### Facility Tour and Technical Presentation

### City of Dover, New Hampshire Phase I Upgrade and MLE Conversion Pilot Program

NEWEA Specialty Conference in Dover, NH August 24, 2016

CONTRACTOR OF

Presented by: Timothy R. Vadney, PE Project Manager



## Presentation Overview

- Why Remove Nitrogen
- Nitrogen Removal Basics
- Facility Planning and Phase I Upgrade
- Modified Ludzack-Ettinger Pilot Program
  - § Pilot Program Background
  - § Nitrogen Removal
  - § Construction
  - § Preliminary Results
- Questions

Why are nutrients an issue in the environment?

- Stimulates algae and plant growth
- Creates dissolved oxygen issues
- P limiting fresh water nutrient
- N limiting marine water nutrient

# **Effects of Nutrients in Receiving Waters**

Healthy Levels of Nutrients

algae growth is limited

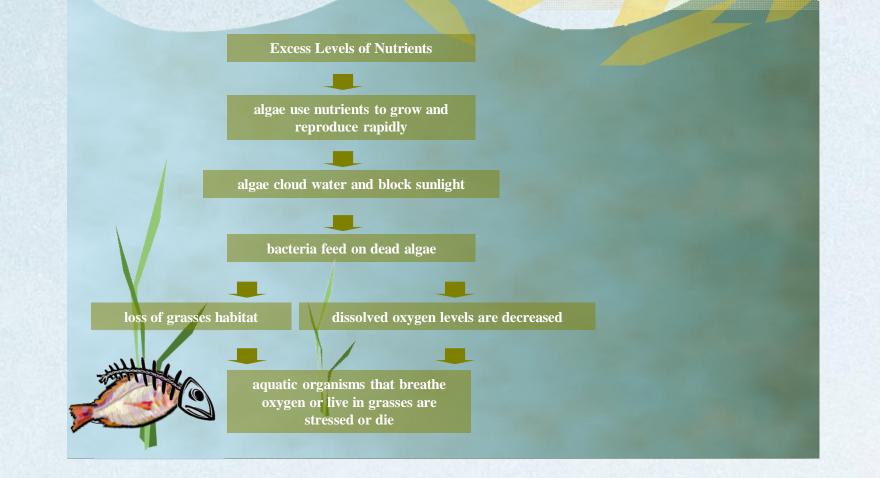
sunlight penetrates clear water

submerged aquatic grasses use sunlight to make food

healthy grasses provide habitat for other organisms grasses produce oxygen

healthy aquatic community

### **Effects of Nutrients in Receiving Waters**



## How Much Estuary Nitrogen is Too Much?

- Typical threshold nitrogen concentration
  ~ 0.2 to 0.5 ppm
- Governed by:
  - dissolved oxygen
  - Eelgrass
  - habitat protection
  - hydrodynamics

## Algal Impact on Water Clarity



## Algal Impact On Water Clarity



### PART I A. EFFLUENT LIMITATIONS AND MONITORING REQUIREMENTS

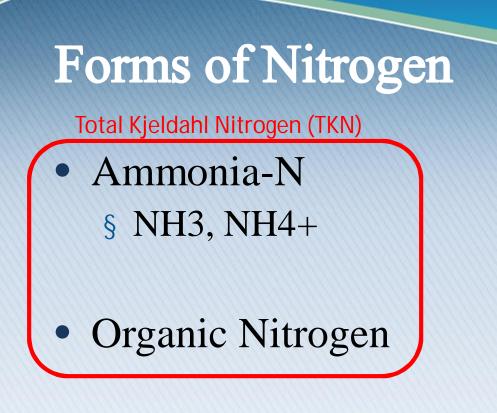
1. During the period beginning on the effective date and lasting through the expiration date, the permittee is authorized to discharge from Outfall Serial Number 001 treated domestic, commercial, and industrial wastewater effluent to the Piscataqua River. Such discharges shall be limited and monitored by the permittee as specified below. Samples taken in compliance with the monitoring requirements specified below shall be taken at end of all processes, including disinfection, or at an alternative representative location approved by the EPA and NHDES-WD.

Effluent Parameter		Effluent Limit			Monitoring Requirement	
		Average Monthly	Average Weekly	Maximum Daily	Frequency	Sample Type
Flow, MGD		Report		Report	Continuous	Recorder
BOD <sub>5</sub> ; mg/l (lb/d)	I Utar mus	14443Q(1136)	, 45 (1764)	50 (1960) U. /	2/Week <sup>2</sup>	24 Hour Composite
TSS; mg/l (lb/d)	Total Am	monia Nitrogen <sup>9</sup>	Nitrogen <sup>9</sup> : mg/l		ort	24 Hour Composite
pH Range <sup>3</sup> ; Standard U				Report		Grab
Fecal Coliform <sup>3,4,7</sup> ; colo		Total Kjeldahl Nitrogen <sup>9</sup> ; mg/l			Report	
Enterococci Bacteria <sup>3,4,8</sup>	Total Nit	Total Nitrate/Nitrite Nitrogen <sup>9</sup> ; mg/l			Report	
Total Residual Chlorine	Total Nit	Total Nitrogen <sup>°</sup> ; mg/l (lb/d)			3.0 (118)	
Total Ammonia Nitroge			<b>,</b>			24 Hour Composite
Total Kjeldahl Nitrogen						24 Hour Composite
<b>Total Nitrate/Nitrite Nit</b>	(Applicat	(Applicable April 1 through October 31)				24 Hour Composite
Total Nitrogen <sup>9</sup> ; mg/l (lb	Total Am	Total Ammonia Nitrogen <sup>9</sup> ; mg/l			ort	24 Hour Composite
(Applicable April 1 thro		Total Kjeldahl Nitrogen <sup>°</sup> ; mg/l			ort	
<b>Total Ammonia Nitroge</b>	Total Nit	Total Nitrate/Nitrite Nitrogen <sup>9</sup> ; mg/l			Report	
Total Kjeldahl Nitrogen	Total Nit	Total Nitrogen <sup>9</sup> ; mg/l (lb/d)		Report		24 Hour Composite
<b>Total Nitrate/Nitrite Nit</b>		· · · · · · · · · · · · · · · · · · ·				24 Hour Composite
Total Nitrogen <sup>9</sup> ; mg/l (lb/d)		Report		Report	2/Week	24 Hour Composite
(Applicable November 1 three	ough March 31)					
Whole Effluent Toxicity						
LC50 <sup>10,11,12</sup> ; Percent Effluent				100	1/Year	24 Hour Composite
Total Recoverable Aluminum <sup>13</sup> ; mg/l				Report	1/Year	24 Hour Composite
Total Recoverable Cadmium <sup>13</sup> ; mg/l				Report	1/Year	24 Hour Composite
Total Recoverable Chromium <sup>13</sup> ; mg/l				Report	1/Year	24 Hour Composite
Total Recoverable Copper <sup>13</sup> ; mg/l				Report	1/Year	24 Hour Composite
Total Recoverable Lead <sup>13</sup> ; mg/l				Report	1/Year	24 Hour Composite
Total Recoverable Nickel <sup>13</sup> ; mg/l				Report	1/Year	24 Hour Composite
Total Recoverable Zinc <sup>13</sup> ; mg/l				Report	1/Year	24 Hour Composite

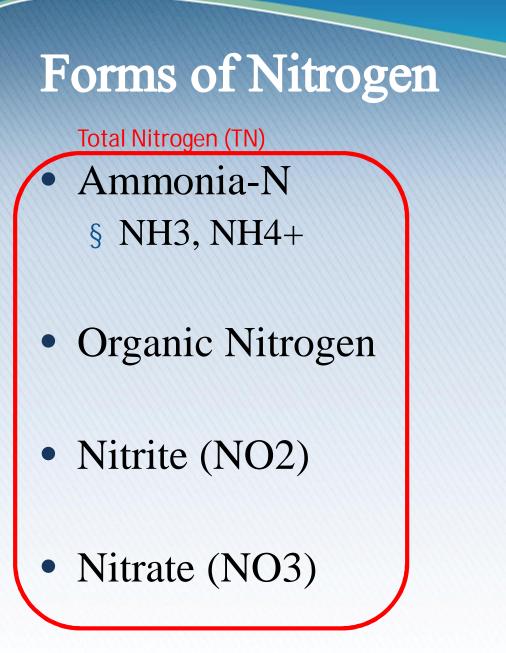
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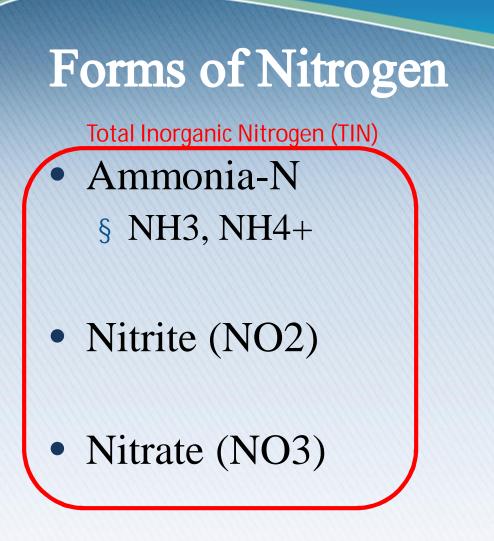
## Forms of Nitrogen

- Ammonia-N
  § NH3, NH4+
- Organic Nitrogen
- Nitrite (NO2)
- Nitrate (NO3)



- Nitrite (NO2)
- Nitrate (NO3)



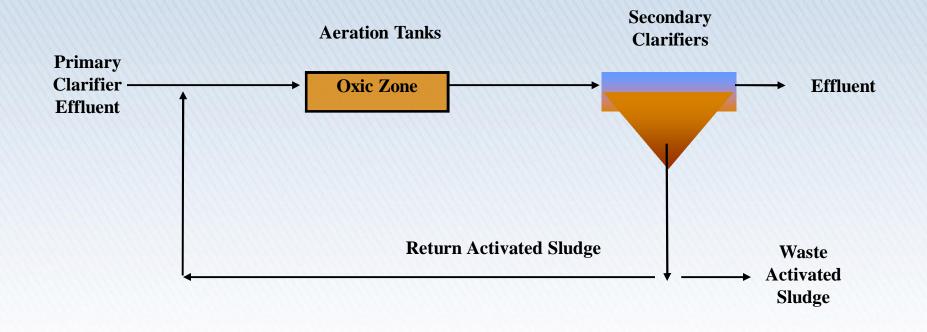


• Organic Nitrogen

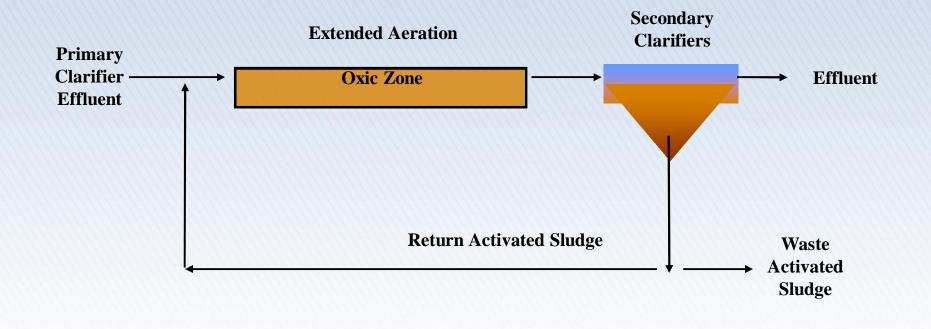
### Typical Nitrogen Wastewater Concentration

		% removal
Typical influent sewage	40 ppm	
Typical secondary effluent	32 ppm	20%
Level 1-N removal	8 ppm	80%
Level 2-N removal	5 ppm	87.5%
Level 3-N removal	3 ppm	92.5%

## Conventional Activated Sludge

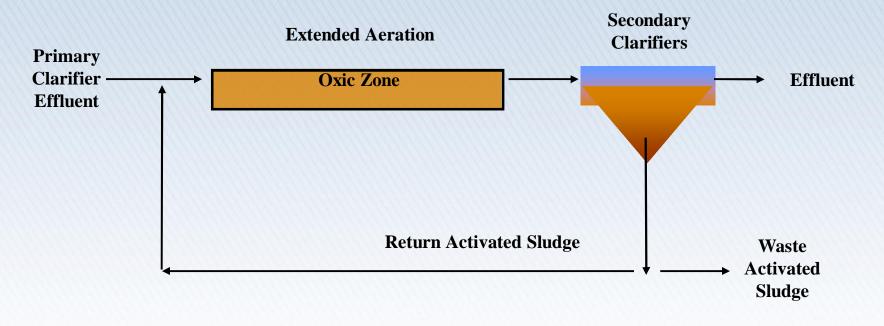


### How to Upgrade for Ammonia Removal

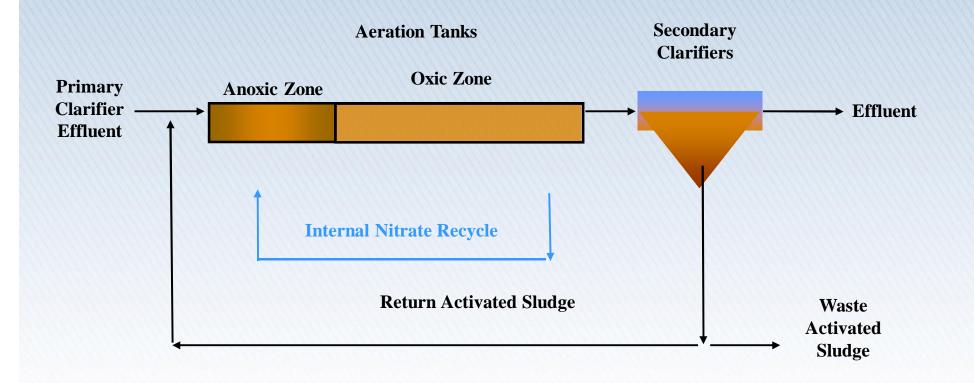


How to Upgrade for Ammonia Removal

### NH3 à NO2 à NO3

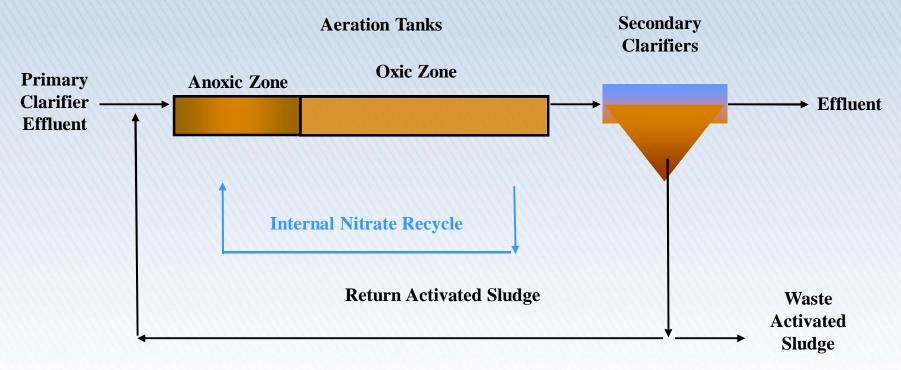


### How to Upgrade for TN Removal MLE Process



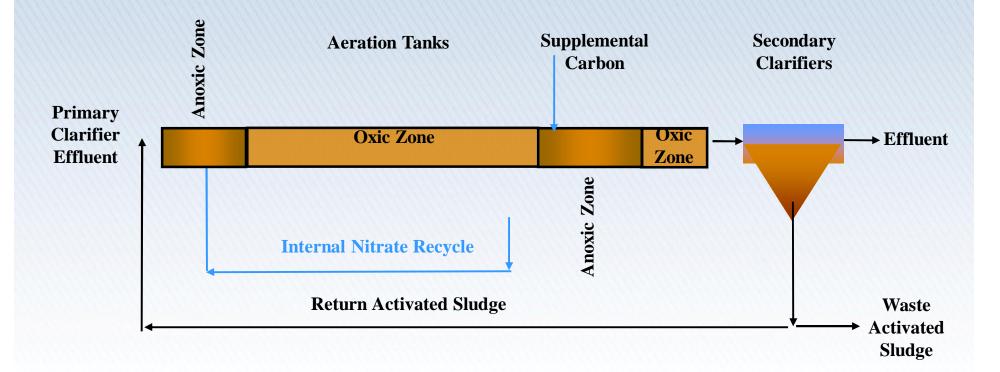
### How to Upgrade for TN Removal MLE Process

### NH3 à NO2 à NO3 à N2+O2



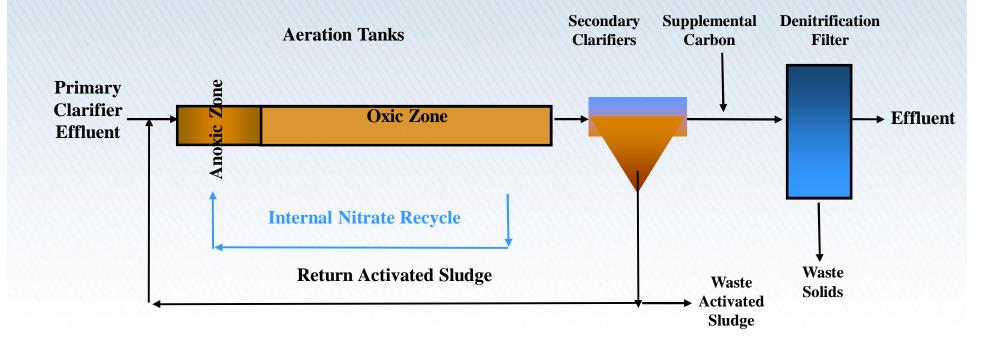
## How to Upgrade for Higher TN Removal (3 to 5 mg/1TN)

### **Four-Stage Bardenpho Process**



### Alternative Approach to TN Limits (3 to 5 mg/1 Range)

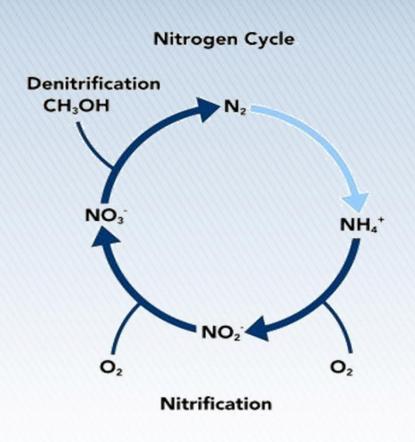
### **MLE Process Coupled with Denitrification Filter**



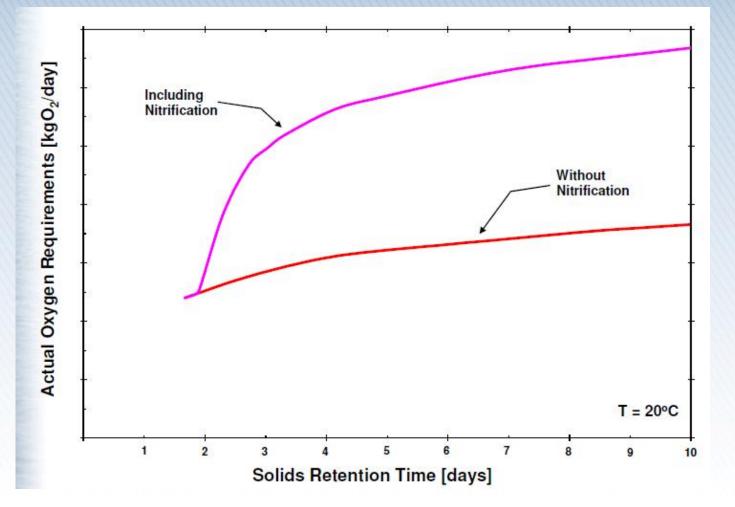
### Nitrogen Removal

### **3-Step Process:**

- Ammonification:
  - § urea & organic N ® NH<sub>4</sub>-N
- Nitrification (aerobic)
  - §  $NH_4-N+O_2$  ®  $NO_3-N$
  - § Autotrophic bacteria
  - § -4.57 mg/L  $O_2$  (consumption)
  - § -7.14 mg/L Alk (consumption)
- Denitrification (anoxic)
  - § NO<sub>3</sub>-N  $\otimes$  N<sub>2</sub>-
  - § facultative bacteria
  - § +3.57 mg/L Alk (gain)
  - $+2.86 \text{ mg/l O}_2 \text{ (credit)}$



## SRT/Nitrification Impact on $0_2$ Demand



## Nitrification Requirements

Parameter	BOD Removal	Nitrification
MCRT (days)	0.5 – 1.0	4 – 15
DO (mg/L)	> 0.5	> 2.0 (optimal)
Temperature (°C)	>0	25 (optimal)
рН	5 – 9	6.5 – 8 (optimal) More alkalinity

# Requirements for Denitrification

- Need nitrate to be formed
  - § Nitrate is formed during nitrification
  - § As long as system is nitrifying, this criterion is met
- Need "denit" or anoxic zone in system:
  - § Nitrate
  - § Bacteria
  - § Substrate (Food/BOD)
  - § No oxygen, but mixing to retain biomass in suspension

### Conditions in the Anoxic Zone

- DO less than 0.3 mg/l
  - § No aeration
  - § Low aeration
  - § Cyclical aeration
- Carbon source
  - § Primary effluent
  - § Endogenous
  - § Methanol or other chemicals

### • Mixing

- § Pulsed or cycled air
- § Submersible mixers
- § Vertical mixers

## City of Dover

Great Bay Issues

### Pending TN Limit

Facility Planning Efforts

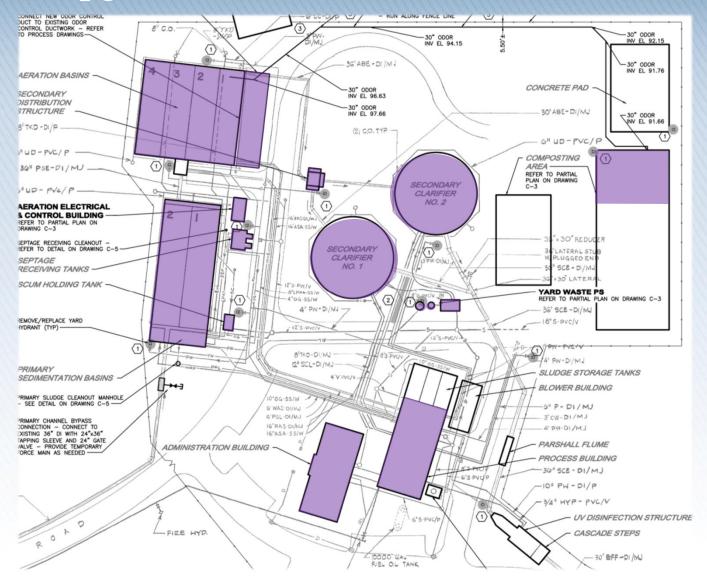
### • Wastewater Facilities Plan

- § Equipment Assessment
- § Building System Assessment
- § Alternatives for removing TN

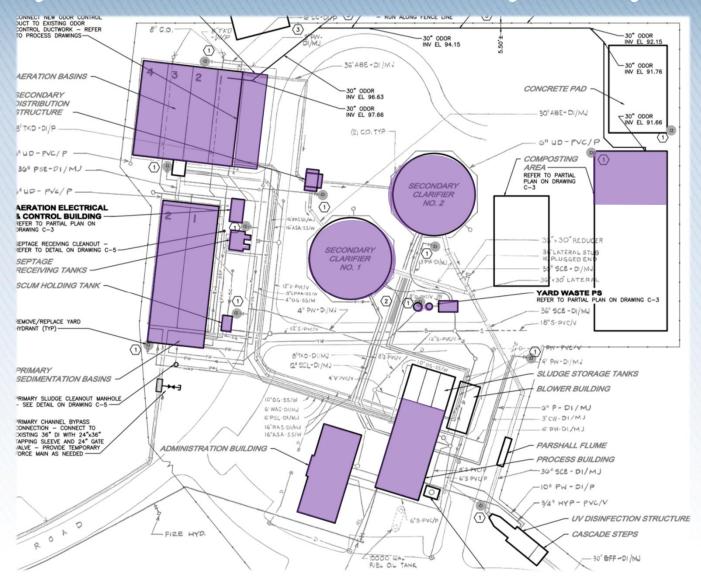
### • Prioritized Improvements

- § Phase I Upgrade
- § Pilot Program to lower effluent TN

### Phase I Upgrade

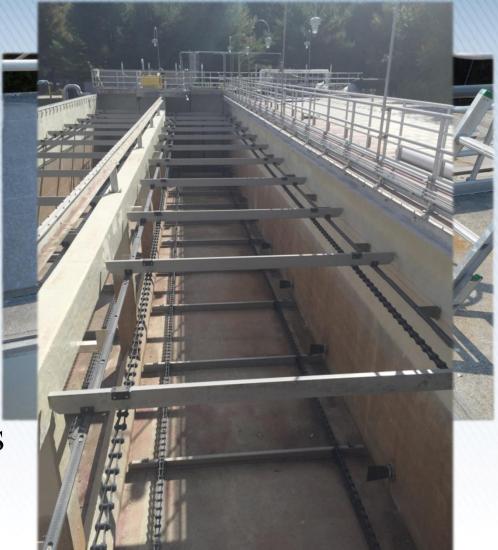


Primary Sedimentation Basins/ Primary Gallery

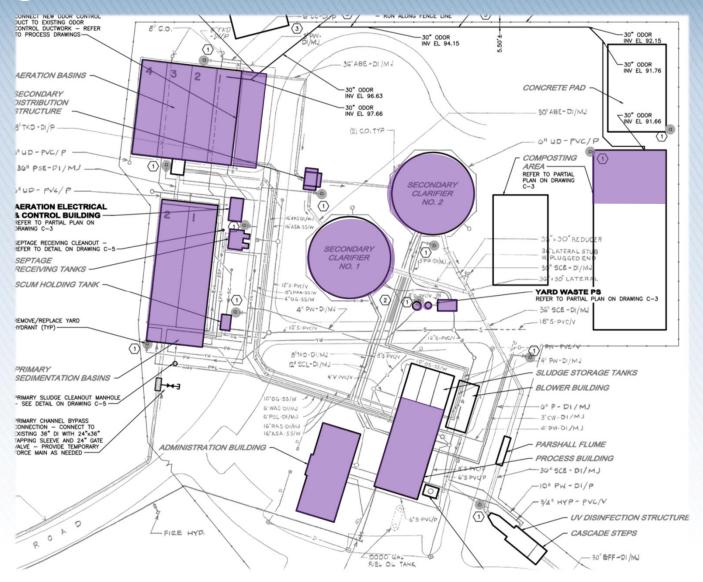


### Project Overview Primary Sedimentation Basins/ Primary Gallery

- H<sub>2</sub>S resistant coatings
- Chain + Flight mechanisms
- Primary sludge pumps, grinder, actuated valves
- Channel air blowers



### Septage/ Scum Tanks

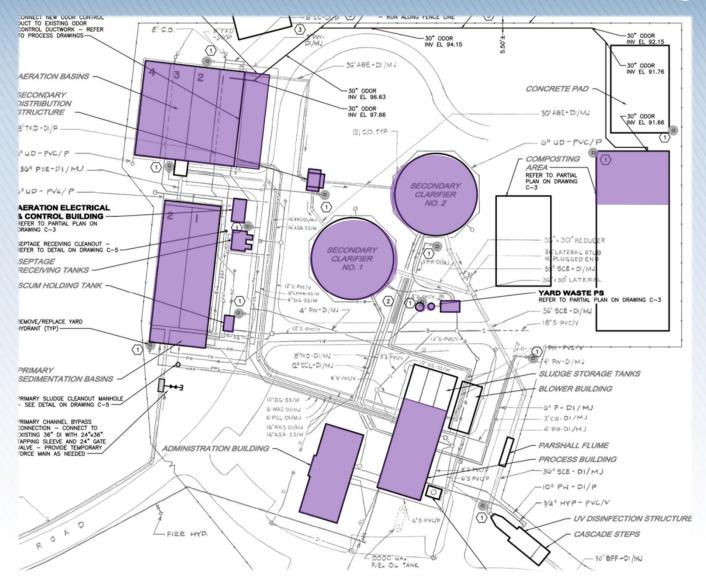


## Project Overview Septage/ Scum Tanks

- Septage pumps
- Septage blowers
- Radar level instruments
- H<sub>2</sub>S resistant coatings
- New hatches



### Aeration Basins/ Aeration, Electrical, and Control Building



### Aeration Basins/ Aeration, Electrical, and Control Building



## Project Overview Secondary Distribution Structure

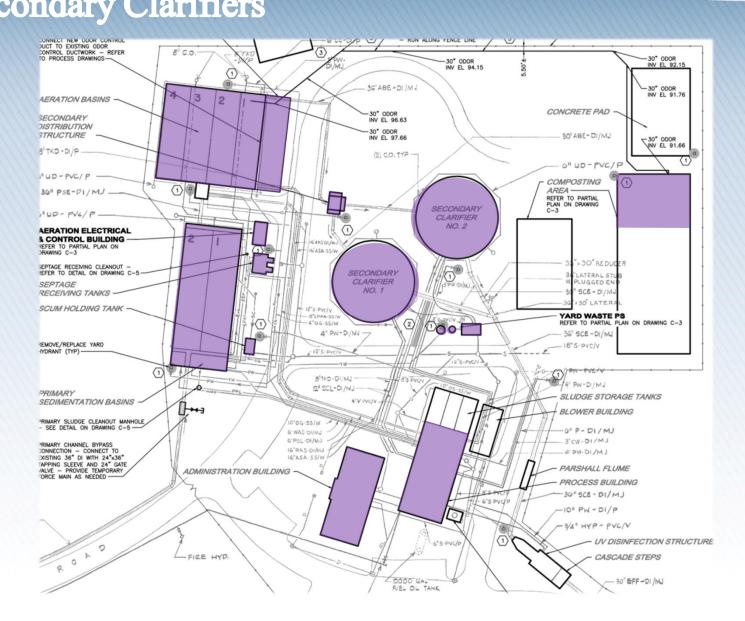
### CONNECT NEW ODOR CONTROL DUCT TO EXISTING ODOR CONTROL DUCTWORK - REFER TO PROCESS DRAWINGS 3 8" C.O 30" ODOR INV EL 92.15 30" ODOR INV EL 94.15 1 a 36" ABE - DI JM J -30" ODOR INV EL 91.76 AERATION BASINS 2 CONCRETE PAD -30" ODOR SECONDARY INV EL 96.63 DISTRIBUTION -30" ODOR INV EL 97.66 STRUCTURE 30" ABE- DI/MJ 30" ODOR NV EL 91.66 B"TKD - DI/P (2) C.O. TYP 6" UD - PVC/P "UD-PVC/P COMPOSTING AREA -30" PSE-DI/MJ REFER TO PARTIAL PLAN ON DRAWING C-3 SECONDARY JUD-PV4/P CLARIFIER NO. 2 **AERATION ELECTRICAL** 0 & CONTROL BUILDING REFER TO PARTIAL PLAN ON DRAWING C-3 6420.00 3 × 30" REDUC SEPTAGE RECEIVING CLEANOUT - REFER TO DETAIL ON DRAWING C SECONDARY LATERAL S CLARIFIER PLUGGED E SEPTAGE NO. 1 SCE - DI/N RECEIVING TANKS 30 LATER SCUM HOLDING TANK 12"S-PVC/V YARD WASTE PS 0 2 REFER TO PARTIAL PLAN ON DRAWING C-3 -4"06-55/W DOOF 4" PW-DI/MJ 36" SCE - DI/MJ a REMOVE/REPLACE YARD 18"S-PVC/V TYDRANT (TYP) 12"5-P -- £ 2"S-PVCN 4" PW-DI/MJ (1) BITKO-DI/MJ S. PVCI 6 12" SEL-DI/MJ PRIMARY SLUDGE STORAGE TANKS SEDIMENTATION BASINS H++= BLOWER BUILDING PRIMARY SLUDGE CLEANOUT MANHOLE 06-55/W G" P-DI/MJ 6" WAS DUMJ 6'PSL-DI/MJ 3°CW-DI/MJ RIMARY CHANNEL BYPASS CONNECTION - CONNECT TO EXISTING 36" DI WITH 24"x36" TAPPING SLEEVE AND 24" GATE IG"RAS-DI/MJ 4" PW-DI/MJ 16"ASA-SS/W PARSHALL FLUME ALVE - PROVIDE TEMPORARY ADMINISTRATION BUILDING PROCESS BUILDING 8'S PVC -30" SCE - DI/MJ 6"S PVCP -10" PW - DI/P 0 3/4" HYP- PVC/V D 1)( 6'S-PVC UV DISINFECTION STRUCTURE 0 4 0 FILE HYD CASCADE STEPS R 0000 GAL - 30' EFF -DI /MJ FUEL OIL TANK

# Project Overview

Secondary Distribution Structure



## Project Overview Secondary Clarifiers



#### Project Overview Secondary Clarifiers

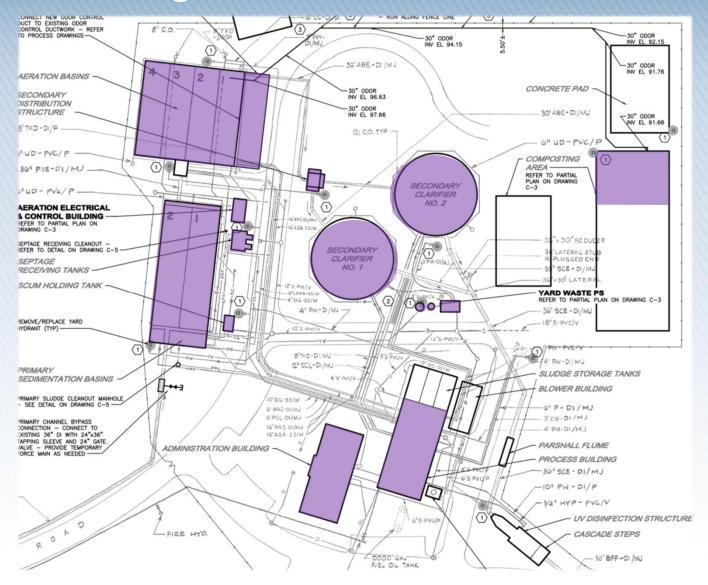
- SS suction header mechanisms
- Full radius skimme arm

LECTION

- Walkway, platform
- Algae sweeps
- Density current baffles
- Concrete coating of launders

#### Project Overview

#### **Process Building**

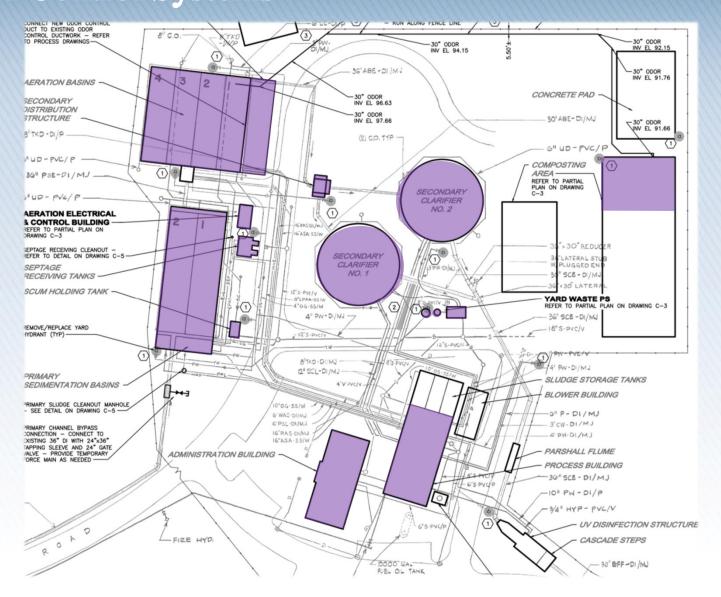


#### Project Overview Process Building

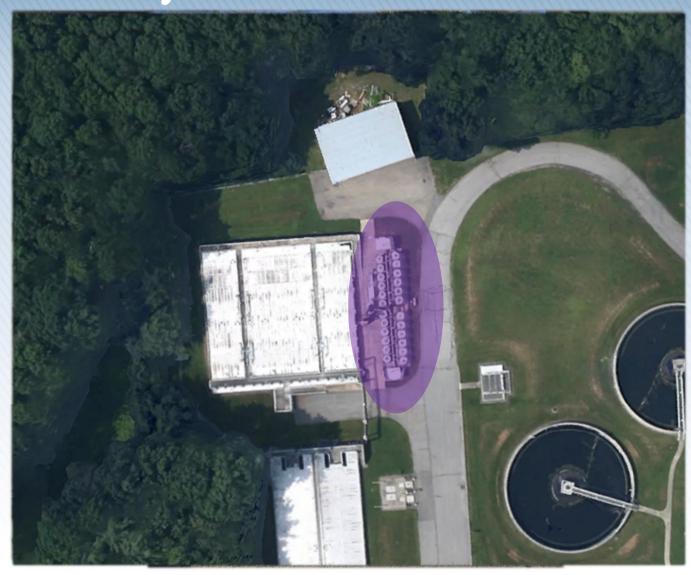
- RAS pumps
- WAS pumps
- Valves, flow meters
- Polymer system
- Hypochlorite system
- Potassium permanganate pumps



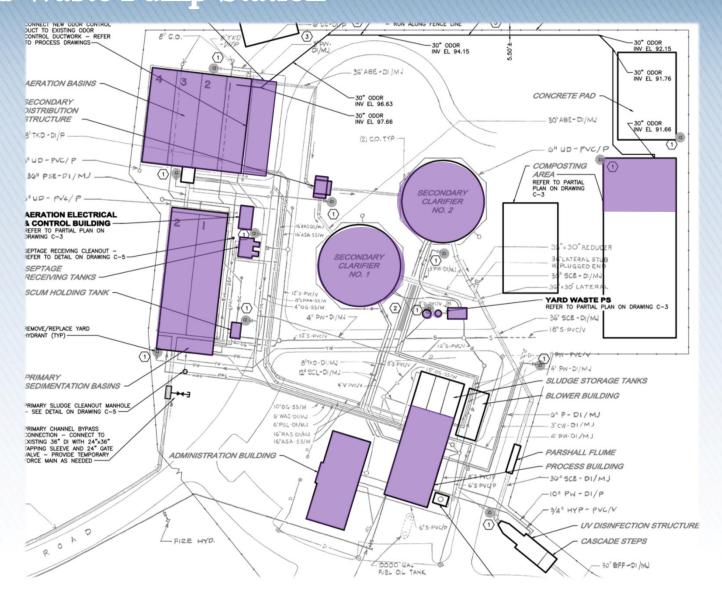
## Project Overview Odor Control Systems



# Project Overview Odor Control Systems



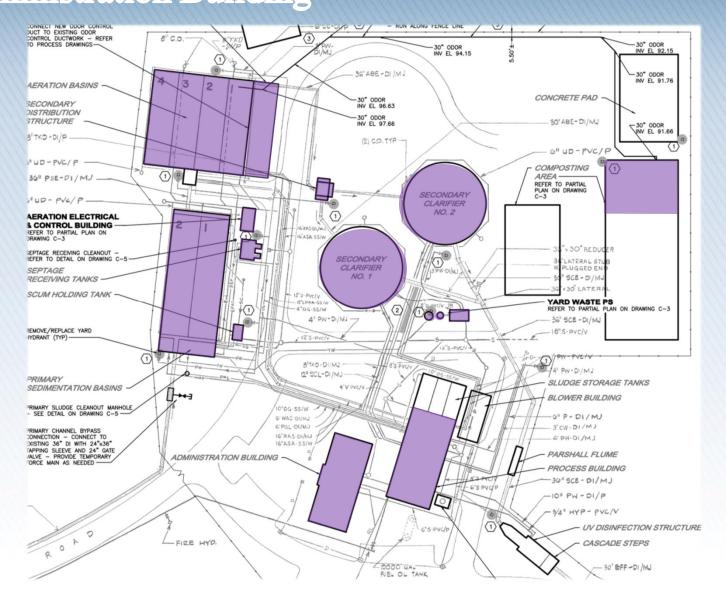
# Project Overview Yard Waste Pump Station



# Project Overview Yard Waste Pump Station



## Project Overview Administration Building



## Project Overview Administration Building

- Boilers
- HVAC
- Roofs
- Floors
- Ceilings
- Laboratory
- SCADA



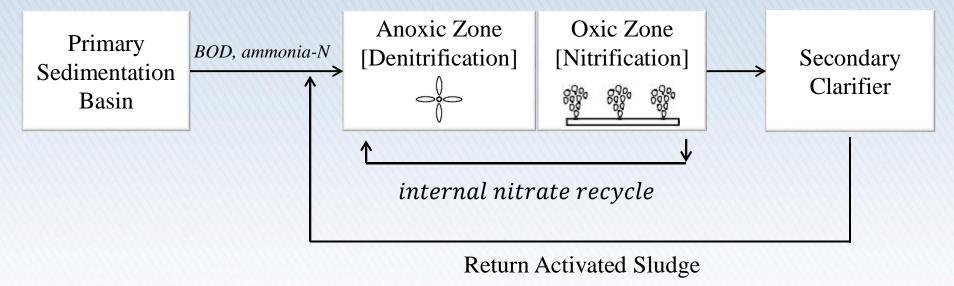
## Modified Ludzack-Ettinger Pilot Program Background

- Pending effluent total nitrogen limits
- Influent sampling program and Biowin modeling
- Reviewed / analyzed BNR processes and technologies
- Selected Modified Ludzack-Ettinger process
- Goal: seasonal average effluent Total Nitrogen < 8 mg/L

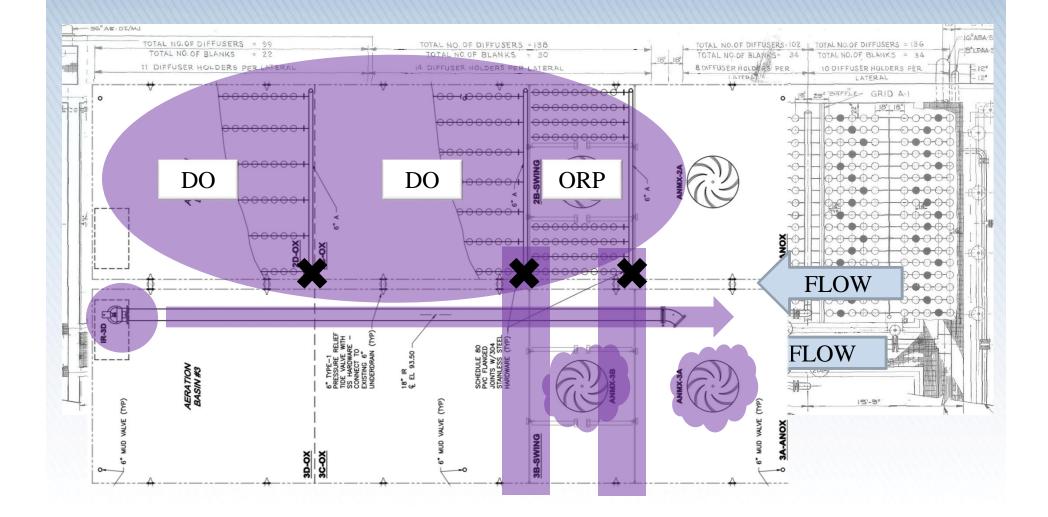
## Modified Ludzack-Ettinger Nitrogen Removal

ammonia- $N + O_2 \rightarrow (nitrifiers) \rightarrow H^+ + H_2O + NO_2 + energy$ 

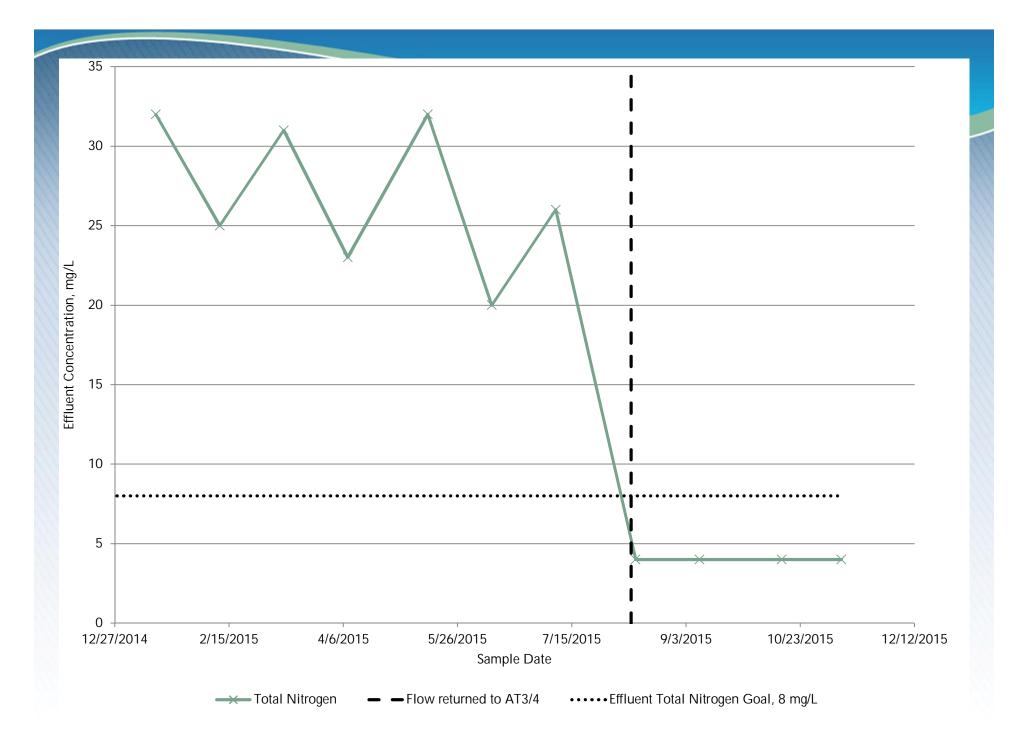
 $BOD + NO_3 \rightarrow (dentoif t dentoif t dentoin Braision) \rightarrow Nographic genergy$ 



#### Modified Ludzack-Ettinger Construction







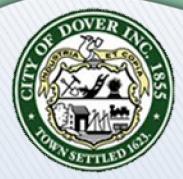
# Modified Ludzack-Ettinger Nitrogen Removal – Preliminary Results

• Goal: effluent Total Nitrogen < 8 mg/L

Conventional		MLE Process	
Sample Date	Total Nitrogen (mg/L)	Sample Date	Total Nitrogen (mg/L)
August 13, 2014	25	August 12, 2015	< 4.0*
September 10, 2014	26	September 9, 2015	< 4.0*
October 8, 2014	27	October 15, 2015	< 4.0*
November 12, 2014	27	November 10, 2015	< 4.0*

\* Result below reporting limit





Thank you!