

Efficient Nutrient Removal under Low Dissolved Oxygen Operations

NEWEA 2017 Annual Conference

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Agenda

St Petersburg Southwest WRF

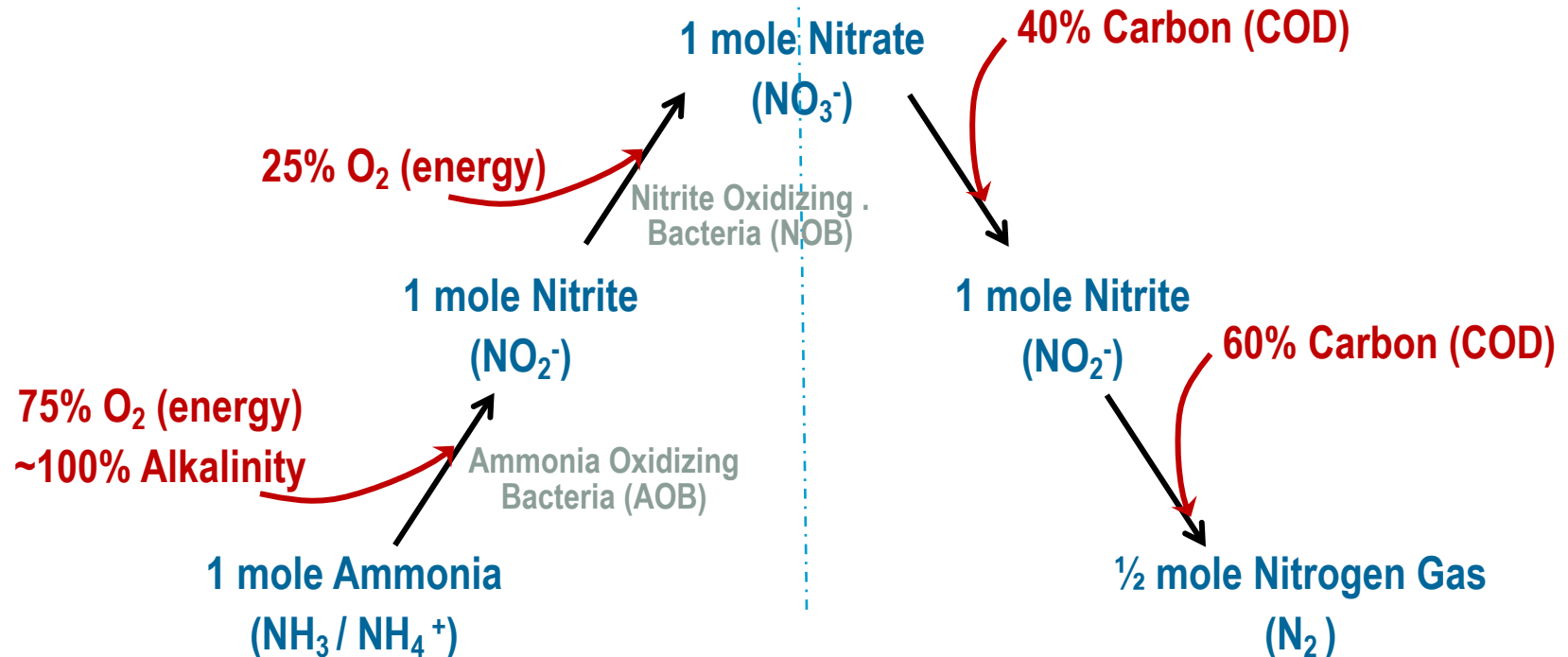
Madison Nine Springs WRF

Rochester NH

Conventional Nitrification-Denitrification

Autotrophic Bacteria
Aerobic Environment

Heterotrophic Bacteria
Anoxic Environment



Nitrification-Denitrification = “Nitrite-Shunt”

Heterotrophic Bacteria can be favored at
Low DO

Nitrification

75% O₂ (energy)

~100% Alkalinity

1 mole Ammonia
(NH₃ / NH₄⁺)

1 mole Nitrite
(NO₂⁻)

Ammonia Oxidizing
Bacteria (AOB)

1 mole Nitrite
(NO₂⁻)

60% Carbon (COD)

Denitrification

½ mole Nitrogen Gas
(N₂)

Benefits

- 25% reduction in oxygen demand (energy)
- 40% reduction in carbon (e⁻ donor) demand
- 40% reduction in biomass production

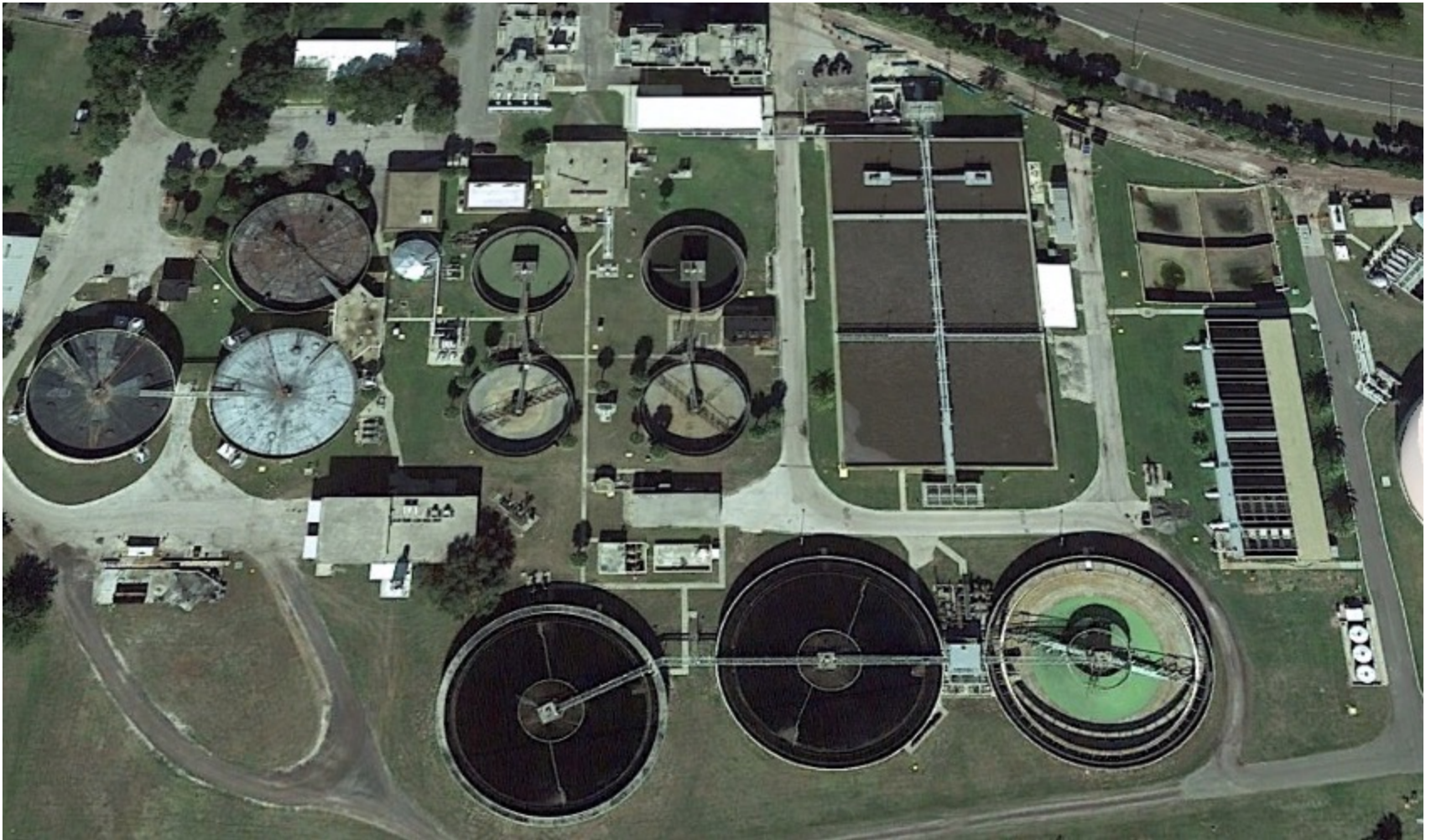
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Mainstream Nitrite Shunt

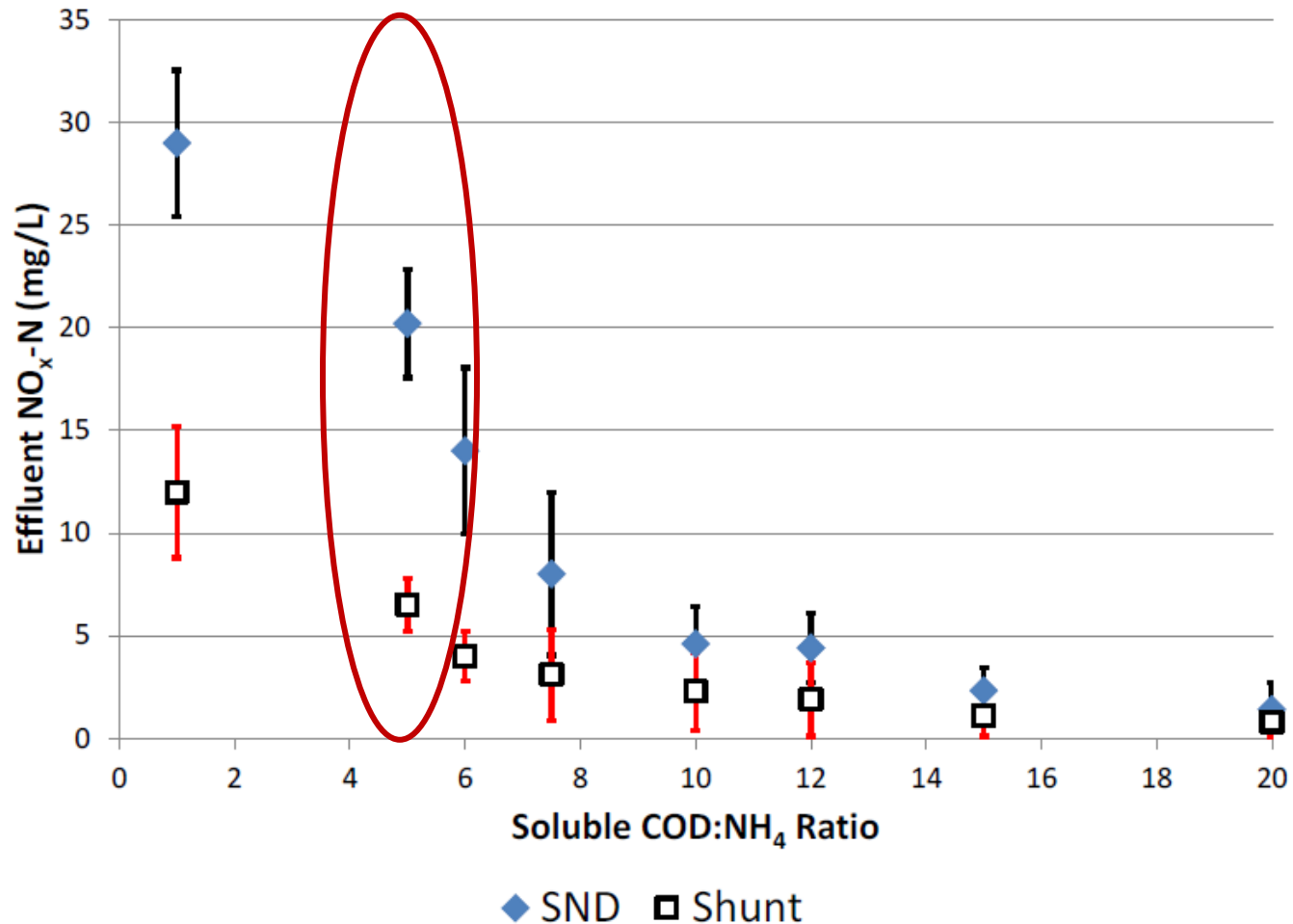
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- Current Average Flow = 9.5 MGD
- Influent TKN \approx 42 mgN/L
- TP \approx 4 mgP/L
- Temp. = 20 to 30 C
- SRT = 4 to 5 days
- Effluent nutrient targets
 - Total N = 10 mg/L
 - Total P = 1.0 mg/L

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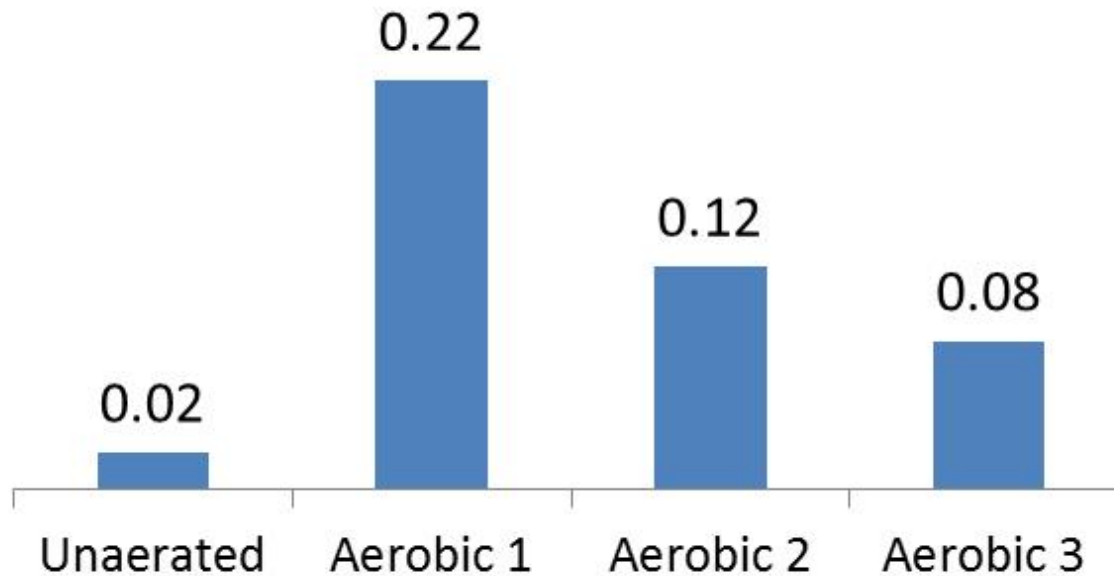
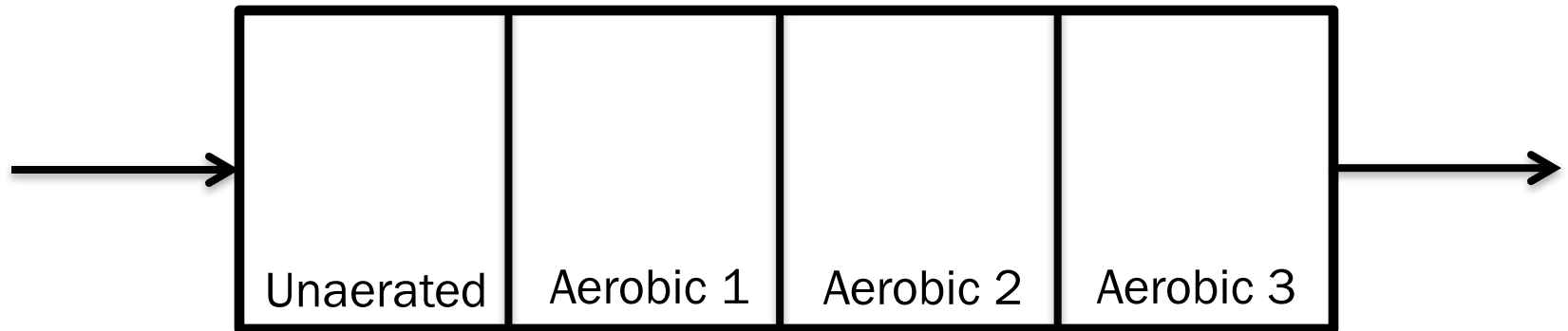
Carbon Requirements for Mainstream Biological Nitrogen Removal Processes



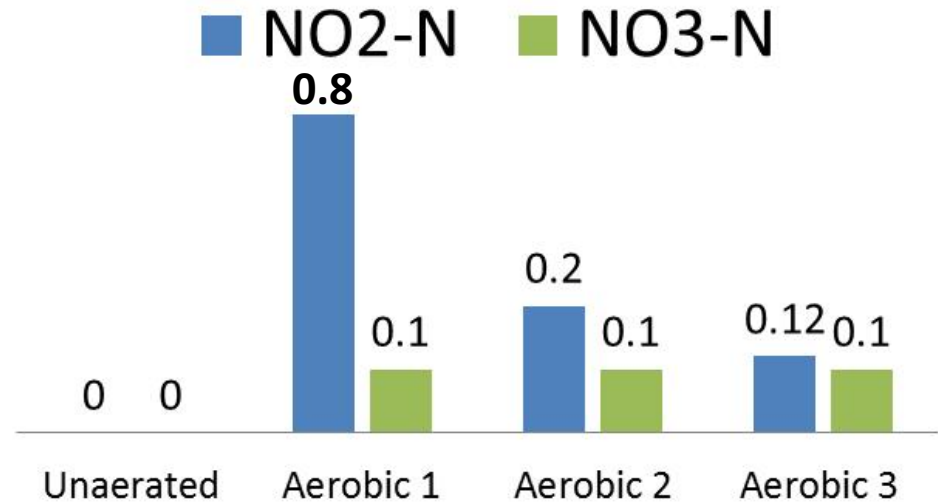
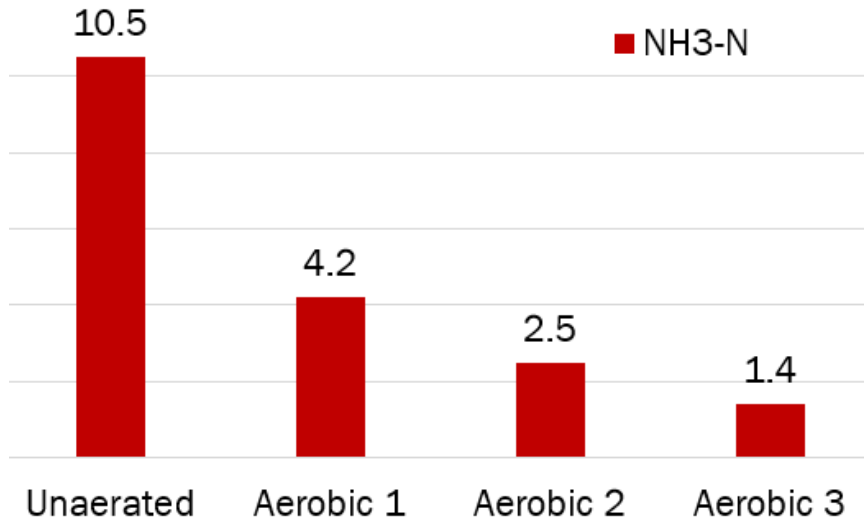
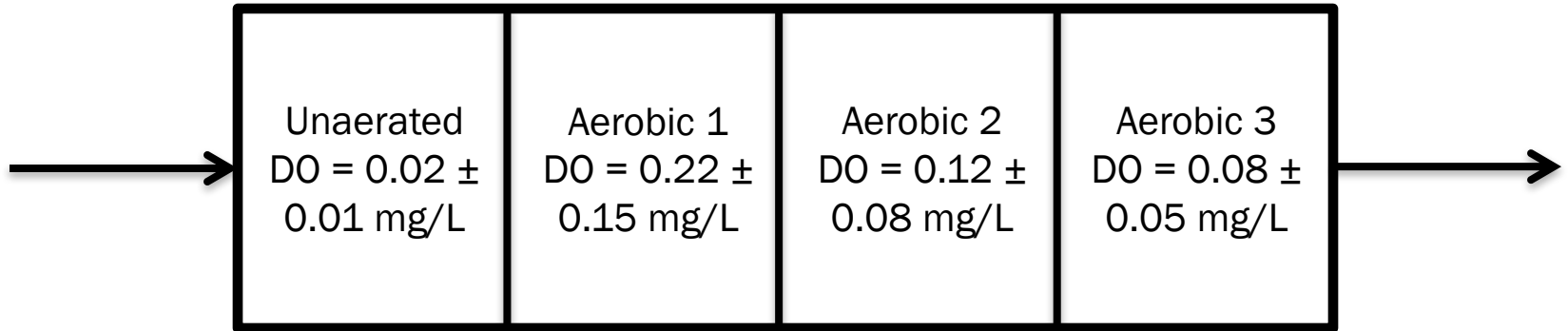
Nitrite Shunt Control Strategy (DO, SRT, NH₄, NO₃)

Control Parameter	Condition	Action
NH ₄ ⁺	< 1 mgN/L	Reduce SRT Maintain DO = 0.1 mg/L
	> 3 mgN/L	Increase SRT Increase DO ≈ 0.3 mg/L
NO ₃ ⁻	> 1 mgN/L	Reduce DO to 0.1 mg/L
	< 1 mgN/L	No action

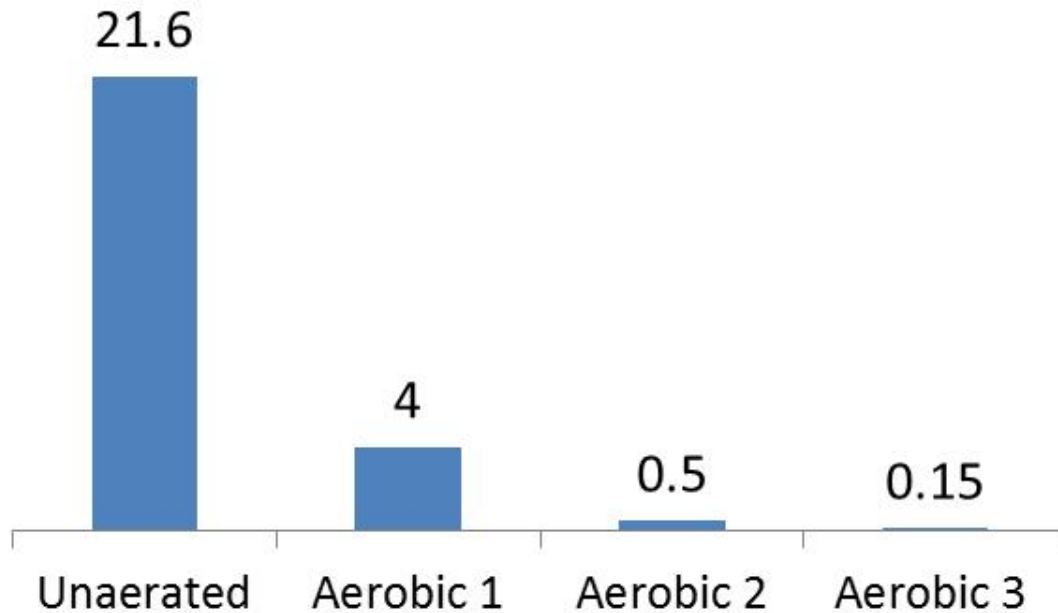
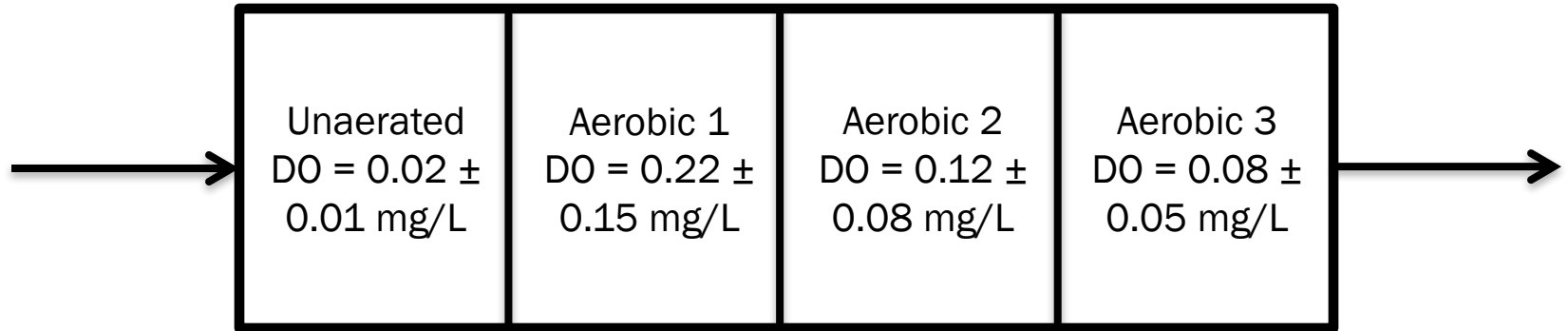
Dissolved Oxygen Profile



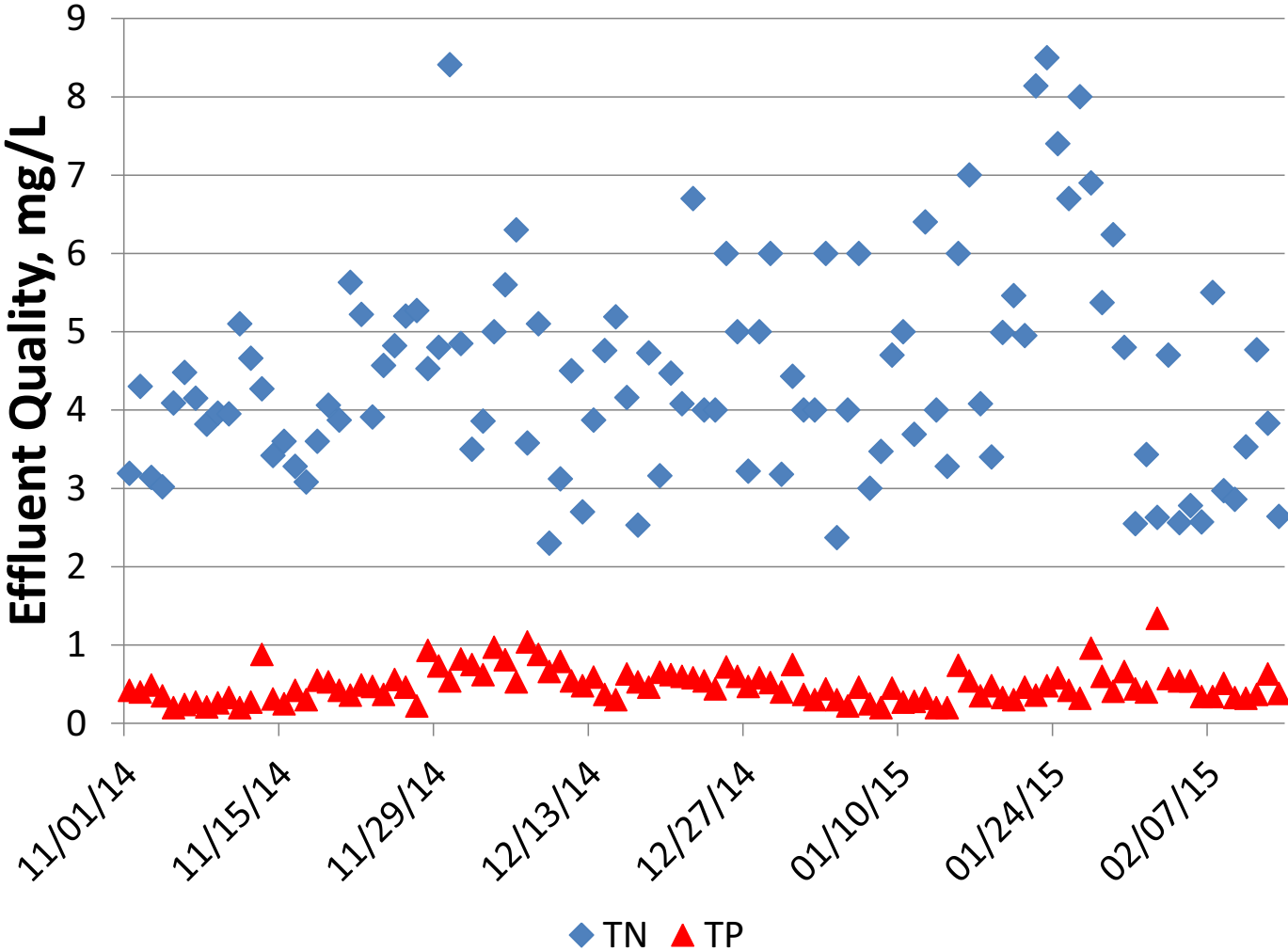
Inorganic Nitrogen Profile



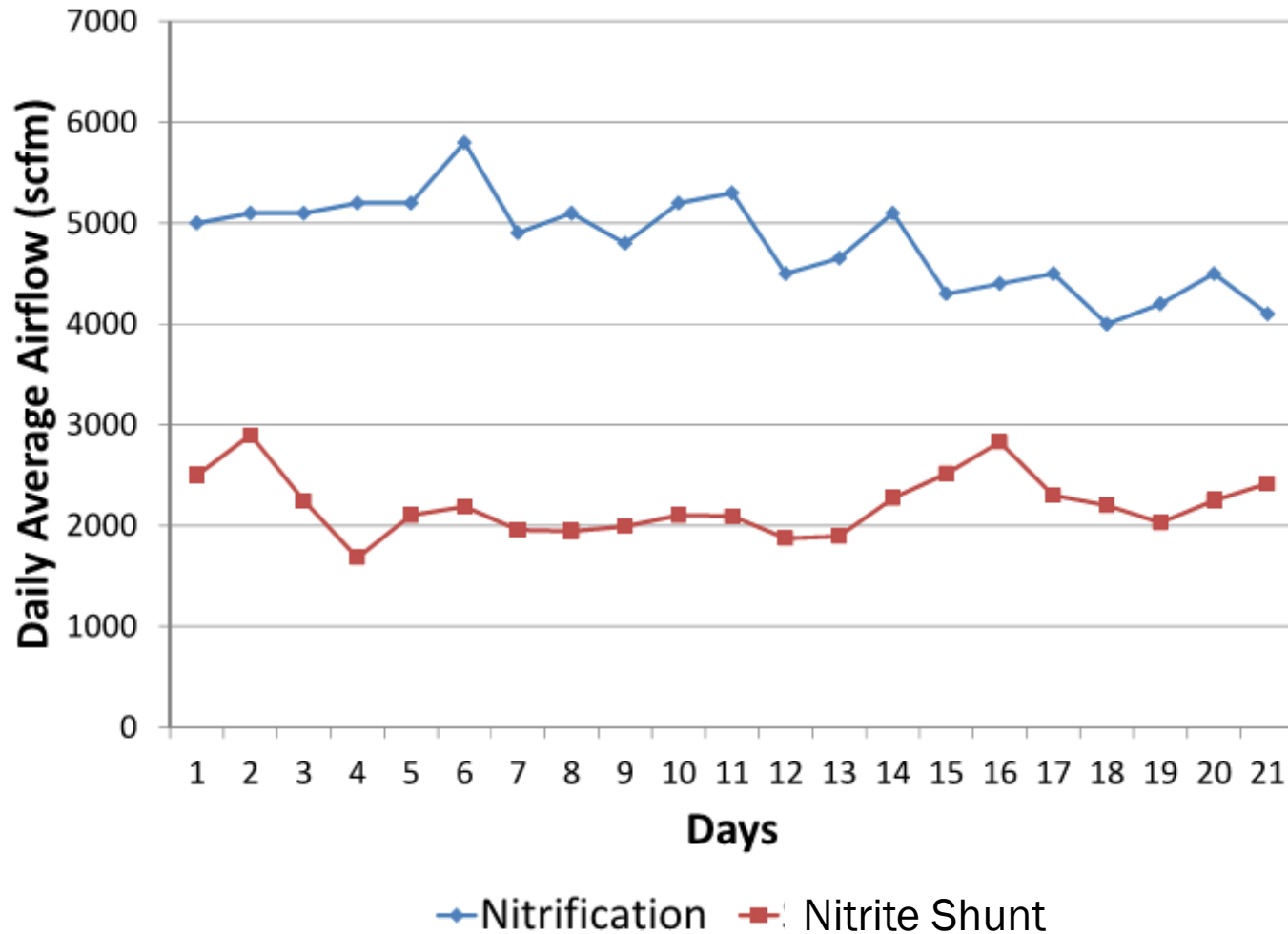
Soluble PO₄-P Profile



Final Effluent TN and TP



Aeration Comparison



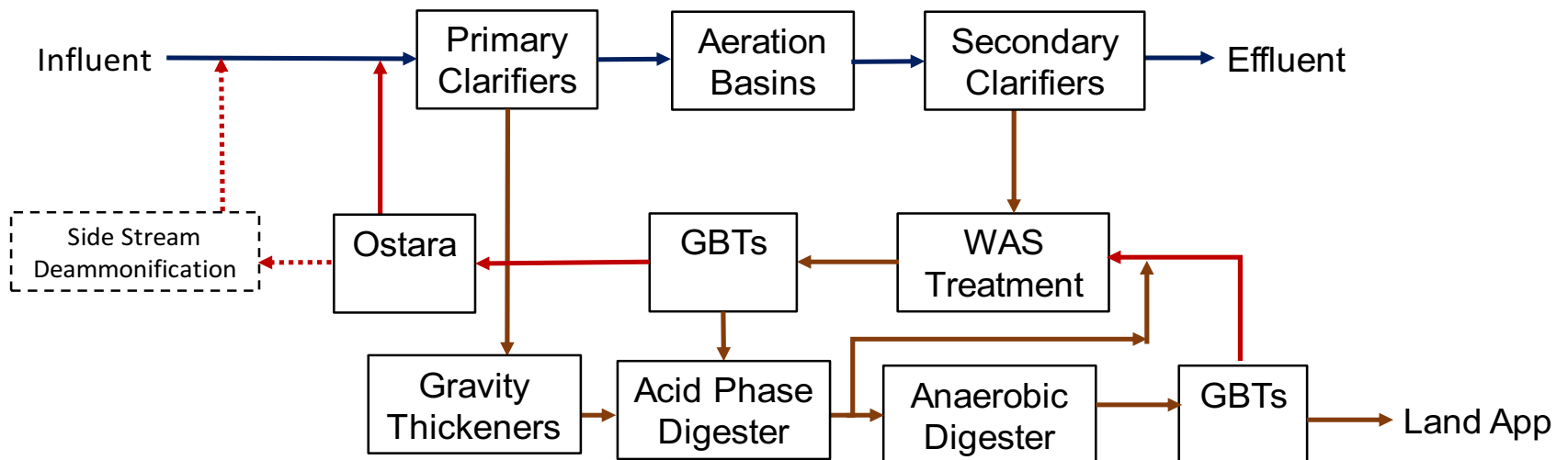
Final Thoughts

- Good N and P removal performance achieved at low DO operation
- Testing showed significant NOB suppression
- Very simple A/O process (RAS only; no IMLR)
- Simple control strategy
- 50% reduction in airflow

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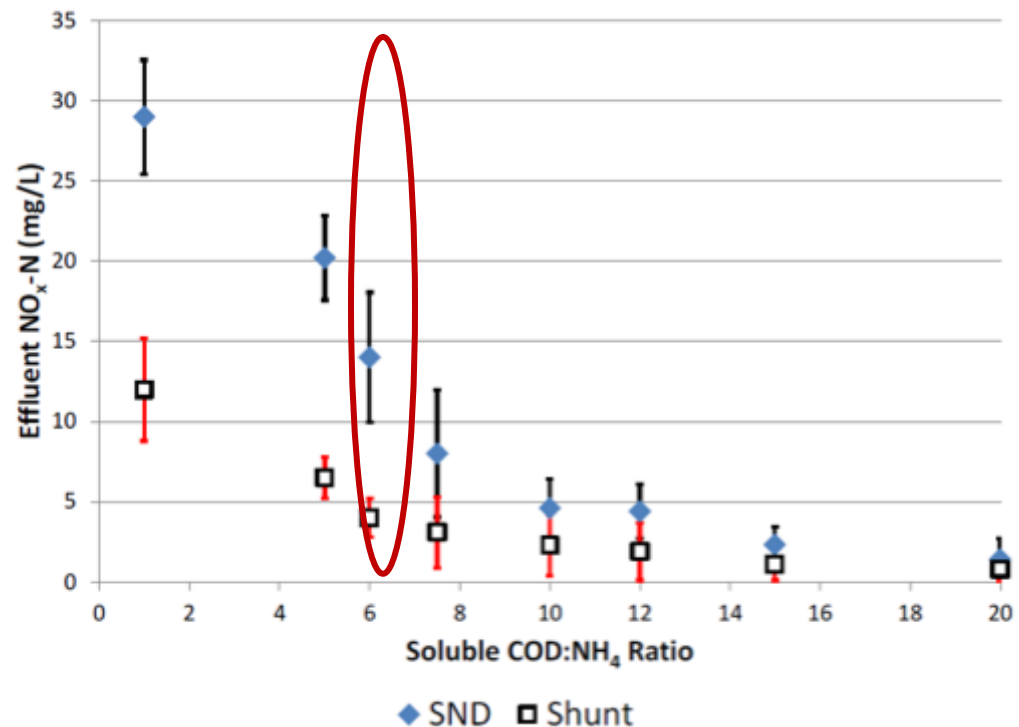
Conventional vs Mainstream Nitrite Shunt

Conventional vs Nitrite Shunt

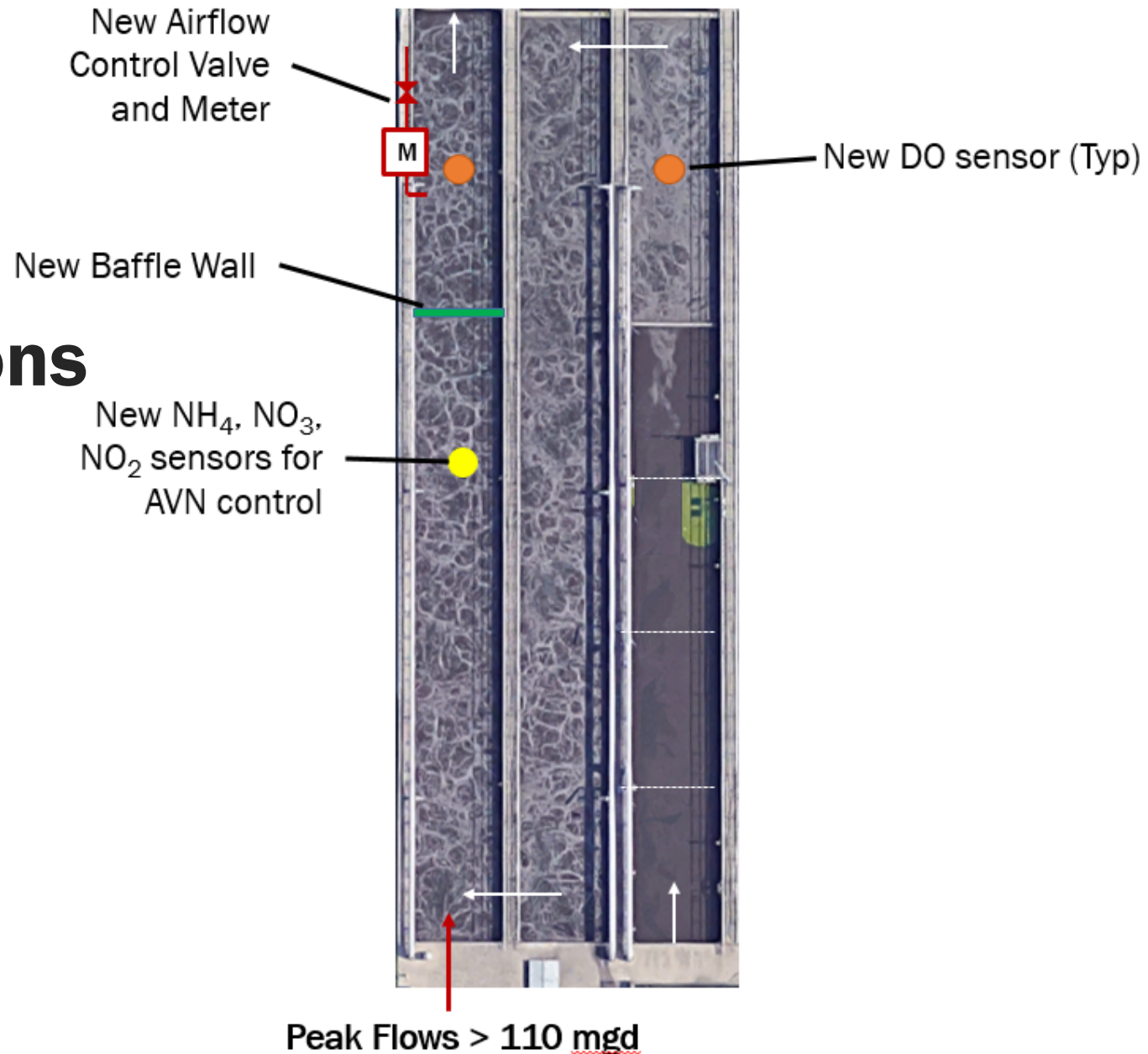


Madison Nine Springs WRF

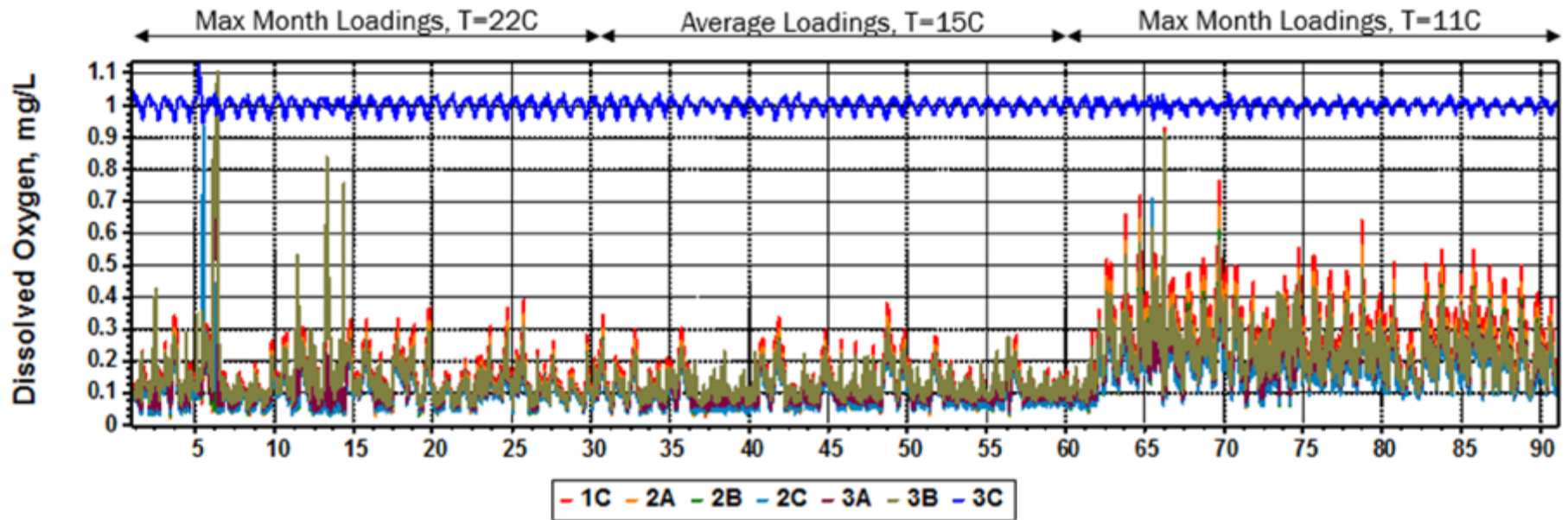
- Design Flow = 60 MGD
- Influent TKN \approx 45 mgN/L
- TP \approx 6 mgP/L
- SRT = 10 days
- Temp. = 11 to 20 C
- Target Effluent
 - Total N = 10 mg/L
 - Total P = 0.4 mg/L
 - Full nitrification



Nitrite Shunt Aeration Basin Modifications



Dissolved Oxygen Profile



BNR Alternative Life Cycle Analysis

Item	Alternative Cost, \$ Million			
	UCT	UCT with Sidestream Deammonification	Mainstream Nitrite Shunt	CEPT with Nitrite Shunt
Capital Costs	\$22	\$27	\$30	\$31
Additional Annual Operating Costs				
Blower energy	\$0.83	\$0.76	\$0.50	\$0.50
Non-blower energy	\$0.10	\$0.12	(\$0.01)	(\$0.01)
Chemicals	\$1.8	\$1.5	\$0.10	\$0.62
O&M Labor	\$0.04	\$0.10	\$0.10	\$0.11
Biosolids/energy/ struvite recovery	\$0.04	\$0.04	(\$0.15)	\$0.05
Total O&M	\$2.8	\$ 2.5	\$0.6	\$1.3
Present Worth	\$74	\$74	\$40	\$55

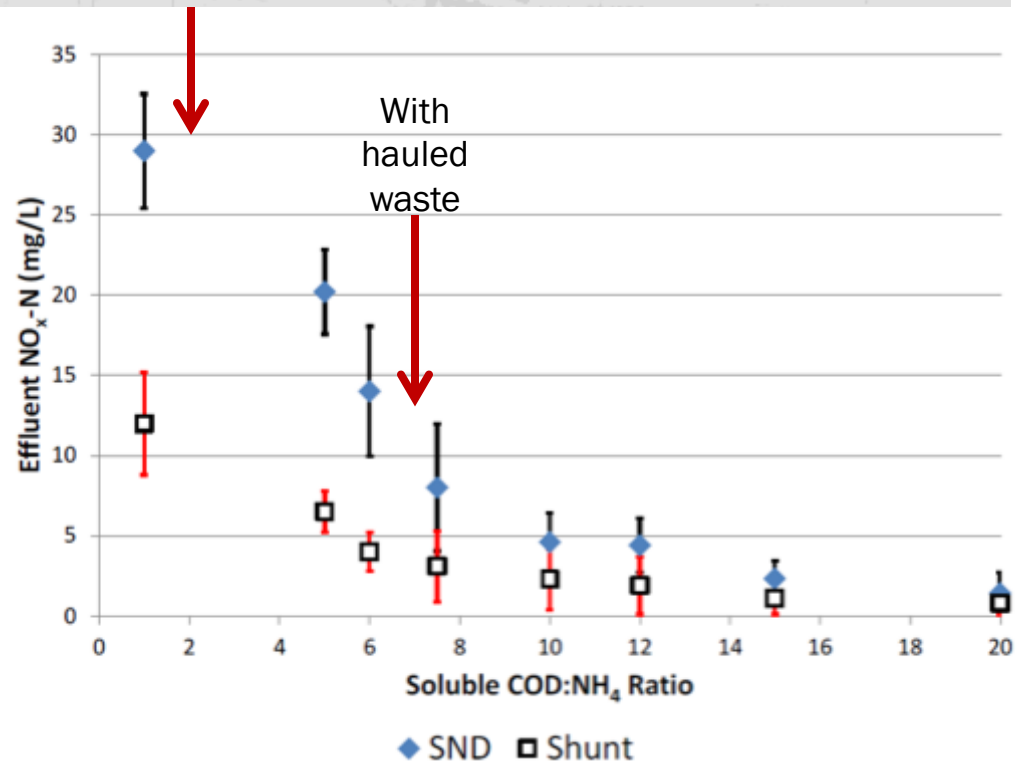
City of Rochester WWTF

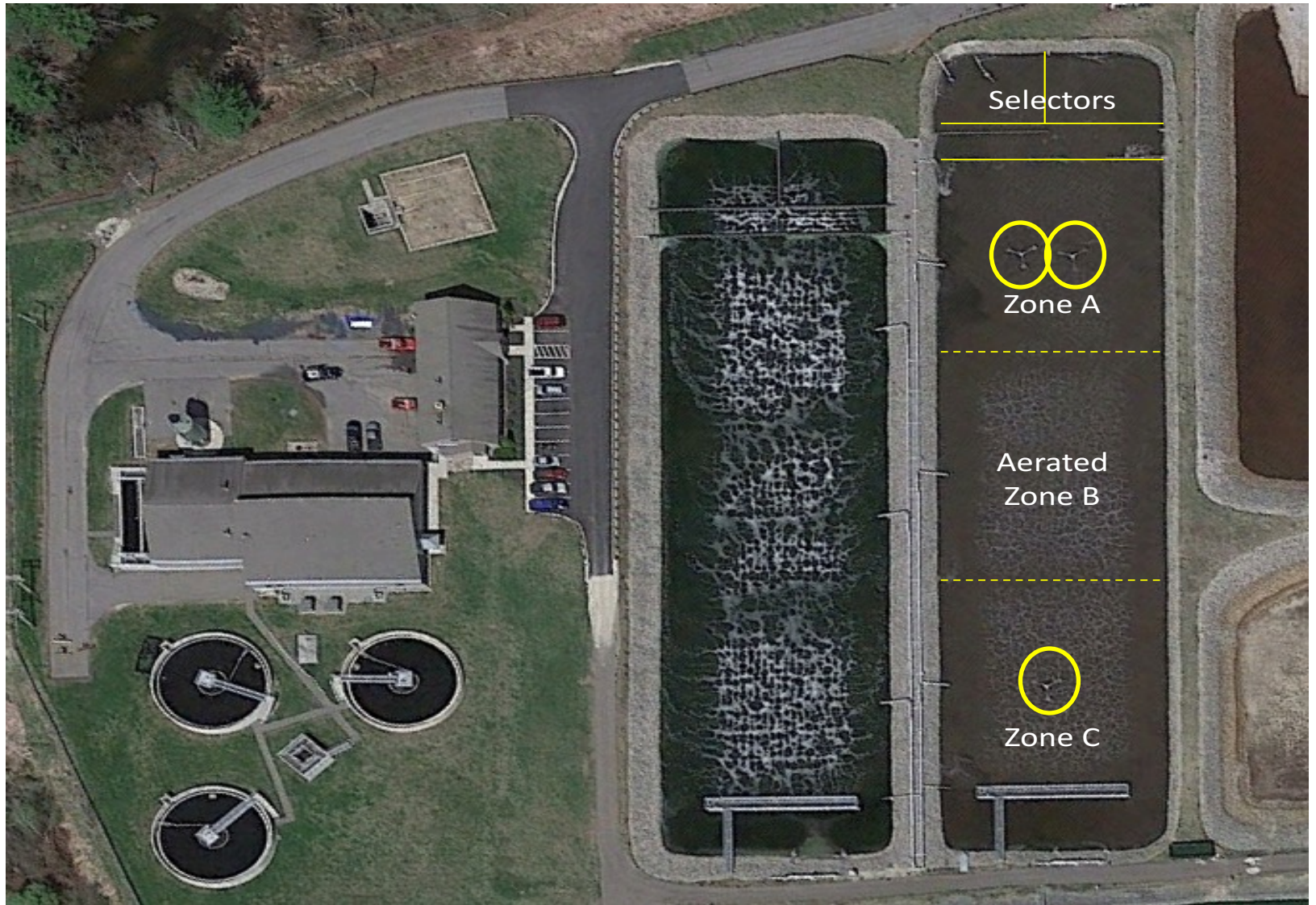
Low DO Operations



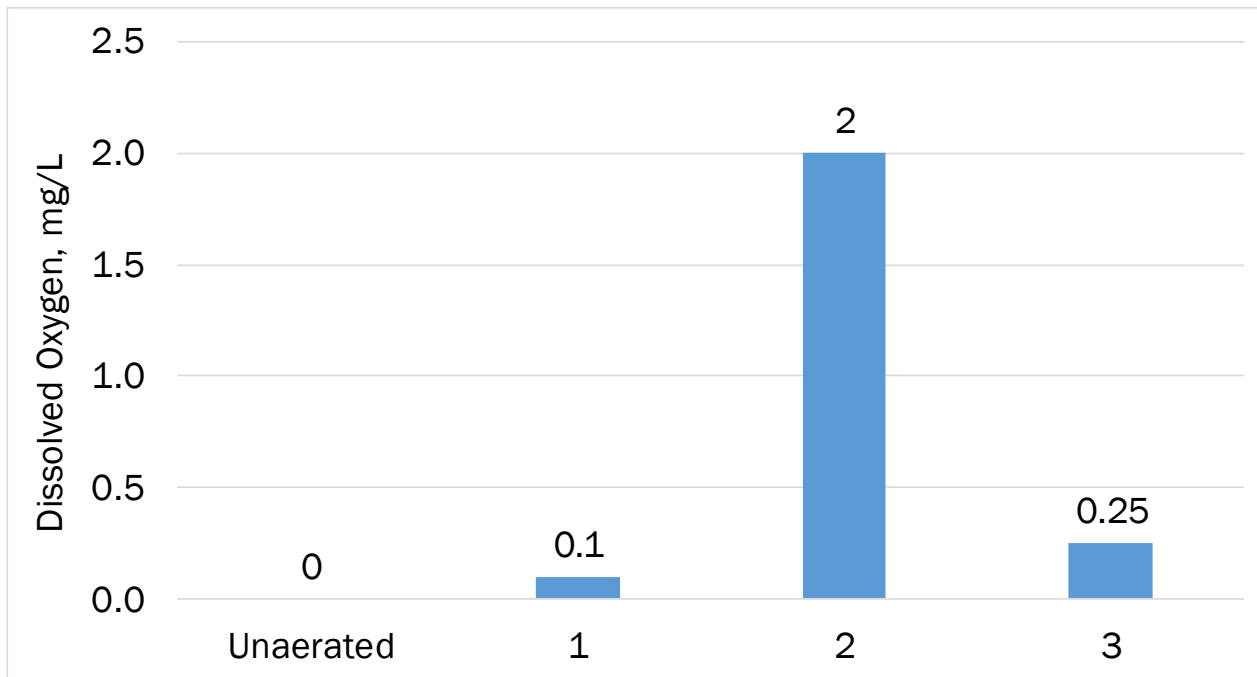
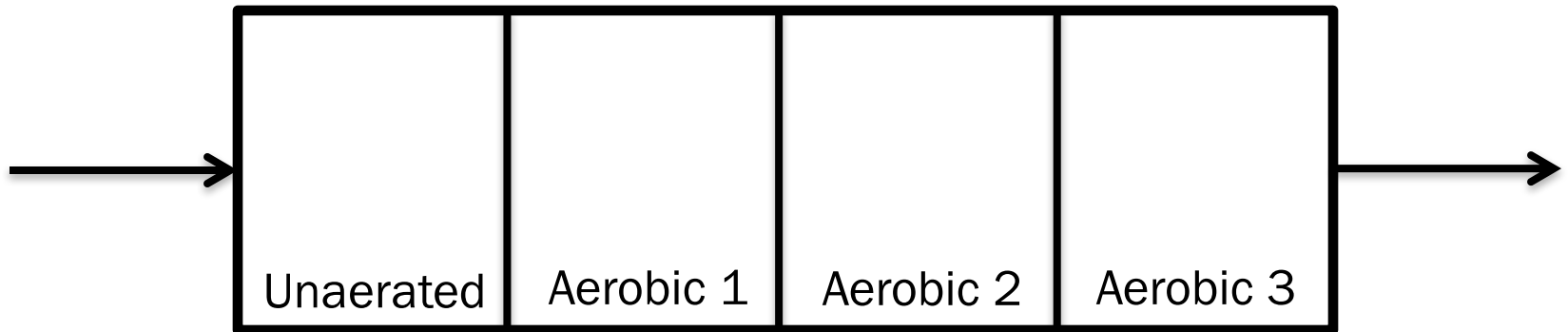
City of Rochester WWTF

- Current Average Flow = 2.9 MGD
- Influent TKN \approx 30 mgN/L
- TP \approx 4 mgP/L
- SRT = 30 days
- Temp. = 6 to 20 C
- Target Effluent
 - Total N = 8 mg/L

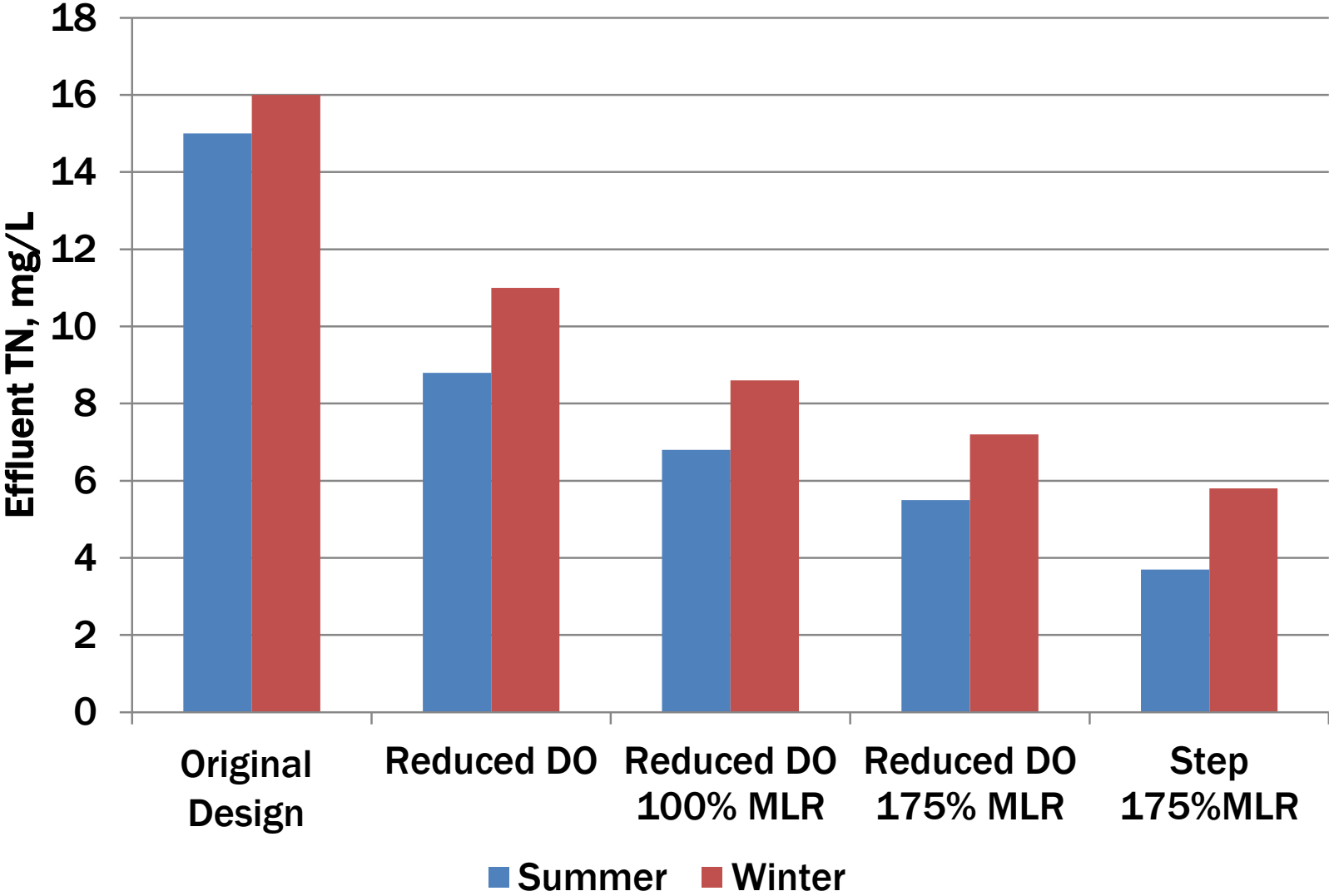




Dissolved Oxygen Profile



Effluent TN



Rochester Big Picture

- Effluent TN < 10 mgN/L
- Effluent TP < 1.0 mg/L
- Annual power costs reduced by $\approx 50\%$
- Alkalinity addition (soda ash) reduced by $\approx 50\%$
- Sludge quality (SVI) not impacted by low DO

Questions & Discussion

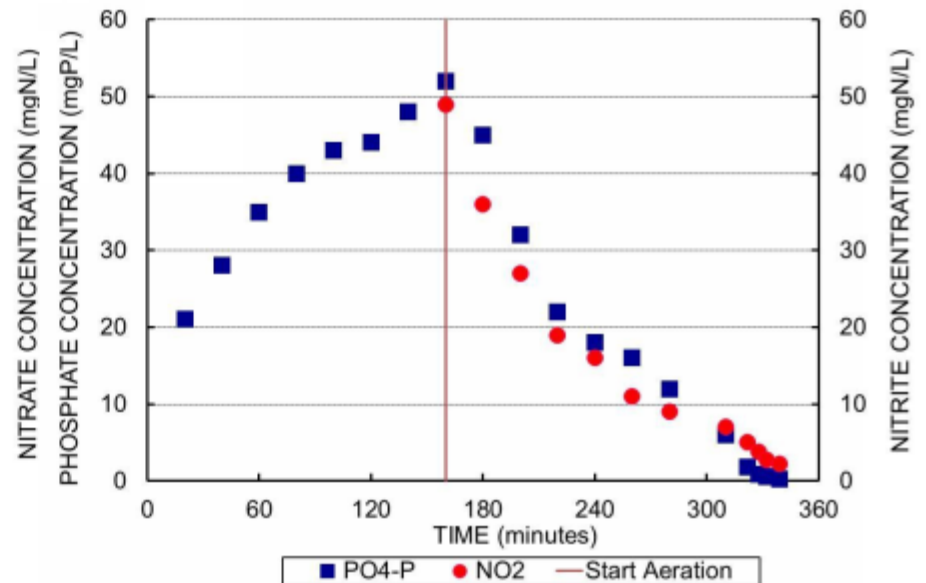
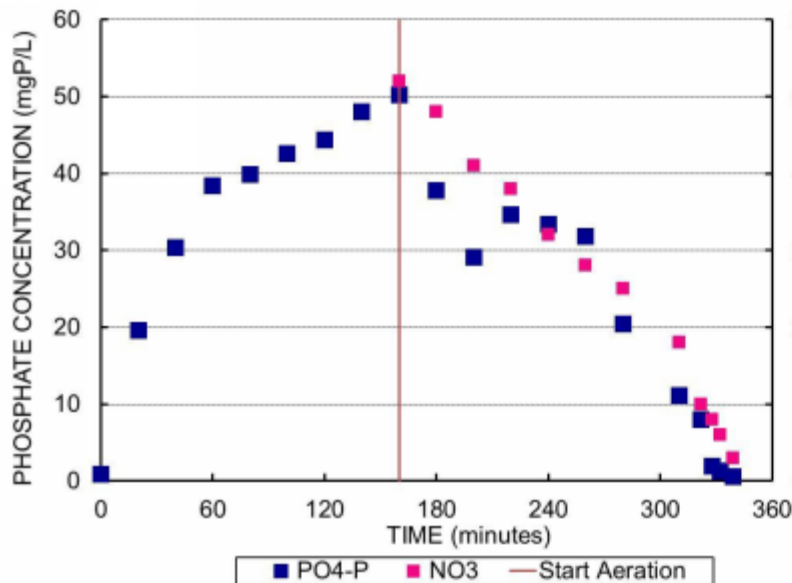


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Phosphorus Release and Uptake Tests



PRU #	DO (mg/L)	Max P-Uptake Rate (mgP/gVSS/hr)	Max P-Release Rate (Ac) (mgP/gVSS/hr)
NO ₂	0 then 0.3	4.01	13.21
NO ₃	0 then 0.3	3.30	16.89