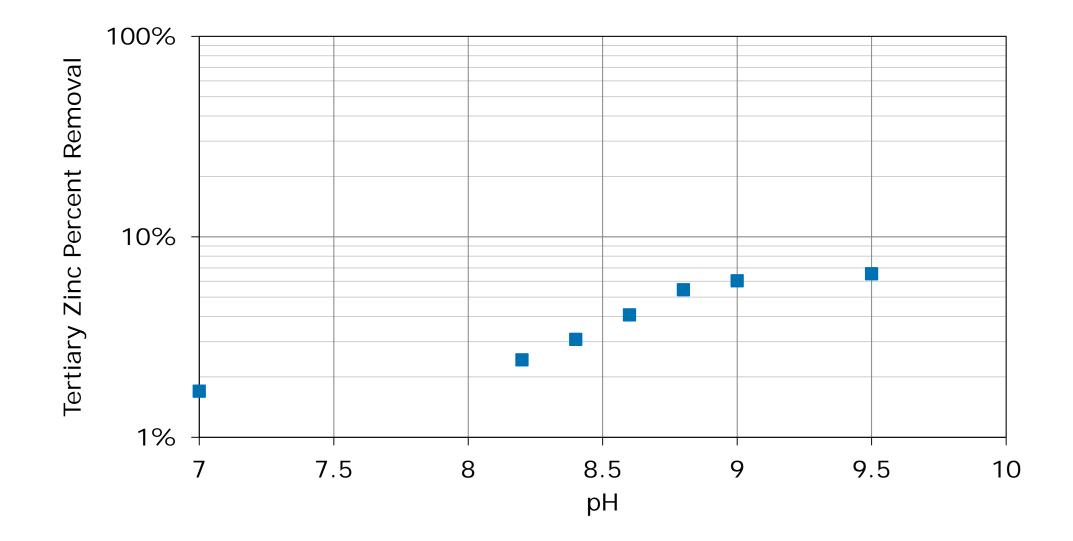






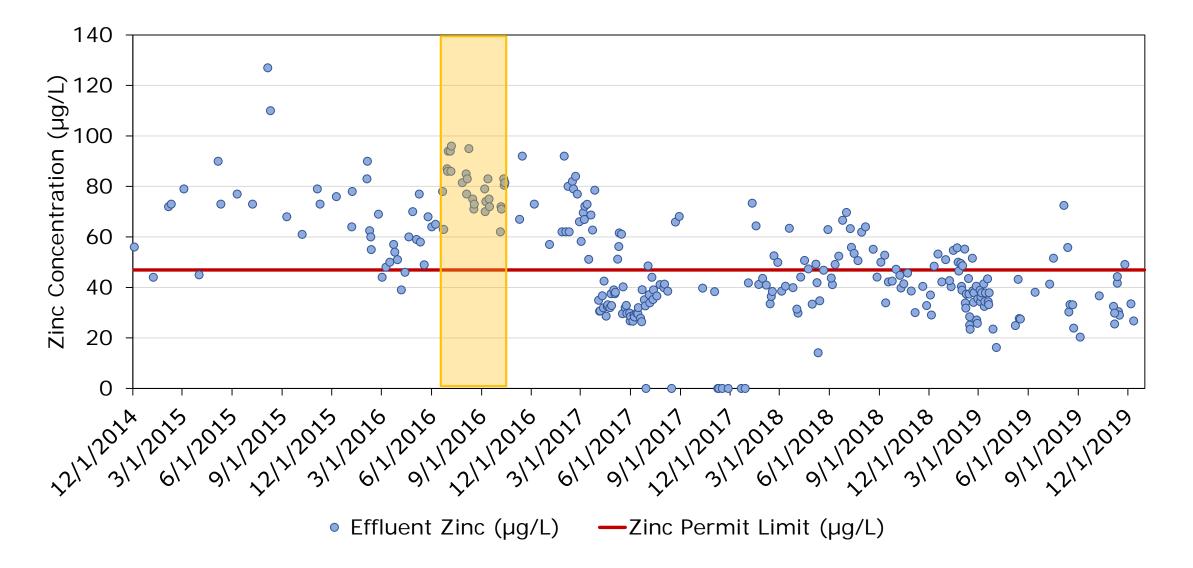
TRIAL 1: TERTIARY PH ADJUSTMENT

TRIAL 1: TERTIARY PH ADJUSTMENT RESULTS





TRIAL 1: TERTIARY PH ADJUSTMENT RESULTS





TRIAL 2: SOURCE REDUCTION

Point Source Contamination

- Reviewed Major Water Users

• Drinking Water

- Source Water
- Zinc Orthophosphorus

Contamination

- Magnetite
- Defoamer
- Sampling Procedures

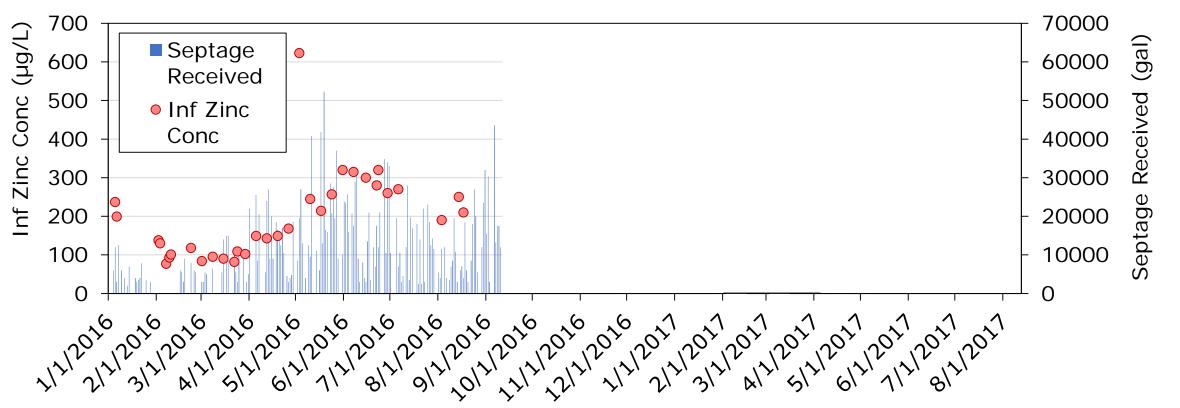




TRIAL 2: SOURCE REDUCTION

- Accepted Waste Streams
 - Septage & Leachate
 - High Strength & Variability



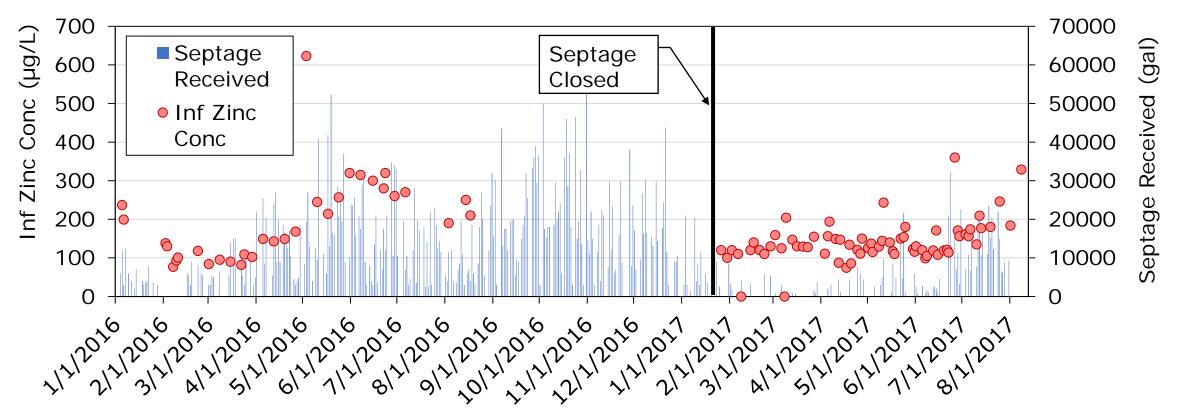


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TRIAL 2: SOURCE REDUCTION

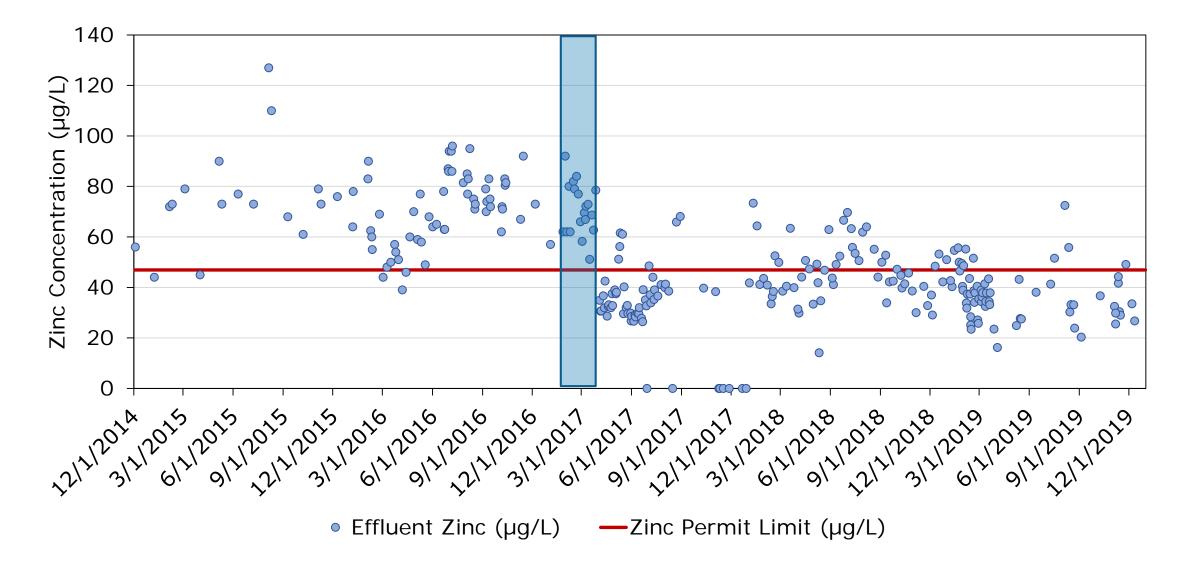
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TRIAL 2: SOURCE REDUCTION RESULTS





TRIAL 3: SECONDARY SYSTEM FERRIC & LIME ADDITION

- Return to Original Operation Mode
- Target Secondary System (BioMag)
 - Curb Increase in Soluble Zn

• Theory

- Increased pH reduces solubility
- Iron has a higher affinity for metals than aluminum



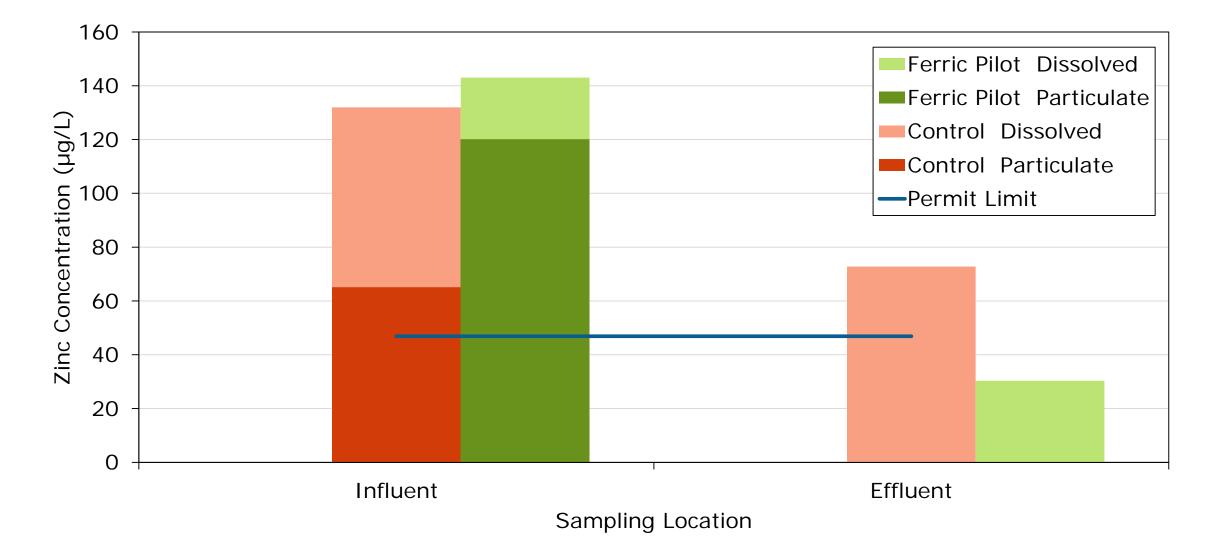


TRIAL 3: FERRIC & LIME PILOT TESTING PLAN

BioMag CoMag (Tertiary System) (Secondary System) INF EFF FeCl₃ FeCl₃ Lime Caustic

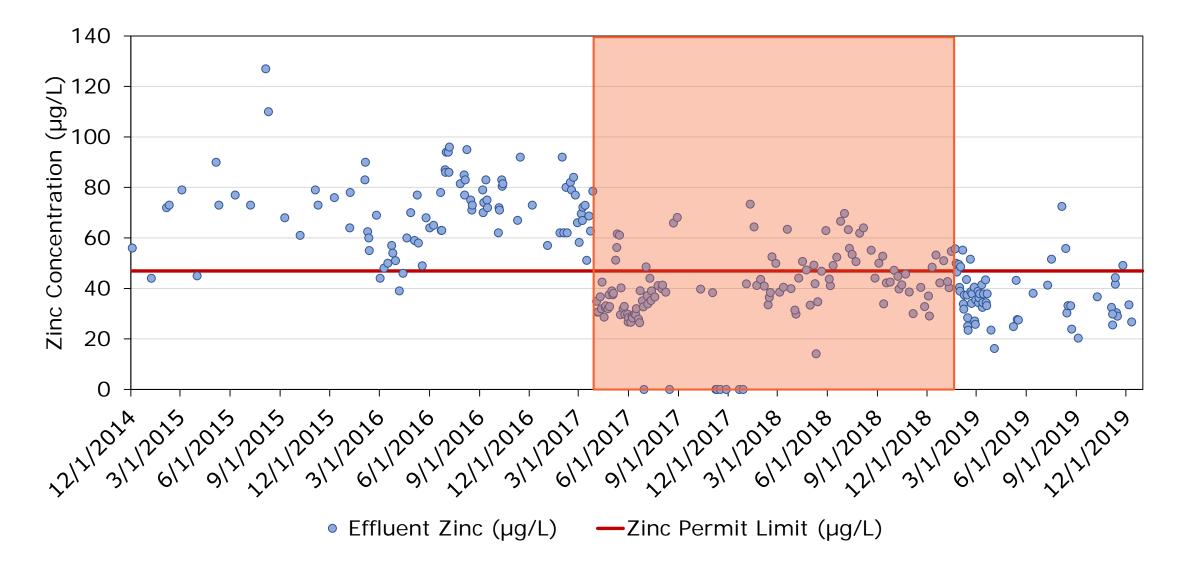


TRIAL 3: FERRIC & LIME PILOT TESTING RESULTS



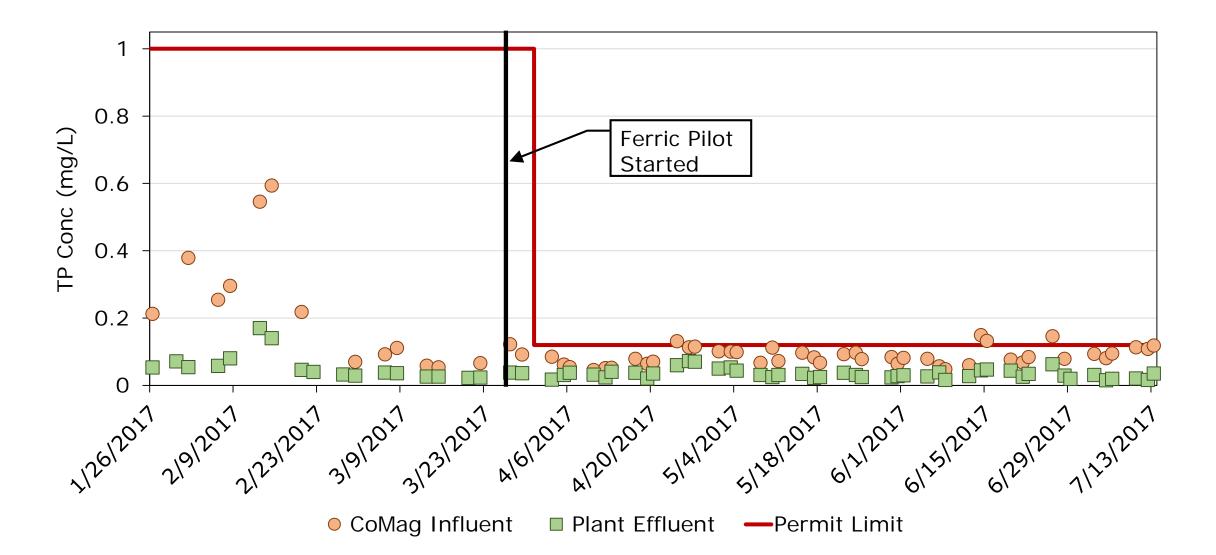


TRIAL 3: FERRIC & LIME ADDITION RESULTS



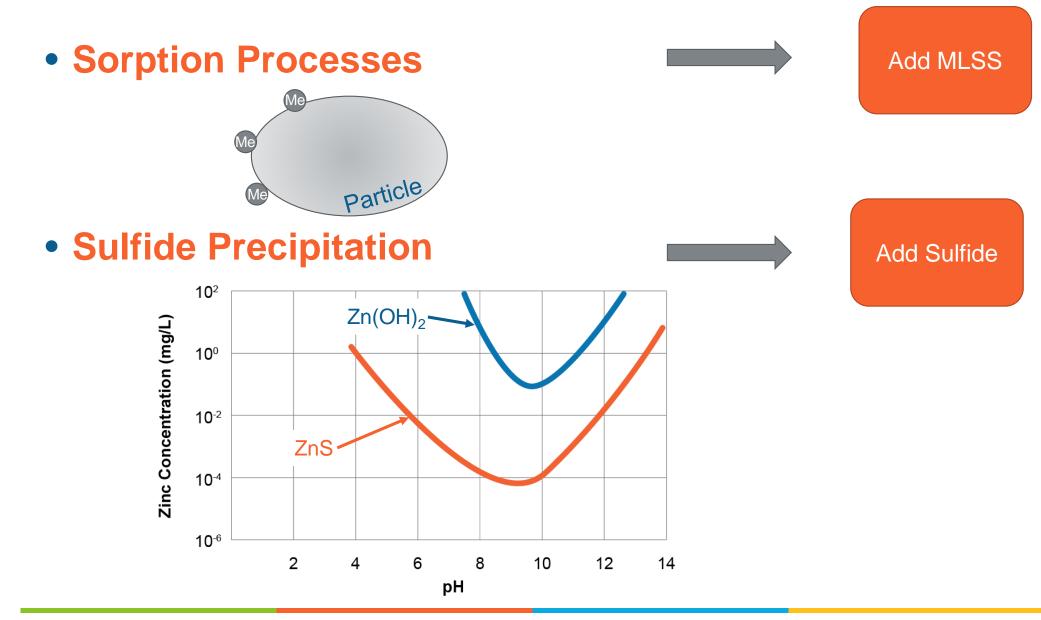


TRIAL 3: TOTAL PHOSPHORUS RESULTS



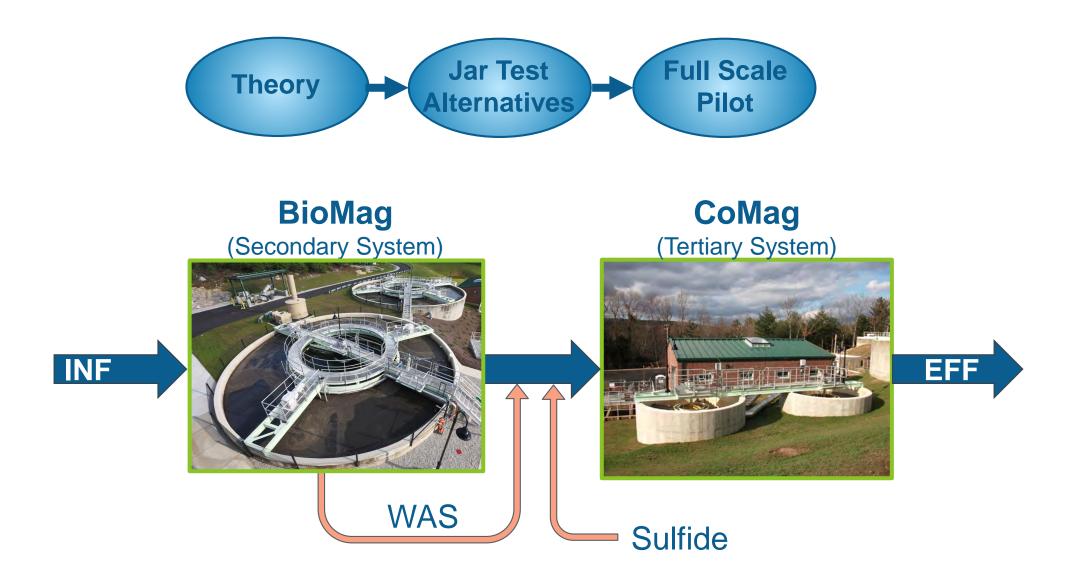


TRIAL 4: EVOQUA ADVANCED REMOVAL TECHNIQUES



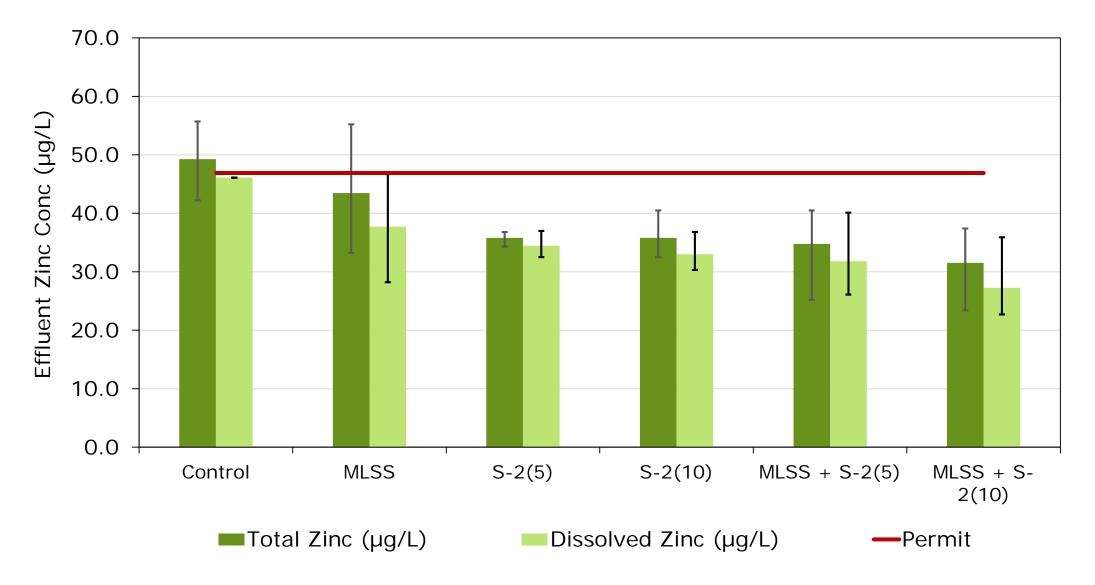
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TRIAL 4: EVOQUA MLSS & SULFIDE PILOT TEST PLAN



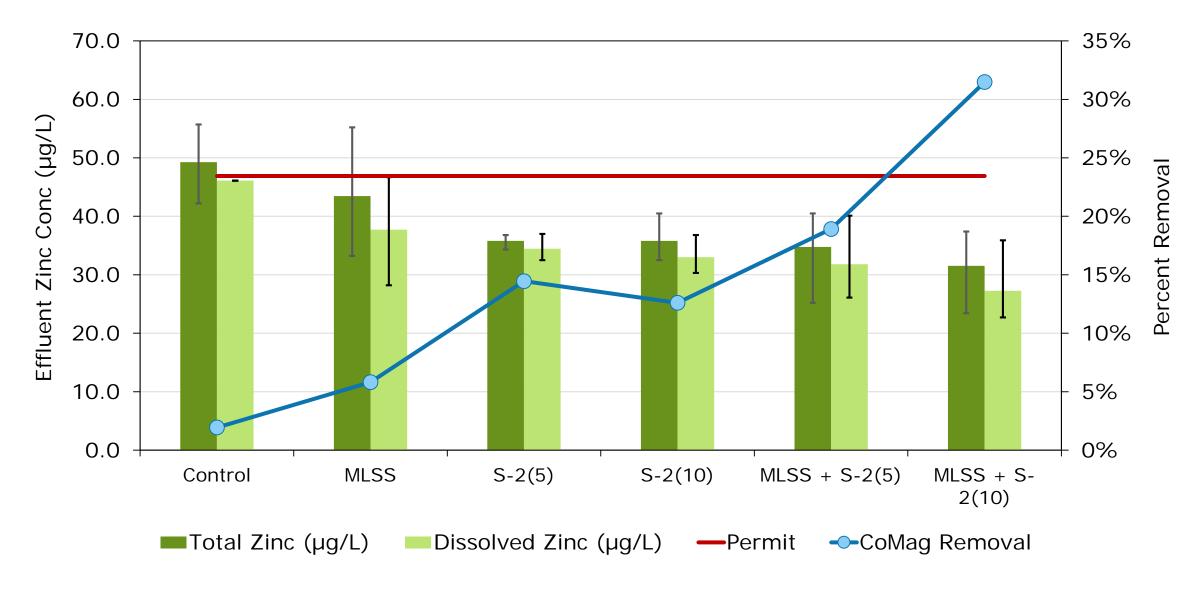


TRIAL 4: EVOQUA MLSS & SULFIDE ADDITION RESULTS



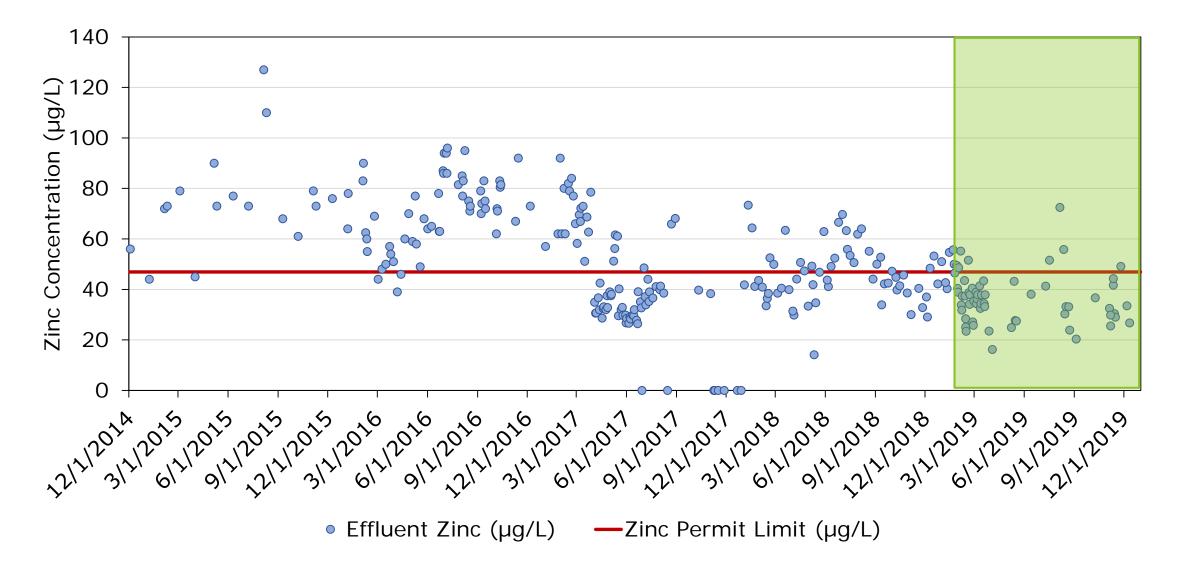


TRIAL 4: EVOQUA MLSS & SULFIDE ADDITION RESULTS





TRIAL 4: MLSS & SULFIDE ADDITION RESULTS



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CONCLUSIONS

- Data collection is essential
- Source reduction can be effective
- Metals often dissolve during Secondary Treatment
- Strategies for metals removal are plant-specific
- Combination of strategies may be needed









 Ian Catlow, PE:
 IBCatlow@tighebond.com

 Austin Weidner, PE:
 ADWeidner@tighebond.com

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